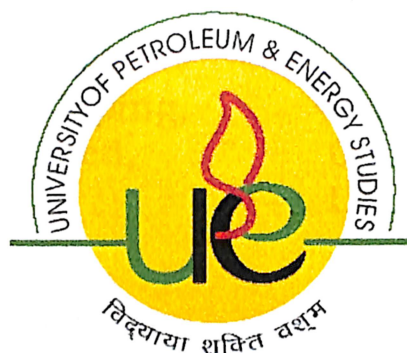


# DESIGN OF PROPYLENE GAS PIPELINE SYSTEM

By

**A.SELVAM**  
**R 160206001**

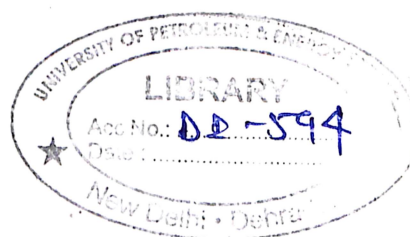


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**COLLEGE OF ENGINEERING**  
**UNIVERSITY OF PETROLEUM & ENERGY STUDIES**  
**ENERGY ACRES, DEHRADUN**

**MAY 2008**

# DESIGN OF PROPYLENE GAS PIPELINE SYSTEM

A thesis submitted in partial fulfillment of the requirements for the  
Degree of  
Master of Technology  
[Pipeline Engineering]

By

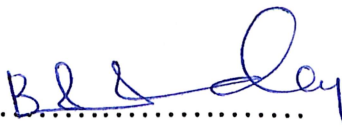
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Under the Guidance of

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Approved

.....

DEAN

**COLLEGE OF ENGINEERING**  
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**ENERGY ACRES, DEHRADUN**

**MAY 2008**

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30<sup>th</sup> April 2008

**To whomsoever it may concern**

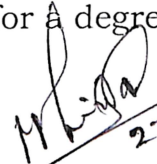
This is to confirm that Mr. A Selvam who is a final year M.Tech student of "UNIVERSITY OF PETROLEUM AND ENERGY STUDIES, Deharadun, has done his academic project on ESSAR in our company along with our team from 24<sup>th</sup> March 2008 to 30<sup>th</sup> April 2008.

**for Saipem India Projects Ltd.**

  
**M Srinivasarao**  
**Manager HR & Organization**

## CERTIFICATE

This is to certify that work contained in this thesis titled "Design of Propylene Gas Pipeline System" has been carried out by Mr.A.Selvam under my supervision and has not been submitted elsewhere for a degree.

  
22/05/2008  
R.P.Shriwas,  
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Date: 22/05/2008

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A.Selvam

M.Tech [Pipeline Engineering]

## ABSTRACT

In the Basic Engineering Package [BEP] process calculations such as Line sizing, Velocity, Pressure calculations, Preparation of Process & Instrumentation Diagram [P&ID] etc has been carried out. After this, it has been forwarded to the Piping department to carry out the Equipment layout, Pipe routing, Isometric Drawing preparation, modeling of the pipelines in Caesar II software to carry out the stress analysis. In the stress analysis proper supports has to be provided in order to check all the stresses are with in the safer specified limits of the ASME code. Finally after checking all the parameters it has been forwarded to the site for construction activities.

This project covers the major activities of the process and piping department for designing a 10 Km propylene gas pipeline for the transportation of 16.68 MSCMD of propylene gas from the refinery complex to the near by petrochemical units to meet the supply and demand in order to increase the productivity.

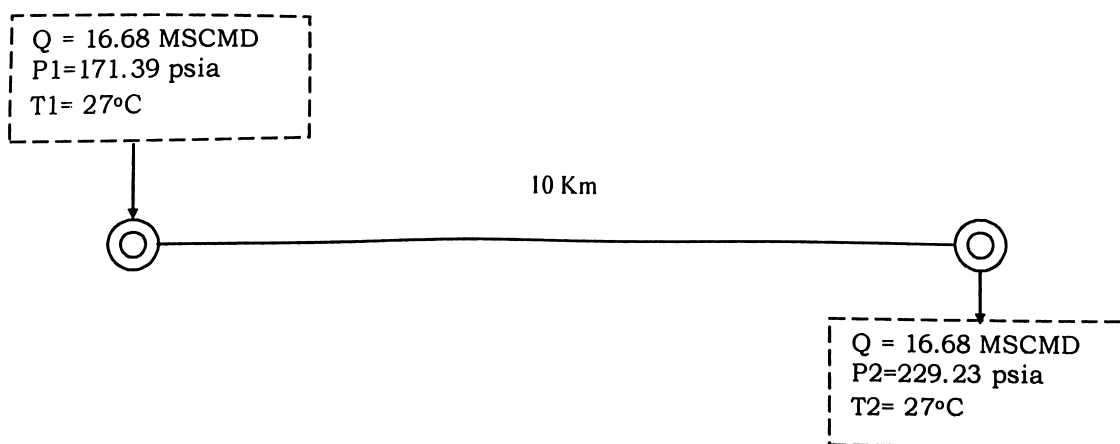


Figure – Pipeline Design Profile

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## **NOMENCLATURE**

- $Q_b$  – Gas flow rate  $\text{ft}^3/\text{hr}$
- $D_i$  – Pipeline inner diameter inch
- $D_o$  – Pipeline Outer diameter inch
- $L$  – Length of the Pipeline ft
- $t$  – Thickness of line pipe inch
- $P$  – Pressure at any section psia
- $P_1$  – Pressure at inlet section psia
- $P_2$  – Pressure at outlet section psia
- $T_f$  – Flowing Gas temperature  $^{\circ}\text{R}$
- $u$  – Gas Velocity ft/sec
- $u_e$  – Erosional Gas Velocity ft/sec
- $Z_1$  – Compressibility Factor at suction condition
- $Z_2$  – Compressibility Factor at discharge condition
- $G$  – Gas Gravity
- $R$  – Gas Constant =  $10.73 \text{ ft}^3 \cdot \text{psia}/\text{lbmoles} \cdot ^{\circ}\text{R}$
- $\eta_a$  – Adiabatic Efficiency
- $\eta_o$  – Overall efficiency
- $\eta_m$  – Mechanical efficiency
- $S$  – Yield strength of the pipe material psi
- $F$  – Basic Design Factor
- $E$  – Longitudinal joint factor
- $T$  – Temperature deaerating factor
- $S_L$  – Longitudinal stress, MPa (psi)
- $S_H$  – Hoop stress, MPa (psi)
- $W$  – Distributed weight of pipe material, contents and insulation, N/m (lbs/ft)
- $n$  – Conversion factor,  $10^{-3} \text{ m}/\text{mm}$  (1 ft/12 in)
- $\gamma$  – Heat Capacity
- $Z$  – Pipe section modulus,  $\text{mm}^3$  ( $\text{in}^3$ )
- $S_E$  – Displacement stress range, MPa (psi)
- $S_A$  – Allowable displacement stress range, MPa (psi)
- $f$  – Stress reduction factor

- Sc – Basic allowable stress of minimum material temperature, MPa (psi)
- Sh – Basic allowable stress at maximum material temperature, MPa (psi)
- N – Equivalent number of full displacement cycles during the expected service life,  $< 2 \times 10^6$
- S<sub>b</sub> – Resultant bending stress, MPa (psi)
- S<sub>t</sub> – Torsional stress, MPa (psi)
- i<sub>i</sub> – In plane stress intensity factor
- M<sub>i</sub> – In plane bending moment, N-m (lb-ft)
- i<sub>o</sub> – Out plane stress intensity factor
- M<sub>o</sub> – Out plane bending moment, N-m (lb-ft)
- M – Torsional moment, N-m (lb-ft)
- Y – Resultant of total displacement strains, mm (in)
- L<sub>s</sub> – Straight line distance between anchors, m (ft)
- K – Constant, 208.3 for SI units
- S<sub>N</sub> – Longitudinal stress from sustained and occasional loads, MPa (psi)

### **1. INTRODUCTION**

There are a lot of users of polymer grade propylene in India, while propylene is in short supply. The pipeline will help all propylene producers and consumers to better manage supply/demand balances and also improve the industry's overall competitiveness. The major propylene derivatives are enjoying healthy markets. Especially polypropylene, which is 50 percent of propylene's take. Plentiful supply, competitive cost, and versatility continue to support an upward trend in the consumption of propylene on a worldwide scale. Increasing, production of propylene gas in the world and the consumption by the petrochemical industries has been transported by pipelines or in liquid form in ships.

This project is aimed to ensure the uninterrupted supply of propylene gas to the nearby petrochemical and polymer industries. For this pipelines are the most efficient, safer and cheaper way of transportation. This project addresses the design of propylene gas pipeline and the compressor station piping layout, piping routing and stress analysis of compressor station piping for the transportation of 16.68 MSCMD propylene gas. Piping inside the boundaries of a chemical plant, refinery, or gas processing plant falls under the scope of ASME B31.3 – Process piping and ASME B31.8, covering gas transmission and distribution piping systems.

Unattended pumping stations move large volume of oil and petroleum products under high pressure. Similarly, gas transmission system supported by compressor stations, deliver large volume of gas to large distance.

Many factors have to be considered in the design and engineering of long distance pipelines, including the nature and volume of fluid to be transported, length of the pipeline, the type of the terrain traversed and the environmental constraints. Construction procedures for most pipeline systems can be adapted to consider specific environmental conditions and are tailored to cause minimal impact on the environment.

### **2. LITERATURE REVIEW**

The use of pipelines has a long history, more than 1,000 years ago, the Romans used lead pipes in their aqueduct system to supply water to Rome. Introduction of steel pipe in the 19<sup>th</sup> century, which greatly increased the strength of pipes of all sizes

Major innovations in pipeline technology made since 1950

- Introduction of new pipeline materials such as ductile iron and large diameter concrete pressure pipes for water, and PVC (polyvinyl chloride) pipe for sewers
- Use of pigs to clean the interior of pipelines and to perform other functions
- Batching of different petroleum products in a common pipeline
- Application of cathodic protection to reduce corrosion and extend pipeline life
- Use of large side booms to lay pipes, machines to drill or bore under rivers and roads for crossing, machines to bend large pipes in the field, x-rays to detect welding flaws, and so forth.

#### **Existing Propylene Pipeline**

The Lou-Tex propylene pipeline is a 263-mile, 10" pipeline that transports chemical grade propylene from Sorrento, La., to Mont Belvieu, Texas.

Lou-Tex, a common carrier pipeline regulated by the Federal Energy Regulatory Commission, transports chemical grade propylene produced from the petrochemical and refinery corridor along the Mississippi River between Baton Rouge and New Orleans to the larger petrochemical complex east of Houston.

#### **Propylene Production**

Global propylene demand typically grows at about 5%/year. Due to their large economic bases, North America, West Europe, and Northeast Asia are the largest producing and consuming regions.

Propylene is produced mostly from steam crackers as an ethylene by-product. Refinery FCC units are the other dominant global supplier of propylene, as a by-product of motor gasoline and distillates production.

### **Products**

Polypropylene production for mechanical parts, containers, fibers, and films is the primary consumer of propylene. Other important propylene consumers include acrylonitrile, propylene oxide, oxo-alcohols, cumene, and acrylic acid.

### **Propylene supply**

By 2010, global propylene supplies will reach 83.7 million tones. Most of the new capacity additions will be in Asia (38%), the Middle East (30%), and North America (10%).

### **Propylene demand**

Global propylene demand continues to grow strongly during the next 5 years, as global economies recover and pent-up demand by consumers further influences the petrochemical industry.

### **Transport, safety and environment benefits**

- Decongestion of road, rail and waterways
- Allowing olefins derivatives (consumer goods) to be produced close to market and consumers
- Decoupling economic growth and transport growth
- Olefins ultimately end up in consumer goods and are linked to economic growth

### **Safety**

- Safest mode of transport if integrity well managed
- Underground transport isolated from general public

### **Reducing emissions**

- Pipelines emissions very low vs. other modes of transport (CO<sub>2</sub> graph)
- Reduction of environmental impact
- No impact on country side after installation

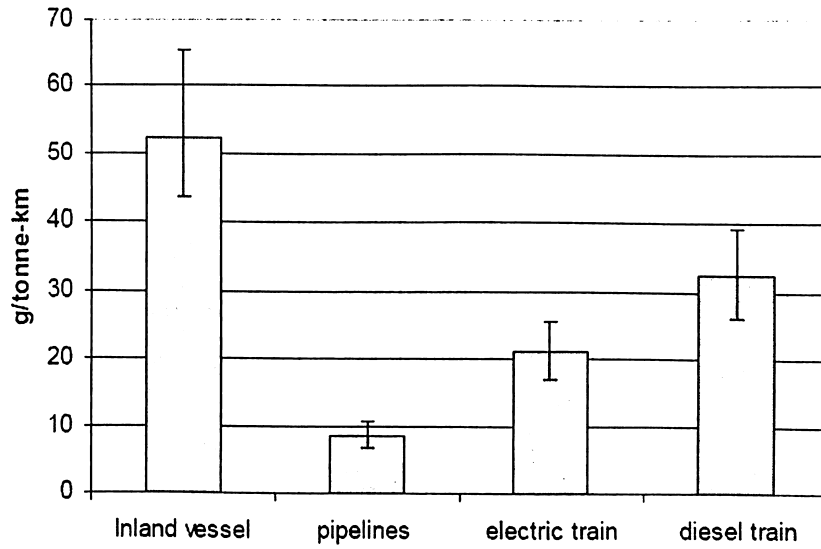


Figure - 01 CO<sub>2</sub> Emission by various transport modes

A pipeline network provides the opportunity to run plants at higher operating rates



### **3. THEORITICAL DEVELOPMENT**

#### **3.1 CODES AND STANDARDS**

Pipelines and related facilities expose the operators and potentially the general public to the inherent risk of high pressure fluid transmission. As a result national and international codes and standards have been developed to limit the risk to a reasonable minimum. They are not intended to be substitutes for good engineering practices for safe design.

The codes and standard have been followed in the design, construction, operation and maintenance of gas pipeline are

ISO 13623 - Petroleum & Natural gas industries – Pipeline transportation systems.

ASME B 31.8 - Gas Transmission and Distribution Piping Systems.

API 5L - Specifications for Line pipe

API 617- Axial and Centrifugal compressors and expander – compressors for petroleum, chemical and gas industry applications

ASME B 31.3 – Process Piping

### **DESIGN CALCULATION**

#### **3.2 PIPELINE SIZING**

$$\text{Pipe Diameter [Di]} = \{1.44 * 10^{-3} * [Q_b * Z * T_f / P * u]\} ^{0.5}$$

Where,

- Q<sub>b</sub> – Gas flow rate ft<sup>3</sup>/hr
- D<sub>i</sub> – Pipeline inner diameter inch
- P – Pressure at any section psia
- T<sub>f</sub> – Flowing Gas temperature °R
- u – Gas Velocity ft/sec
- Z – Compressibility Factor

### 3.3 EROSIONAL VELOCITY

The Erosional velocity represents the upper limit of gas velocity in a pipeline. As the gas velocity increases, vibration and noise result. Higher velocities also cause erosion of the pipe wall over a long time period. The Erosional velocity ( $u_e$ ) may be calculated as follows

$$\text{Erosional velocity } [u_e] = 100/[29 \cdot G \cdot P / Z \cdot R \cdot T]^{0.5}$$

Where,

- P – Minimum Pressure at any section psia
- $T_f$  – Flowing Gas temperature °R
- $u_e$  – Erosional Gas Velocity ft/sec
- Z – Compressibility Factor
- G – Gas Gravity
- R – Gas Constant = 10.73 ft<sup>3</sup>·psia/lbmoles·°R

The recommended value for the gas velocity for the gas pipelines is 40 – 50 % of the Erosional velocity or for 50- 60 % of the Erosional velocity for non major mainlines [i.e. 15-17 m/s]

$$\text{Gas operating velocity } [u] = \text{Erosional velocity } [u_e] \cdot 0.6$$

### 3.4 OPERATING VELOCITY

$$\text{Gas operating velocity } [u] = 1.44 \cdot 10^{-3} \cdot [Q_b \cdot Z \cdot T_f / P \cdot D_i^2]$$

### 3.5 REYNOLDS NUMBER

The Reynolds number can be used to check the flow regime of the gas transmission pipeline

$$Re = [45 \cdot Q_b \cdot G] / D_i$$

Where

- $Q_b$  – Gas flow rate ft<sup>3</sup>/hr
- $D_i$  – Pipeline inner diameter inch
- G – Gas Gravity

If the calculated value of the Reynolds number is more than 4000 than the flow is fully turbulent.

### **3.6 TRANSMISSION FACTOR**

The transmission factor for fully turbulent flow is given by Nikuradse equation as

$$[1/f]^{0.5} = 4 \cdot \log [3.7 \cdot D_i / K_e]$$

Where         $[1/f]$  – Transmission Factor  
                $D_i$  – Pipeline Inner Diameter inch  
                $K_e$  – Effective Roughness inch

The Nikuradse equation shows that if the effective roughness of the pipe is increased, the transmission factor decreases and results in higher pressure drop. By decreasing the effective roughness, higher transmission factor or lower pressure drop is obtained

The effective roughness that is measured and used for uncoated commercial pipes are with in the range of 650 -700 micro inches

### **3.7 PRESSURE CALCULATION**

Steady State Flow Equation: Panhandle A Equation

Panhandle A equation is normally used for medium to relatively large diameter pipeline, operating under medium to high pressure. These equations have been successfully used for Reynolds numbers in the range of 4 million to 40 million.

$$P_1^2 - P_2^2 = K_1 Q_b^n$$

$$R = 2.552 \cdot 10^{-4} \cdot T_f \cdot Z \cdot [G^{0.855} / D_i^{4.856}]$$

$$n = 1.855$$

$$K_1 = R \cdot L$$

Where,         $Q_b$     – Gas flow rate ft<sup>3</sup>/hr  
                $D_i$     – Pipeline inner diameter inch  
                $L$      – Length of the Pipeline ft  
                $P_1$     – Pressure at inlet section psia  
                $P_2$     – Pressure at outlet section psia  
                $T_f$     – Flowing Gas temperature °R  
                $Z$      – Compressibility Factor  
                $G$      – Gas Gravity

### **3.8 COMPRESSOR CALCULATION**

The compressor compresses the gas and raises its pressure (and its temperature) to the level required to ensure that the gas will be transported from one point to another point, such that the required outlet pressure can be maintained. The higher the outlet pressure at destination, the higher will be the pressure required at source. This will cause the compressors to work harder. The energy input to the gas by the compressors will depend upon the compression ratio and gas flow rate, among other factors.

#### **3.8.1 COMPRESSION RATIO**

Generally the compression ratio is limited to 1.2 to 1.8 for centrifugal compressors

Compression Ratio  $R = \text{Discharge Pressure} / \text{Suction Pressure}$

#### **3.8.2 ADIABATIC EFFICIENCY**

The adiabatic efficiency can be calculated, knowing the actual discharge temperature of the gas, suction and discharge pressures and the compressibility factors, using the following equation

$$\text{Adiabatic Efficiency } [\eta_a] = (T_2 / T_1 - T_1) * (Z_1 / Z_2) * \{(P_2 / P_1)^{\gamma - 1} / \gamma - 1\}$$

#### **3.8.3 HORSEPOWER REQUIRED**

From the energy input to the gas, following equation is used to calculate the compressor HP

$$\text{HP} = 4.0639 * (\gamma / \gamma - 1) * Q * (Z_1 + Z_2 / 2) * T_1 * (1 / \eta_a) * \{(P_2 / P_1)^{\gamma - 1} / \gamma - 1\}$$

Where

HP – compression horsepower

$\gamma$  –  $C_p / C_v$  the ratio of specific heats of gas

Q – Gas flow rate, MSCMD

$T_1$  – Suction temperature of gas, °K

$P_1$  – Suction pressure of gas, psia

$P_2$  – Discharge pressure of gas, psia

$Z_1$  – Compressibility of gas at suction conditions, dimensionless

$Z_2$  – Compressibility of gas at discharge conditions, dimensionless

$\eta_a$  – Compressor adiabatic efficiency

### 3.8.4 BRAKE HORSEPOWER (BHP)

Taking into account a mechanical efficiency  $\eta_m$  of the compressor driver, the Brake Horsepower (BHP) required may be calculated as follows

$$\text{BHP} = \text{HP} / \eta_m$$

### 3.8.5 OVERALL EFFICIENCY

The mechanical efficiency  $\eta_m$  of the driver generally varies from 0.95 to 0.98.

By multiplying the two efficiencies, we get the overall efficiency  $[\eta_o]$  as follows

$$\text{Overall efficiency } [\eta_o] = \eta_a \times \eta_m$$

## 3.9 STRENGTH OF PIPE

The internal pressure in a pipe is limited to what the pipe material and wall thickness can withstand at a certain temperature. As the pipe pressure is increased, the stress in the pipe material increases. Ultimately, at some internal pressure the pipe will rupture. Therefore for each pipe size and wall thickness, depending upon the pipe material, there is a safe internal pressure beyond which it is not advisable to operate the pipeline. This is known as the maximum allowable operating pressure (MAOP), sometimes shortened to maximum operating pressure (MOP).

There are two stresses developed in a pipe wall due to internal pressure. The larger of the two is called the hoop stress and acts in the circumferential direction. The second is the axial or longitudinal stress that acts along the axial direction. The axial stress is one-half the magnitude of the hoop stress.

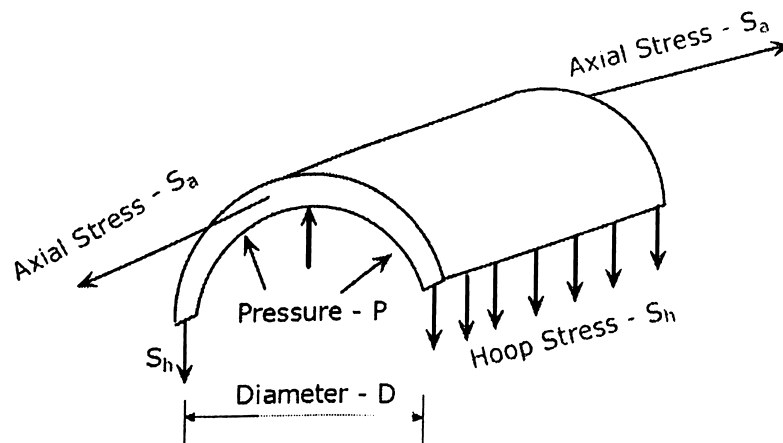


Figure – 02 Pipe stresses due to internal pressure

### **3.9.1 HOOP STRESS**

The allowable internal pressure can be easily calculated using the Barlow's equation as follows.

$$S_H = [P \cdot D_o] / [2 \cdot t]$$

Where,  $S_H$  – Allowable hoop stress in pipe, psia  
 $P$  – Allowable internal pressure, psia  
 $D_o$  – Pipe outside diameter, inch.  
 $t$  – Pipe wall thickness, inch.

### **3.9.2 LONGITUDINAL STRESS**

The longitudinal stress,  $S_L$  can be calculated from the below equation as follows

$$S_L = [P \cdot D] / [4 \cdot t]$$

It must be noted that unlike the General Flow equation or other flow equations, the diameter used here is the outside diameter, not the inside diameter. In practice, to calculate the internal design pressure for a gas pipeline, we modify the Barlow's equation slightly by introducing some factors that depend upon the pipeline manufacturing method, operating temperature and the class location of the pipeline. The modified equation is as follows

$$\text{Thickness } [t] = [P \cdot D] / [2 \cdot S \cdot F \cdot E \cdot T]$$

### **3.10 THICKNESS CALCULATION**

Thickness of the line pipe is calculated as per ASME B 31.8

$$t = [P \cdot D] / [2 \cdot S \cdot F \cdot E \cdot T]$$

Where,  $D_o$  – Pipeline Outer diameter inch  
 $t$  – Thickness of line pipe inch  
 $P$  – Pressure at any section psia  
 $S$  – Yield strength of the pipe material psi  
 $F$  – Basic Design Factor  
 $E$  – Longitudinal joint factor  
 $T$  – Temperature deaerating factor

### **Location Class 1**

A Location Class 1 is any 1 mile section that has 10 or fewer buildings intended for human occupancy. A Location Class 1 is intended to reflect areas such as wasteland, deserts, mountains, grazing land, farmland, and sparsely populated areas.

#### **Division 1**

A Class 1 location where the design factor of the pipe is greater than 0.72, but equal to or less than 0.80, and which has been hydrostatically tested to 1.25 times the maximum operating pressure.

#### **Division 2**

Class 1 location where the design factor of the pipe is equal to or less than 0.72 and which has been tested to 1.1 times the maximum operating pressure.

### **Location Class 2**

A Location Class 2 is any 1 mile section that has more than 10 but fewer than 46 buildings intended for human occupancy. A Location Class 2 is intended to reflect areas where the degree of population is intermediate between Location Class 1 and Location Class 3 such as fringe areas around cities and towns, industrial areas, ranch or country estates, etc.

### **Location Class 3**

A Location Class 3 is any 1 mile section that has 46 or more buildings intended for human occupancy except when a Location Class 4 prevails. A Location Class 3 is intended to reflect areas such as suburban housing developments, shopping centers, residential areas, industrial areas, and other populated areas not meeting Location Class 4 requirements.

### **Location Class 4**

Location Class 4 includes areas where multistory buildings are prevalent, and where traffic is heavy or dense and where there may be numerous other utilities underground. Multistory means 4 or more floors above ground including the first or ground floor.

**Basic Design Factor [F]**

<b>Location Class</b>	<b>Design Factor</b>
Location Class 1, Division 1	0.80
Location Class 1, Division 2	0.72
Location Class 2	0.60
Location Class 3	0.50
Location Class 4	0.40

Table 01 – Basic Design Factor [F]

**Longitudinal Joint Factor [E] for API 5L**

<b>Pipe class</b>	<b>E Factor</b>
Seamless	1.0
Electric resistance welded	1.0
Electric flash welded	1.0
Furnace butt welded	0.6
Submerged arc welded	1.0

Table 02 – Longitudinal joint Factor [E]

**Temperature Derating Factor [T] for Steel Pipe**

<b>Temperature °C</b>	<b>T Factor</b>
121 or less	1.000
149	0.967
177	0.933
204	0.900
232	0.867

Table 03 – Temperature Derating Factor [T] for Steel Pipe



### 3.11 COMPRESSOR STATION PIPING LAYOUT & DESIGN

Piping design and equipment arrangement are interrelated subjects that cannot be well taught in the classroom. Most good designers throughout history have learned their profession by a combination of academic and practical work. The use of previous designs and drawings is a good way to learn and improve on current designs.

The experienced piping designer needs to have a working knowledge of plant layout, equipment arrangement, and system functionality associated with one or more fields of endeavor, such as commercial, industrial, refinery, petrochemical, or power. In addition, the designer must have an understanding of the practical application of piping materials, valves, pumps, tanks, pressure vessels, heat exchangers, power boilers, vendor-supplied skid assemblies, steam turbine drivers, and other machinery and equipment.

#### **CENTRIFUGAL COMPRESSOR**

##### **Inlet Piping**

With higher compressor velocities and rotating speeds the plant layout designer must give greater consideration to the compressor inlet line piping. The ASME test code requires a minimum of three diameters of straight run piping between the elbow and the inlet nozzle. However, such factors as gas velocities, molecular weight and temperature must be considered for optimum layout. An equipment engineer should be consulted at the outset to develop a base case layout requirement. The preferred design is one in which the horizontal run is parallel to the compressor shaft. Another factor that could influence the straight run requirements is the need to inject wash water into the gas stream to clean compressor blades.

##### **Suction Line strainers**

Compressor suction lines must be free from any foreign particles that could damage the internals of the machine. Strainers are installed in the inlet line between the block valve and the compressor inlet nozzle. If the strainer is of permanent type, a clean out connection must be added to remove any trapped foreign matter during a shutdown of the compressor.

### **Break-Out flanges**

All lines to the compressor that must be removed for maintenance of the compressor or strainer removal must have a set of flanges in the line in addition to the set at the compressor nozzle

### **Straightening Vanes**

When the straight run on the inlet piping is less than desired, a straightening vane may be installed to smooth the flows and improve the compressor performance. This vane must be in accordance with ASME standards. If the use of vanes can be tolerated, the length for any arrangement can be divided by four.

## **3.12 CONSIDERATIONS FOR PIPING LAYOUT**

### **1. Project Client and Owner Requirements**

Most projects have project-specific requirements imposed by the owner. These usually include additional requirements above the codes and standards which may have direct impact on both pipe layout and equipment location. Most of these requirements derive from operations feedback which the owner contractually invokes on future projects. Owners may not have a thorough understanding of all the levels of detail required to produce a piping design, but they know the finished product. It is very important that all project personnel and designers know and understand these requirements.

### **2. System Piping and Instrumentation Diagrams (P&ID)**

These are the schematic single line process diagrams which define the sequence of equipment, valves, inline components, pipeline sizes, and overall system arrangement required for proper system function.

### **3. P&ID Implementation and Physicalization**

Piping and instrumentation diagrams are the piping designer's roadmap for laying out piping systems. The designer should understand the P&ID and the specific system characteristics. With this knowledge the designer is required to

develop the P&ID and arrange connections and branches as required to best suit the process to actual physical design.

### **4. Project Piping Specifications**

These documents or databases define the following essential information

- System design and operating pressures and temperatures
- Piping materials
- Pipe wall thickness or schedules
- Types of fittings to be used, e.g., butt weld, socket weld, or screwed
- Valve and flange pressure rating and insulation requirements
- In addition, the piping specification defines the fabrication, examination, testing, inspection, and installation requirements, including the requirements for seismic installations, where applicable.

### **5. Equipment Outlines**

These documents can be either imported computer-aided design or drafting (CADD) files or prints of the equipment being piped. They include overall dimensions and the pipe size, wall thickness, flange pressure rating, and locating dimensions of all pipe nozzles and other connections.

### **6. General Arrangements or Equipment Location Drawings**

These drawings will indicate the location of all major pieces of equipment in the plant which the designer will either verify or relocate, as required, to accommodate the physical pipe routing as designed or redesign the piping to accommodate the particular piece of equipment. Generally equipment location drawings are developed by senior-level piping designers during the proposal preparation and are taken over by the project team upon award of the contract. From this point on they are revised and updated as part of the normal process of design development. Equipment should be arranged with the piping layout in mind. Equipment locations and relational arrangements should be evaluated during the piping layout design process. Adjustments and occasionally major changes to equipment arrangement are required to solve major piping

arrangement problems. Piping system design is dependent on the input from numerous reference sources prior to the start of piping design.

### **7. Piping Layout Considerations and Planning Studies for Improved Piping Economics**

Proper planning is an important activity performed by the piping designer in the early stages of a project. Space conservation and a symmetric piping arrangement are achieved when all the systems are evaluated in the preliminary stages of design. This study will become the final design. It is important to consider the cost of the piping material at this time for the expensive lines. These lines should be kept as short as possible, while maintaining proper piping flexibility even if this requires changing the equipment arrangement.

Piping layout then becomes a matter of designing dimensioned routings from one point to another point with the branches, valves, piping specialties, and instrumentation as indicated on the P&ID. This statement, however, is an oversimplification of the process, since many other factors must be considered, such as interference, piping flexibility, material costs, pipe supports, operation and maintenance, and safety and construction requirements.

### **8. Interferences**

One of the most important aspects of piping layout is the avoidance of interferences with other facilities in the plant such as other piping systems; structural steel and concrete; heating, ventilating, and air-conditioning (HVAC) ductwork and electric cable trays and conduit. Once the designer is satisfied that the current system layout is interference-free, it will be added to the area composite drawing and the plastic model.

Specifically, three-dimensional (3D) computer modeling can provide an efficient, accurate, and cost-effective alternative to the traditional manual methods for interference detection.

### **9. Piping Flexibility**

The effects of the thermal expansion of pipe and fittings as a result of system

operating temperature changes cannot be overlooked during the layout and routing of any piping system. The function of piping flexibility or stress analysis has, for the most part, been delegated to the computer particularly in the case of high temperature, high-pressure piping systems. The piping stress analyst translates and enters the piping design data into the computer, reviews the output data, and if the system is too rigid, may suggest appropriate corrective redesigns. However, it is the piping designer's responsibility to ensure that the final stress analysis results are incorporated into the final pipe support and pipe routing design.

The piping designer should route piping with flexibility designed into it, using the minimum amount of pipe, fittings, and expansion loops by considering the following:

- Avoid the use of a straight run of pipe between two pieces of equipment or between two anchor points.
- A piping system between two anchor points in a single plane should, as a minimum, be L-shaped, consisting of two runs of pipe and a single elbow. This type of arrangement should be subjected to a "quick-check" analysis to determine if a formal computer stress analysis is required. A preferred solution in this case may be a series of two or more L-shaped runs of pipe.
- A piping system between two anchor points with the piping in two planes may consist of two L-shaped runs of pipe, e.g., one L-shaped run in the horizontal plane and another in the vertical plane. This arrangement should also be subjected to a quick-check analysis.
- A three-plane configuration may consist of a series of L-shaped runs and/or U shaped expansion loops designed into the normal routing of the system.
- When the expected thermal expansion in any given run of pipe is high, consider the use of an anchor at or near the center of the run, thereby distributing the expansion in two directions.
- For systems consisting of a large-diameter main and numerous smaller branch lines, the designer must ascertain that the branches are flexible enough to withstand the expansion in the main header.
- Systems which are to be purged by steam or hot gas must be reviewed to ensure that they will be flexible during the purging operation.

- System or equipment bypass lines may be cold due to lack of flow while the main runs are at operating design temperature, resulting in excessive stresses.
- Temperatures during initial start-up and testing are often greater than those at operating conditions.
- Closed relief valve and hot blow down systems should be given special attention due to rapid transients in temperature.

### 10. Valves

The piping designer must be familiar with proper application of all types of valves including gate, globe, plug, butterfly, ball, angle, diaphragm, check, pressure relief, and control valves and their methods of operation including manual, chain, gear, air, hydraulic, or motor. The following general guidelines should be applied when locating valves in any piping system:

- Valves should be installed with the stems between the vertically upward and horizontal positions with particular attention given to avoiding head and knee knockers, tripping hazards, and valve stems in the horizontal plane at eye level that may be a safety hazard. Large motor-operated valves should be installed in the vertical upright position where possible to facilitate support and maintenance.
- Valves in acid and caustic services should be located below the plant operator's eye level or in such a manner as to not present a safety hazard.
- The location of valves, with consideration for operating accessibility, should be accomplished in the natural routing of the system from point to point, avoiding the use of vertical loops and pockets.
- Valves in overhead piping with their stems in the horizontal position should be located such that the bottom of the hand wheel is not more than 6.5 ft (2 m) above the floor or platform. Only infrequently operated valves should be located above this elevation, and then the designer should consider the use of a chain operator or a platform for access.
- Where chain operators are used, the valves should be located such that the chain does not present a safety hazard to the operating personnel.
- A minimum of 4 in (100 mm) of knuckle clearance should be provided around all valve hand wheels.

- Valves should not be installed upside down.
- Space should be provided for the removal of all valve internals.

Improper application and placement of valves in the piping system can be detrimental to system function. This can result in malfunction of the valve and in water hammer, and this can cause the valves to literally self-destruct.

The following are some specific recommendations and methods of avoiding these problems for some specific types of valves.

### **10 - i. Control Valves**

All control valve stations should be designed with the valve stem in the vertical upright position and a minimum of three diameters of straight pipe both upstream and downstream of the control valve, in order to reduce the turbulence entering and leaving the valve and to provide space for removal of the flange studs or bolts. Where applicable, this straight pipe will include the usual reduction in pipe size required to match the control valve size. Space must be provided for flange stud bolt removal where control valve bodies are designed for through bolt installation.

### **10 - ii. Butterfly Valves**

Butterfly valves should be provided with a minimum of five diameters of straight pipe upstream of the valve; and if this requirement has been met, the valve stem and operator may be oriented in the position best suited for operation and maintenance. When a butterfly valve is preceded by an elbow and this straight-pipe requirement cannot be met, the valve stem must be oriented in the same plane as the elbow. That is, if the elbow is in the vertical plane, the valve stem must also be in the vertical plane. This recommendation is based on the fact that the velocity profile of the discharge of an elbow is not symmetric. The result can be fluid dynamic torque that is twice the magnitude of that found for a valve with a straight run of pipe upstream. The resultant eccentric forces applied to valve disk produces excessive vibration and disk flutter which eventually may completely destroy the valve.

### 10 – iii. Check Valves

The preferred installation of any check valve is in a horizontal, continuously flooded run of pipe with cap up; however, swing check valves will function properly in vertical runs of pipe with the flow up. However, the velocity and the rate of flow must be adequate to move the valve disk away from the seat and to maintain the valve in the open position, as required.

Experience has indicated that check valves are highly susceptible to chattering due to upstream turbulence caused by elbows and branches. Therefore the designer should provide upstream straight pipe in accordance with the valve manufacturer's recommendations. However, where this information is not available, the preliminary design should include a minimum of five diameters of straight pipe upstream of all check valves. In addition, the designer should be aware that this requirement can be as much as 10 diameters of straight pipe depending on the type of valve and the manufacturer.

### 10 – iv. Safety Relief Valves

The arrangement for installation of safety and relief valves is very critical and involves the actual location of the valve itself, the design of the vent stack, and the design of any associated drain piping. The designer should adhere to the valve manufacturer's recommendations

### 10 – v. Valve Location

- All relief valves must be in the vertical upright position and fitting-bound to the top of a horizontal run of pipe, the pressure source, and must not be located less than one nominal header diameter from any butt weld.
- A safety valve inlet connection in a high-velocity steam line should be located at least 8 to 10 nominal header diameters downstream of any bend in the header, to minimize the possibility of acoustically induced vibrations. In addition, it should be at least 8 to 10 nominal header diameters either upstream or downstream of any diverging or converging T or Y fitting.
- No other header branch penetration, for any purpose, should be made in the same circumferential cross section containing the safety valve inlet nozzle.



- Where more than one safety valve or a service branch is to be installed in the same header run, a minimum distance of 24 in (600 mm) or 3 times the sum of the nozzle inside radii, whichever is greater, shall be provided between the nozzles.
- Where more than two safety valves are located in the same header run, the spacing between valves should be varied such that the distance between two adjacent valves differs by at least an inlet nozzle diameter.

### **11. Pipe Racks**

Pipe racks are structures designed and built specifically to support multiple pipes where adequate structure is not available. Pipe layout on pipe racks should follow the Pipe Planning Study concepts. Avoid designing one pipe at a time in order to avoid unnecessary overcrowding and fittings for pipes to enter and depart from the rack. Where possible, pipes should rest directly on the rack with the use of insulation, if required. Steam piping should exit the rack with a vertical up-and-over to avoid condensate collection points, while water piping should exit the rack with a vertical down-and-under to avoid a high-point air pocket collection point.

### **12. Insulation**

The piping designer should be familiar with these requirements and specifically with the thickness of insulation for any given system. In the location and spacing of piping systems, there must be clearance space between the insulation of one pipe and any adjacent pipe and/or other possible interference such as structural steel. The piping designer should also recognize that in some applications insulation may not be required for the prevention of heat loss but will be needed for personnel protection and the spacing and clearances should be adjusted accordingly.

### **13. Pipe Supports**

Pipe supports require structural support, which means that piping should be located in close proximity to steel or concrete. Do not locate the pipe too close to the structure, so as to allow adequate space for the pipe support hardware

to facilitate installation. Additionally the pipe insulation needs to be considered for clearances and insulation saddles. The most preferred location is either resting directly on structural steel for bottom support or using a single rod to the structure directly above the pipe.

### **14. Operability, Maintenance, Safety, and Accessibility**

Operability, maintenance, safety, and accessibility are interdependent, and certainly if any given piping component is accessible, it is also assumed to be operable and maintainable. However, maintenance may require additional space for dismantling the component. It is the responsibility of the piping designer to design a piping arrangement that satisfies all these (and other) requirements with the lowest total cost, i.e., resulting in the shortest pipe runs and the fewest fittings and pipe supports.

#### **14 - i. Operability**

From the standpoint of operating personnel, operability means being able to perform daily functions in an efficient manner. This is done with consideration for the frequency of operation and the degree of physical effort required to performing it. The designer cannot make every valve and instrument ideally accessible, but will concentrate on those requiring the most frequent operation. Safety-related equipment and valves that are required to be operated during an emergency or to perform critical system functions must be accessible without exception.

To ensure success, the designer, system engineer, and operating personnel work out the final arrangement. In difficult cases, models or even full-size mock-ups have been used as design aids. In general, an operable valve or instrument is one that can be readily reached when standing at grade or on an elevated floor or platform provided for that purpose. The position of the valve hand wheel should be such that the force necessary to operate it can be applied without strain or undue contortions or interference from valves, lines, or other equipment. It is recognized that plant operating personnel will occasionally have to reach for a drain from a kneeling position or a vent valve

from a ladder, but these are infrequent operations and as such can be tolerated.

### **14 – ii. Maintenance**

Ease of maintenance actually begins with the development of the plant arrangement and equipment locations by providing sufficient space around each piece of equipment not only for the maintenance of the machinery alone but also for the pipe and the maintenance of the related components. These space allocations should include the pull spaces, lay down spaces, and rotor and tube removal spaces for the dismantling of all pieces of equipment. The engineering of the system P&IDs will indicate the need for maintenance facilities in the form of bypasses and block valves that would permit certain pieces of equipment or components to be worked on while the system is operating, or at least with a minimum of downtime. The designer has to design these facilities into the system and to provide the accessibility necessary to accomplish that maintenance, including the provision for any lifting gear such as cranes, davits, monorails, and hoists.

### **14 – iii. Safety and Accessibility**

Stairs, platforms, ladders, aisles, means-of-egress aisle ways, and minimum headroom allowances designed in accordance with OSHA will provide a safe place to work. It is the responsibility of the piping designer to place equipment, valves, and other piping components in such positions that they do not create hazards. These hazards could include any piping components that presented themselves as “head knockers,” “knee knockers,” or trippers.

The most common cause of these problems is valve stems, and common sense would say to place a valve in a horizontal run of pipe with the stem vertical, wherever possible. When this cannot be done, the designer should ascertain that the stem does not project into an access area and become a hazard. The designer should make every effort to keep such projections out of heights of 4 1/2 to 6 ft (1.5 to 2 m), or specifically at face level.

Steam system valves must not be placed at face level in the horizontal position since a packing gland leak may blow steam into the face of an operator; if this

were a superheated steam leak, the vapor would not be visible. This same principle applies to hazardous and toxic fluids. However, this may be too restrictive, and it is not meant to rule out any perfectly safe arrangement of valves at face level if

- They are outside the limit of a platform.
- They are a part of a manifold of valves, all projecting about the same distance and with adequate access space in front of them.
- It is an isolated valve guarded by an adjacent pipe or structural steel.

The designer should review the layout and determine if there is a need for any platforms which access a remotely located valve or component.

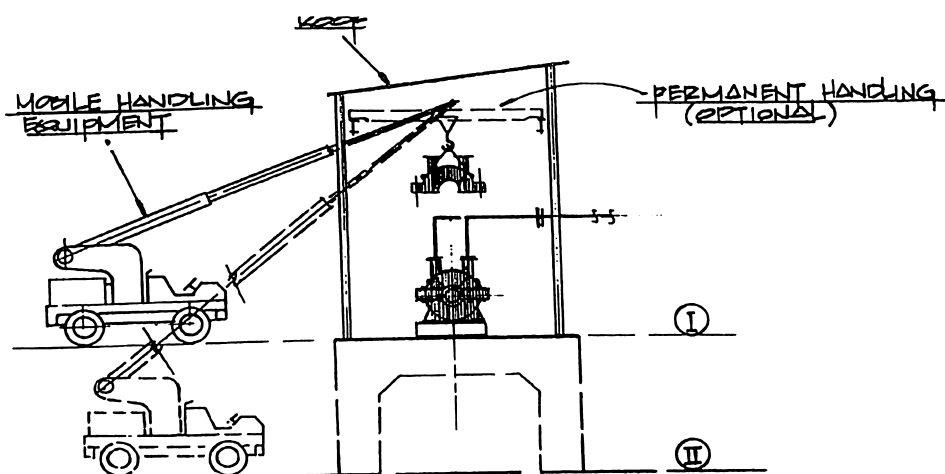


Figure 03 - Compressor Handling

### 15. Interfacing Disciplines and Organizations

Piping design requires coordination and cooperation with all interfacing disciplines including civil, electrical, instrumentation, and construction. Piping arrangements should blend with the layout design of interfacing disciplines. Pipes that require extensive support schemes in lieu of being conveniently located near structural support steel should be avoided. Pipes or electrical trays that twist and turn to avoid one another should be uniformly designed in a coordinated design effort which reduces congestion and reduces TIC. Most piping designs are not completed by a single designer or company, which makes the coordination between designers and different organizations critical. The best way to address this concern is to agree to specific divisions of responsibility in the planning phase of the project.

### 3.13 APPLICATION OF COMPUTER-AIDED DESIGN TO PIPING LAYOUT

The piping industry today is very diverse in its use of computer-aided design. This diversity is shown by the various levels of sophistication of the CAD applications in use by different segments of the industry. Even within the same company, the sophistication of CAD use can vary widely from discipline to discipline, department to department. This diversity ranges from a surprisingly large portion of the industry in which there is little use of CAD to a few who claim to be approaching a paperless office. Between these two extremes, most of the industry appears to be using CAD as computer-aided drafting. In this sense, CAD becomes an electronic pencil, not necessarily a design tool.

### 3.14 STRESS ANALYSIS

After piping materials, design pressure and sizes have been selected, a stress analysis is performed that relates the selected piping system to the piping layout and piping supports.

The analysis ensures that the piping system meets intended service and loading condition requirements while optimizing the layout and support design. The analysis may result in successive reiterations until a balance is struck between stresses and layout efficiency, and stresses and support upon system complexity and the design code.

ASME B31.3 requires the analysis of three stress limits

- Stresses due to sustained loads
- Stresses due to displacement strains
- Stresses due to occasional loads

#### 3.14.1 STRESSES DUE TO SUSTAINED LOADS

The stress analysis for sustained loads includes internal pressure stresses, external pressure stresses and longitudinal stresses. ASME B31.3 considers stresses due to internal and external pressures to be safe if the wall thickness meets the pressure integrity requirements. The sum of the longitudinal stresses in the piping system that result from pressure, weight and any other sustained

loads do not exceed the basic allowable stress at the maximum metal temperature.

$$S_L < S_h$$

Where,  $S_L$  – Longitudinal stress, MPa (psi)  
 $S_h$  – Basic allowable stress at maximum material temperature, MPa (psi)

The internal pressure in piping normally produces stresses in the pipe wall because the pressure forces are offset by pipe wall tension. The exception is pressure transients such as water hammer which add load to pipe supports.

The longitudinal stress from pressure is calculated by

$$S_L = P \cdot D_o / [4 \cdot t]$$

Where,  $D_o$  – Pipeline Outer diameter inch  
 $t$  – Thickness of line pipe in inch  
 $P$  – Pressure (design) at any section Pisa  
 $S_L$  – Longitudinal stress, MPa (psi)

The longitudinal stress due to weight is dependent upon support locations and pipe span. The formula to calculate the pipe stress is

$$S_L = 0.1 \cdot [W \cdot L^2 / n \cdot Z]$$

Where,  $S_L$  – Longitudinal stress, MPa (psi)  
 $W$  – Distributed weight of pipe material, contents and insulation, N/m (lbs/ft)  
 $n$  – Conversion factor,  $10^{-3}$  m/mm (1 ft/12 in)  
 $Z$  – Pipe section modulus,  $\text{mm}^3$  ( $\text{in}^3$ )  
 $L$  – Pipe span, m (ft)

$$Z = 3.14 / 32 \cdot \{ [D_o^4 - D_i^4] / D_o \}$$

Where,  $D_o$  – Pipeline Outer diameter inch  
 $D_i$  – Pipeline inner diameter inch

### 3.14.2 STRESSES DUE TO DISPLACEMENT STRAINS

Constraint of piping displacements resulting from thermal expansion, seismic activities or piping support and terminal movements cause local stress

conditions. These localized conditions can cause failure of piping or supports from fatigue or over-stress, leakage at joints or distortions. To ensure that piping systems have sufficient flexibility to prevent these failures, ASME B31.3 requires that the displacement stress range does not exceed the allowable displacement stress range.

$$S_E < S_A$$

Where,  $S_E$  – Displacement stress range, MPa (psi)  
 $S_A$  – Allowable displacement stress range, MPa (psi)

$$S_A = f * [1.25 * (S_C + S_h) - S_L]$$

Where,  $f$  – Stress reduction factor  
 $S_C$  – Basic allowable stress of minimum material temperature, MPa (psi),  
 $S_h$  – Basic allowable stress at maximum material temperature, MPa (psi)

$$f = 6.0 * [N]^{-0.2} \leq 1$$

Where,  $N$  – Equivalent number of full displacement cycles during the expected service life,  $< 2 \times 10^6$

$$S_E = [S_b^2 + 4S_t^2]^{0.5}$$

Where,  $S_E$  – Displacement stress range, MPa (psi)  
 $S_b$  – Resultant bending stress, MPa (psi)  
 $S_t$  – Torsional stress, MPa (psi)

$$S_b = [(i_i M_i)^2 - (i_o M_o)^2]^{0.5} / (n * Z)$$

Where,  $S_b$  – Resultant bending stress, MPa (psi)  
 $i_i$  – In plane stress intensity factor  
 $M_i$  – In plane bending moment, N-m (lb-ft)  
 $i_o$  – Out plane stress intensity factor  
 $M_o$  – Out plane bending moment, N-m (lb-ft)  
 $n$  – Conversion factor,  $10^{-3}$  m/mm (1 ft/12 in)  
 $Z$  – Pipe section modulus, mm (in)

$$S_t = M_t / [2 * Z * n]$$

- Where,
- $S_t$  – Torsional stress, MPa (psi)
  - $M_t$  – Torsional moment, N-m (lb-ft)
  - $n$  – Conversion factor,  $10^{-3}$  m/mm (1 ft/12 in)
  - $Z$  – Pipe section modulus, mm (in)

A formal flexibility analysis is not required when the new piping system replaces in kind, or without significant change, a system with a successful service record the new piping system can be readily judged adequate by comparison to previously analyzed systems and the new piping system is of uniform size, has 2 or less fixed has no intermediate restraints, and meets the following empirical condition

$$[D_o * Y] / [L - L_s]^2 * K_1$$

- Where,
- $D_o$  – Pipeline Outer diameter inch
  - $L$  – Length of the Pipeline between anchors, m (ft)
  - $Y$  – Resultant of total displacement strains, mm (in)
  - $L_s$  – Straight line distance between anchors, m (ft)
  - $K_1$  – Constant, 208.3 for SI units

### 3.14.3 STRESSES DUE TO OCCASIONAL LOADS

The sum of the longitudinal stresses due to both sustained and occasional loads does not exceed 1.33 times the basic allowable stress at maximum material temperature.

$$S_L = 1.33 * S_h$$

- Where,
- $S_h$  – Basic allowable stress at maximum material temperature, MPa (psi)
  - $S_L$  – Longitudinal stress from sustained and occasional loads, MPa (psi)

The occasional loads that are analyzed include seismic, wind, snow and ice, and dynamic loads. Seismic and wind loads do not have to be considered as acting standards. Stress analysis has been carried out by means of CAESAR II software.



## **4. COMPUTATIONS**

### **4.1 DESIGN BASIS**

Throughput	= 16.68 MSCMD
Length Of pipeline	= 10 Km
Supply Pressure	= 171.39 psia
Supply Temperature	= 27°C
Receiving Terminal Pressure	= 213.35 – 227.57 psia [Minimum]
Design Pressure	= 300 psia = MAOP
Fluid Name	= Propylene Gas

### **GAS COMPOSITION**

<b>Component</b>	<b>Mole %</b>
C <sub>3</sub> H <sub>6</sub>	99.55
C <sub>2</sub> H <sub>6</sub>	0.02
C <sub>3</sub> H <sub>8</sub>	0.43
Total	100

Table 04 – Gas Composition

### **GRADE OF LINE PIPE**

XS

### **DESIGN CALCULATIONS**

#### **4.2 PIPELINE SIZING**

$$\begin{aligned} \text{Pipe Diameter [Di]} &= \{1.44 * 10^{-3} * [Q_b * Z * T_f / P * u]\} ^{0.5} \\ &= \{1.44 * 10^{-3} * [24543695.7 * 0.786 * 540.27 / 298.2635 \\ &\quad * 59.9311]\} ^{0.5} \end{aligned}$$

$$\text{Pipe Diameter [Di]} = 28.9762 \text{ inch}$$

#### **4.3 EROSIONAL VELOCITY**

$$\begin{aligned} \text{Erosional velocity [ue]} &= 100 / [29 * G * P / Z * R * T] ^{0.5} \\ &= 100 / [29 * 0.69 * 229.2362 / 0.786 * 10.73 * 540.27] ^{0.5} \end{aligned}$$

$$\text{Erosional velocity [ue]} = 99.5810 \text{ ft/sec}$$

The recommended value for the gas velocity for the gas pipelines is 40 – 50 % of the Erosional velocity or for 50- 60 % of the Erosional velocity for non major mainlines [i.e. 15-17 m/s]

$$\begin{aligned}\text{Operating velocity [u]} &= \text{Erosional velocity [ue]} * 0.6 \\ &= 99.5817 * 0.6\end{aligned}$$

$$\text{Operating velocity [u]} = 59.7486 \text{ ft/sec}$$

#### 4.4 OPERATING VELOCITY

$$\begin{aligned}\text{Operating velocity [u]} &= 1.44 * 10^{-3} * [Q_b * Z * T_f / P * D_i^2] \\ &= 1.44 * 10^{-3} * [24543695.7 * 0.786 * 540.27 / 298.2635 \\ &\quad * 28.9762^2]\end{aligned}$$

$$\text{Operating velocity [u]} = 59.9311 \text{ ft/sec}$$

#### 4.5 REYNOLDS NUMBER

The Reynolds number can be used to check the flow regime of the gas transmission pipeline

$$\begin{aligned}Re &= [45 * Q_b * G] / D_i \\ &= [45 * 2.454369 * 10^7 * 0.69] / 28.9765\end{aligned}$$

$$Re = 26299987$$

The calculated value of the pipeline is much more than 4000 so the flow is fully turbulent.

#### 4.6 TRANSMISSION FACTOR

The transmission factor for fully turbulent flow is given by Nikuradse equation as

$$[1/f]^{0.5} = 4 * \log [3.7 * D_i / Ke]$$

$$[1/f]^{0.5} = 4 * \log [3.7 * 28.9765 / 0.0007]$$

$$[1/f]^{0.5} = 20.74$$

#### 4.7 PRESSURE CALCULATION

Panhandle A Equation

$$P_1^2 - P_2^2 = K_1 Q_b^n$$

$$R = 2.552 * 10^{-4} * T_f * Z_{avg} * [G^{0.855} / D_i^{4.856}]$$

$$n = 1.855$$

$$K_1 = R * L$$

$$K_1 = 2.552 * 10^{-4} * 540.27 * 0.786 * [0.69^{0.855} / 28.9763^{4.856}] * 32808.34$$

$$\begin{aligned} &= 0.000262 \\ 298.2635^2 - P_2^2 &= 0.000262 * 24540.45^{4.856} \\ P_2^2 &= 52549.2178 \\ P_2 &= 229.2361 \text{ psia} \end{aligned}$$

#### **4.8 COMPRESSOR CALCUATIONS**

##### **4.8.1 COMPRESSION RATIO**

Generally the compression ratio is limited to 1.2 to 1.8 for centrifugal compressors

$$\begin{aligned} \text{Compression Ratio} &= \text{Discharge Pressure/Suction Pressure} \\ &= 298.26/171.39 \\ &= 1.74 \end{aligned}$$

##### **4.8.2 ADIABATIC EFFICIENCY**

$$\begin{aligned} \text{Adiabatic Efficiency } [\eta_a] &= (T_1/ T_2 - T_1)*(Z_1/Z_2/)*\{(P_2/P_1) ^ (\gamma - 1/ \gamma)-1\} \\ &= (540.27/ 709.47 - 540.27)*(0.786/0.72)* \\ &\quad \{(298.26/171.39) ^ (1.371 - 1/ 1.371)-1\} \\ \eta_a &= 0.7982 \end{aligned}$$

##### **4.8.3 HORSEPOWER REQUIRED**

From the energy input to the gas, following equation is used to calculate the compressor HP

$$\begin{aligned} \text{HP} &= 4.0639*(\gamma/ \gamma - 1)*Q*(Z_1+Z_2/2)*T_1*(1/ \eta_a)*\{(P_2/P_1) ^ (\gamma - 1/ \gamma)-1\} \\ &= 4.0639*(1.371/ 1.371 - 1)*16.68*(0.786+0.72/2)*300*(1/ .7982)* \\ &\quad \{(298.26/171.39) ^ (1.371 - 1/ 1.371)-1\} \end{aligned}$$

$$\text{HP} = 15978.76 \text{ kW}$$

##### **4.8.4 BRAKE HORSEPOWER (BHP)**

Brake Horsepower (BHP) required may be calculated as follows

$$\begin{aligned} \text{BHP} &= \text{HP}/\eta_m \\ &= 15978.76/0.98 \end{aligned}$$

$$\text{BHP} = 16819.75 \text{ kW}$$

#### **4.8.5 OVERALL EFFICIENCY**

$$\begin{aligned}\text{Overall efficiency } [\eta_o] &= \eta_a * \eta_m \\ &= 0.7982 * 0.98 \\ \eta_o &= 0.7822\end{aligned}$$

#### **4.9 STRENGTH OF PIPE**

##### **4.9.1 HOOP STRESS**

$$\begin{aligned}\text{Hoop stress } S_H &= [P * D] / [2 * t] \\ &= [300 * 30] / [2 * 0.511] \\ S_H &= 8806.26 \text{ psia}\end{aligned}$$

##### **4.9.2 LONGITUDINAL STRESS**

$$\begin{aligned}\text{Longitudinal stress } S_L &= [P * D] / [4 * t] \\ &= [300 * 30] / [4 * 0.511] \\ S_L &= 4403.13 \text{ psia}\end{aligned}$$

#### **4.10 THICKNESS CALCULATION**

Considering the Location Class 2, Electric resistance welded pipe, and the temperature below 121 °C

$$F = 0.60$$

$$E = 1.00$$

$$T = 1.00$$

**Case:** 30 inch, XS Grade pipe

$$\begin{aligned}\text{Thickness } [t] &= [P * D] / [2 * S * F * E * T] \\ &= [300 * 30] / [2 * 14600 * 0.60 * 1.00 * 1.00]\end{aligned}$$

$$\text{Thickness } [t] = 0.511 \text{ inch} - \text{Calculated}$$

**4.11 PROCESS & INSTRUMENTATION DIAGRAM LEGEND**

**MISCELLANEOUS ABBREVIATIONS**

- SYMBOLS NOTE 2**
- AA - AIR
  - AB - AIRBORNE
  - AC - AIR CONDITIONING
  - AD - AIR DUCT
  - AE - AIR EXHAUST
  - AF - AIR FLOW
  - AG - AIR GATE
  - AH - AIR HEATER
  - AI - AIR INLET
  - AL - AIR LINE
  - AM - AIR METER
  - AN - AIR NIPPLE
  - AO - AIR OUTLET
  - AP - AIR PUMP
  - AQ - AIR QUALITY
  - AR - AIR REGISTER
  - AS - AIR SUPPLY
  - AT - AIR TREATMENT
  - AV - AIR VALVE
  - AW - AIR WASH
  - AX - AIR EXHAUST
  - AY - AIR YARD
  - AZ - AIR ZONE
  - BA - BATTERY
  - BB - BATTERY BANK
  - BC - BATTERY CHARGE
  - BD - BATTERY DISCHARGE
  - BE - BATTERY EQUALIZER
  - BF - BATTERY FILL
  - BG - BATTERY GROUND
  - BH - BATTERY HEATER
  - BI - BATTERY INLET
  - BJ - BATTERY JUNCTION
  - BK - BATTERY KITCHEN
  - BL - BATTERY LINE
  - BM - BATTERY METER
  - BN - BATTERY NIPPLE
  - BO - BATTERY OUTLET
  - BP - BATTERY PUMP
  - BQ - BATTERY QUALITY
  - BR - BATTERY REGISTER
  - BS - BATTERY SUPPLY
  - BT - BATTERY TREATMENT
  - BV - BATTERY VALVE
  - BW - BATTERY WASH
  - BX - BATTERY EXHAUST
  - BY - BATTERY YARD
  - BZ - BATTERY ZONE
  - CA - CABLE
  - CB - CABLE BANK
  - CC - CABLE CHARGE
  - CD - CABLE DISCHARGE
  - CE - CABLE EQUALIZER
  - CF - CABLE FILL
  - CG - CABLE GROUND
  - CH - CABLE HEATER
  - CI - CABLE INLET
  - CJ - CABLE JUNCTION
  - CK - CABLE KITCHEN
  - CL - CABLE LINE
  - CM - CABLE METER
  - CN - CABLE NIPPLE
  - CO - CABLE OUTLET
  - CP - CABLE PUMP
  - CQ - CABLE QUALITY
  - CR - CABLE REGISTER
  - CS - CABLE SUPPLY
  - CT - CABLE TREATMENT
  - CV - CABLE VALVE
  - CW - CABLE WASH
  - CX - CABLE EXHAUST
  - CY - CABLE YARD
  - CZ - CABLE ZONE
  - DA - DAM
  - DB - DAM BANK
  - DC - DAM CHARGE
  - DD - DAM DISCHARGE
  - DE - DAM EQUALIZER
  - DF - DAM FILL
  - DG - DAM GROUND
  - DH - DAM HEATER
  - DI - DAM INLET
  - DJ - DAM JUNCTION
  - DK - DAM KITCHEN
  - DL - DAM LINE
  - DM - DAM METER
  - DN - DAM NIPPLE
  - DO - DAM OUTLET
  - DP - DAM PUMP
  - DQ - DAM QUALITY
  - DR - DAM REGISTER
  - DS - DAM SUPPLY
  - DT - DAM TREATMENT
  - DV - DAM VALVE
  - DW - DAM WASH
  - DX - DAM EXHAUST
  - DY - DAM YARD
  - DZ - DAM ZONE
  - EA - EARTH
  - EB - EARTH BANK
  - EC - EARTH CHARGE
  - ED - EARTH DISCHARGE
  - EE - EARTH EQUALIZER
  - EF - EARTH FILL
  - EG - EARTH GROUND
  - EH - EARTH HEATER
  - EI - EARTH INLET
  - EJ - EARTH JUNCTION
  - EK - EARTH KITCHEN
  - EL - EARTH LINE
  - EM - EARTH METER
  - EN - EARTH NIPPLE
  - EO - EARTH OUTLET
  - EP - EARTH PUMP
  - EQ - EARTH QUALITY
  - ER - EARTH REGISTER
  - ES - EARTH SUPPLY
  - ET - EARTH TREATMENT
  - EV - EARTH VALVE
  - EW - EARTH WASH
  - EX - EARTH EXHAUST
  - EY - EARTH YARD
  - EZ - EARTH ZONE
  - FA - FAN
  - FB - FAN BANK
  - FC - FAN CHARGE
  - FD - FAN DISCHARGE
  - FE - FAN EQUALIZER
  - FF - FAN FILL
  - FG - FAN GROUND
  - FH - FAN HEATER
  - FI - FAN INLET
  - FJ - FAN JUNCTION
  - FK - FAN KITCHEN
  - FL - FAN LINE
  - FM - FAN METER
  - FN - FAN NIPPLE
  - FO - FAN OUTLET
  - FP - FAN PUMP
  - FQ - FAN QUALITY
  - FR - FAN REGISTER
  - FS - FAN SUPPLY
  - FT - FAN TREATMENT
  - FV - FAN VALVE
  - FW - FAN WASH
  - FX - FAN EXHAUST
  - FY - FAN YARD
  - FZ - FAN ZONE
  - GA - GAS
  - GB - GAS BANK
  - GC - GAS CHARGE
  - GD - GAS DISCHARGE
  - GE - GAS EQUALIZER
  - GF - GAS FILL
  - GG - GAS GROUND
  - GH - GAS HEATER
  - GI - GAS INLET
  - GJ - GAS JUNCTION
  - GK - GAS KITCHEN
  - GL - GAS LINE
  - GM - GAS METER
  - GN - GAS NIPPLE
  - GO - GAS OUTLET
  - GP - GAS PUMP
  - GQ - GAS QUALITY
  - GR - GAS REGISTER
  - GS - GAS SUPPLY
  - GT - GAS TREATMENT
  - GV - GAS VALVE
  - GW - GAS WASH
  - GX - GAS EXHAUST
  - GY - GAS YARD
  - GZ - GAS ZONE
  - HA - HAZARDOUS
  - HB - HAZARDOUS BANK
  - HC - HAZARDOUS CHARGE
  - HD - HAZARDOUS DISCHARGE
  - HE - HAZARDOUS EQUALIZER
  - HF - HAZARDOUS FILL
  - HG - HAZARDOUS GROUND
  - HH - HAZARDOUS HEATER
  - HI - HAZARDOUS INLET
  - HJ - HAZARDOUS JUNCTION
  - HK - HAZARDOUS KITCHEN
  - HL - HAZARDOUS LINE
  - HM - HAZARDOUS METER
  - HN - HAZARDOUS NIPPLE
  - HO - HAZARDOUS OUTLET
  - HP - HAZARDOUS PUMP
  - HQ - HAZARDOUS QUALITY
  - HR - HAZARDOUS REGISTER
  - HS - HAZARDOUS SUPPLY
  - HT - HAZARDOUS TREATMENT
  - HV - HAZARDOUS VALVE
  - HW - HAZARDOUS WASH
  - HX - HAZARDOUS EXHAUST
  - HY - HAZARDOUS YARD
  - HZ - HAZARDOUS ZONE
  - IA - INSULATION
  - IB - INSULATION BANK
  - IC - INSULATION CHARGE
  - ID - INSULATION DISCHARGE
  - IE - INSULATION EQUALIZER
  - IF - INSULATION FILL
  - IG - INSULATION GROUND
  - IH - INSULATION HEATER
  - II - INSULATION INLET
  - IJ - INSULATION JUNCTION
  - IK - INSULATION KITCHEN
  - IL - INSULATION LINE
  - IM - INSULATION METER
  - IN - INSULATION NIPPLE
  - IO - INSULATION OUTLET
  - IP - INSULATION PUMP
  - IQ - INSULATION QUALITY
  - IR - INSULATION REGISTER
  - IS - INSULATION SUPPLY
  - IT - INSULATION TREATMENT
  - IV - INSULATION VALVE
  - IW - INSULATION WASH
  - IX - INSULATION EXHAUST
  - IY - INSULATION YARD
  - IZ - INSULATION ZONE
  - JA - JUNCTION
  - JB - JUNCTION BANK
  - JC - JUNCTION CHARGE
  - JD - JUNCTION DISCHARGE
  - JE - JUNCTION EQUALIZER
  - JF - JUNCTION FILL
  - JG - JUNCTION GROUND
  - JH - JUNCTION HEATER
  - JI - JUNCTION INLET
  - JJ - JUNCTION JUNCTION
  - JK - JUNCTION KITCHEN
  - JL - JUNCTION LINE
  - JM - JUNCTION METER
  - JN - JUNCTION NIPPLE
  - JO - JUNCTION OUTLET
  - JP - JUNCTION PUMP
  - JQ - JUNCTION QUALITY
  - JR - JUNCTION REGISTER
  - JS - JUNCTION SUPPLY
  - JT - JUNCTION TREATMENT
  - JV - JUNCTION VALVE
  - JW - JUNCTION WASH
  - JX - JUNCTION EXHAUST
  - JY - JUNCTION YARD
  - JZ - JUNCTION ZONE
  - KA - KEYS
  - KB - KEYS BANK
  - KC - KEYS CHARGE
  - KD - KEYS DISCHARGE
  - KE - KEYS EQUALIZER
  - KF - KEYS FILL
  - KG - KEYS GROUND
  - KH - KEYS HEATER
  - KI - KEYS INLET
  - KJ - KEYS JUNCTION
  - KK - KEYS KITCHEN
  - KL - KEYS LINE
  - KM - KEYS METER
  - KN - KEYS NIPPLE
  - KO - KEYS OUTLET
  - KP - KEYS PUMP
  - KQ - KEYS QUALITY
  - KR - KEYS REGISTER
  - KS - KEYS SUPPLY
  - KT - KEYS TREATMENT
  - KV - KEYS VALVE
  - KW - KEYS WASH
  - KX - KEYS EXHAUST
  - KY - KEYS YARD
  - KZ - KEYS ZONE
  - LA - LAMP
  - LB - LAMP BANK
  - LC - LAMP CHARGE
  - LD - LAMP DISCHARGE
  - LE - LAMP EQUALIZER
  - LF - LAMP FILL
  - LG - LAMP GROUND
  - LH - LAMP HEATER
  - LI - LAMP INLET
  - LJ - LAMP JUNCTION
  - LK - LAMP KITCHEN
  - LL - LAMP LINE
  - LM - LAMP METER
  - LN - LAMP NIPPLE
  - LO - LAMP OUTLET
  - LP - LAMP PUMP
  - LQ - LAMP QUALITY
  - LR - LAMP REGISTER
  - LS - LAMP SUPPLY
  - LT - LAMP TREATMENT
  - LV - LAMP VALVE
  - LW - LAMP WASH
  - LX - LAMP EXHAUST
  - LY - LAMP YARD
  - LZ - LAMP ZONE
  - MA - METER
  - MB - METER BANK
  - MC - METER CHARGE
  - MD - METER DISCHARGE
  - ME - METER EQUALIZER
  - MF - METER FILL
  - MG - METER GROUND
  - MH - METER HEATER
  - MI - METER INLET
  - MJ - METER JUNCTION
  - MK - METER KITCHEN
  - ML - METER LINE
  - MM - METER METER
  - MN - METER NIPPLE
  - MO - METER OUTLET
  - MP - METER PUMP
  - MQ - METER QUALITY
  - MR - METER REGISTER
  - MS - METER SUPPLY
  - MT - METER TREATMENT
  - MV - METER VALVE
  - MW - METER WASH
  - MX - METER EXHAUST
  - MY - METER YARD
  - MZ - METER ZONE
  - NA - NIPPLE
  - NB - NIPPLE BANK
  - NC - NIPPLE CHARGE
  - ND - NIPPLE DISCHARGE
  - NE - NIPPLE EQUALIZER
  - NF - NIPPLE FILL
  - NG - NIPPLE GROUND
  - NH - NIPPLE HEATER
  - NI - NIPPLE INLET
  - NJ - NIPPLE JUNCTION
  - NK - NIPPLE KITCHEN
  - NL - NIPPLE LINE
  - NM - NIPPLE METER
  - NO - NIPPLE NIPPLE
  - NP - NIPPLE OUTLET
  - NQ - NIPPLE QUALITY
  - NR - NIPPLE REGISTER
  - NS - NIPPLE SUPPLY
  - NT - NIPPLE TREATMENT
  - NV - NIPPLE VALVE
  - NW - NIPPLE WASH
  - NX - NIPPLE EXHAUST
  - NY - NIPPLE YARD
  - NZ - NIPPLE ZONE
  - OA - OIL
  - OB - OIL BANK
  - OC - OIL CHARGE
  - OD - OIL DISCHARGE
  - OE - OIL EQUALIZER
  - OF - OIL FILL
  - OG - OIL GROUND
  - OH - OIL HEATER
  - OI - OIL INLET
  - OJ - OIL JUNCTION
  - OK - OIL KITCHEN
  - OL - OIL LINE
  - OM - OIL METER
  - ON - OIL NIPPLE
  - OO - OIL OUTLET
  - OP - OIL PUMP
  - OQ - OIL QUALITY
  - OR - OIL REGISTER
  - OS - OIL SUPPLY
  - OT - OIL TREATMENT
  - OV - OIL VALVE
  - OW - OIL WASH
  - OX - OIL EXHAUST
  - OY - OIL YARD
  - OZ - OIL ZONE
  - PA - PUMP
  - PB - PUMP BANK
  - PC - PUMP CHARGE
  - PD - PUMP DISCHARGE
  - PE - PUMP EQUALIZER
  - PF - PUMP FILL
  - PG - PUMP GROUND
  - PH - PUMP HEATER
  - PI - PUMP INLET
  - PJ - PUMP JUNCTION
  - PK - PUMP KITCHEN
  - PL - PUMP LINE
  - PM - PUMP METER
  - PN - PUMP NIPPLE
  - PO - PUMP OUTLET
  - PP - PUMP PUMP
  - PQ - PUMP QUALITY
  - PR - PUMP REGISTER
  - PS - PUMP SUPPLY
  - PT - PUMP TREATMENT
  - PV - PUMP VALVE
  - PW - PUMP WASH
  - PX - PUMP EXHAUST
  - PY - PUMP YARD
  - PZ - PUMP ZONE
  - QA - QUALITY
  - QB - QUALITY BANK
  - QC - QUALITY CHARGE
  - QD - QUALITY DISCHARGE
  - QE - QUALITY EQUALIZER
  - QF - QUALITY FILL
  - QG - QUALITY GROUND
  - QH - QUALITY HEATER
  - QI - QUALITY INLET
  - QJ - QUALITY JUNCTION
  - QK - QUALITY KITCHEN
  - QL - QUALITY LINE
  - QM - QUALITY METER
  - QN - QUALITY NIPPLE
  - QO - QUALITY OUTLET
  - QP - QUALITY PUMP
  - QQ - QUALITY QUALITY
  - QR - QUALITY REGISTER
  - QS - QUALITY SUPPLY
  - QT - QUALITY TREATMENT
  - QV - QUALITY VALVE
  - QW - QUALITY WASH
  - QX - QUALITY EXHAUST
  - QY - QUALITY YARD
  - QZ - QUALITY ZONE
  - RA - REGISTER
  - RB - REGISTER BANK
  - RC - REGISTER CHARGE
  - RD - REGISTER DISCHARGE
  - RE - REGISTER EQUALIZER
  - RF - REGISTER FILL
  - RG - REGISTER GROUND
  - RH - REGISTER HEATER
  - RI - REGISTER INLET
  - RJ - REGISTER JUNCTION
  - RK - REGISTER KITCHEN
  - RL - REGISTER LINE
  - RM - REGISTER METER
  - RN - REGISTER NIPPLE
  - RO - REGISTER OUTLET
  - RP - REGISTER PUMP
  - RQ - REGISTER QUALITY
  - RR - REGISTER REGISTER
  - RS - REGISTER SUPPLY
  - RT - REGISTER TREATMENT
  - RV - REGISTER VALVE
  - RW - REGISTER WASH
  - RX - REGISTER EXHAUST
  - RY - REGISTER YARD
  - RZ - REGISTER ZONE
  - SA - SIGNAL
  - SB - SIGNAL BANK
  - SC - SIGNAL CHARGE
  - SD - SIGNAL DISCHARGE
  - SE - SIGNAL EQUALIZER
  - SF - SIGNAL FILL
  - SG - SIGNAL GROUND
  - SH - SIGNAL HEATER
  - SI - SIGNAL INLET
  - SJ - SIGNAL JUNCTION
  - SK - SIGNAL KITCHEN
  - SL - SIGNAL LINE
  - SM - SIGNAL METER
  - SN - SIGNAL NIPPLE
  - SO - SIGNAL OUTLET
  - SP - SIGNAL PUMP
  - SQ - SIGNAL QUALITY
  - SR - SIGNAL REGISTER
  - SS - SIGNAL SUPPLY
  - ST - SIGNAL TREATMENT
  - SV - SIGNAL VALVE
  - SW - SIGNAL WASH
  - SX - SIGNAL EXHAUST
  - SY - SIGNAL YARD
  - SZ - SIGNAL ZONE
  - TA - TANK
  - TB - TANK BANK
  - TC - TANK CHARGE
  - TD - TANK DISCHARGE
  - TE - TANK EQUALIZER
  - TF - TANK FILL
  - TG - TANK GROUND
  - TH - TANK HEATER
  - TI - TANK INLET
  - TJ - TANK JUNCTION
  - TK - TANK KITCHEN
  - TL - TANK LINE
  - TM - TANK METER
  - TN - TANK NIPPLE
  - TO - TANK OUTLET
  - TP - TANK PUMP
  - TQ - TANK QUALITY
  - TR - TANK REGISTER
  - TS - TANK SUPPLY
  - TT - TANK TREATMENT
  - TV - TANK VALVE
  - TW - TANK WASH
  - TX - TANK EXHAUST
  - TY - TANK YARD
  - TZ - TANK ZONE
  - UA - UNDERGROUND
  - UB - UNDERGROUND BANK
  - UC - UNDERGROUND CHARGE
  - UD - UNDERGROUND DISCHARGE
  - UE - UNDERGROUND EQUALIZER
  - UF - UNDERGROUND FILL
  - UG - UNDERGROUND GROUND
  - UH - UNDERGROUND HEATER
  - UI - UNDERGROUND INLET
  - UJ - UNDERGROUND JUNCTION
  - UK - UNDERGROUND KITCHEN
  - UL - UNDERGROUND LINE
  - UM - UNDERGROUND METER
  - UN - UNDERGROUND NIPPLE
  - UO - UNDERGROUND OUTLET
  - UP - UNDERGROUND PUMP
  - UQ - UNDERGROUND QUALITY
  - UR - UNDERGROUND REGISTER
  - US - UNDERGROUND SUPPLY
  - UT - UNDERGROUND TREATMENT
  - UV - UNDERGROUND VALVE
  - UW - UNDERGROUND WASH
  - UX - UNDERGROUND EXHAUST
  - UY - UNDERGROUND YARD
  - UZ - UNDERGROUND ZONE
  - VA - VALVE
  - VB - VALVE BANK
  - VC - VALVE CHARGE
  - VD - VALVE DISCHARGE
  - VE - VALVE EQUALIZER
  - VF - VALVE FILL
  - VG - VALVE GROUND
  - VH - VALVE HEATER
  - VI - VALVE INLET
  - VJ - VALVE JUNCTION
  - VK - VALVE KITCHEN
  - VL - VALVE LINE
  - VM - VALVE METER
  - VN - VALVE NIPPLE
  - VO - VALVE OUTLET
  - VP - VALVE PUMP
  - VQ - VALVE QUALITY
  - VR - VALVE REGISTER
  - VS - VALVE SUPPLY
  - VT - VALVE TREATMENT
  - VV - VALVE VALVE
  - VW - VALVE WASH
  - VX - VALVE EXHAUST
  - VY - VALVE YARD
  - VZ - VALVE ZONE
  - WA - WATER
  - WB - WATER BANK
  - WC - WATER CHARGE
  - WD - WATER DISCHARGE
  - WE - WATER EQUALIZER
  - WF - WATER FILL
  - WG - WATER GROUND
  - WH - WATER HEATER
  - WI - WATER INLET
  - WJ - WATER JUNCTION
  - WK - WATER KITCHEN
  - WL - WATER LINE
  - WM - WATER METER
  - WN - WATER NIPPLE
  - WO - WATER OUTLET
  - WP - WATER PUMP
  - WQ - WATER QUALITY
  - WR - WATER REGISTER
  - WS - WATER SUPPLY
  - WT - WATER TREATMENT
  - WV - WATER VALVE
  - WW - WATER WASH
  - WX - WATER EXHAUST
  - WY - WATER YARD
  - WZ - WATER ZONE
  - XA - EXHAUST
  - XB - EXHAUST BANK
  - XC - EXHAUST CHARGE
  - XD - EXHAUST DISCHARGE
  - XE - EXHAUST EQUALIZER
  - XF - EXHAUST FILL
  - XG - EXHAUST GROUND
  - XH - EXHAUST HEATER
  - XI - EXHAUST INLET
  - XJ - EXHAUST JUNCTION
  - XK - EXHAUST KITCHEN
  - XL - EXHAUST LINE
  - XM - EXHAUST METER
  - XN - EXHAUST NIPPLE
  - XO - EXHAUST OUTLET
  - XP - EXHAUST PUMP
  - XQ - EXHAUST QUALITY
  - XR - EXHAUST REGISTER
  - XS - EXHAUST SUPPLY
  - XT - EXHAUST TREATMENT
  - XV - EXHAUST VALVE
  - XW - EXHAUST WASH
  - XX - EXHAUST EXHAUST
  - XY - EXHAUST YARD
  - XZ - EXHAUST ZONE
  - YA - YARD
  - YB - YARD BANK
  - YC - YARD CHARGE
  - YD - YARD DISCHARGE
  - YE - YARD EQUALIZER
  - YF - YARD FILL
  - YG - YARD GROUND
  - YH - YARD HEATER
  - YI - YARD INLET
  - YJ - YARD JUNCTION
  - YK - YARD KITCHEN
  - YL - YARD LINE
  - YM - YARD METER
  - YN - YARD NIPPLE
  - YO - YARD OUTLET
  - YP - YARD PUMP
  - YQ - YARD QUALITY
  - YR - YARD REGISTER
  - YS - YARD SUPPLY
  - YT - YARD TREATMENT
  - YV - YARD VALVE
  - YW - YARD WASH
  - YX - YARD EXHAUST
  - YY - YARD YARD
  - YZ - YARD ZONE
  - ZA - ZONE
  - ZB - ZONE BANK
  - ZC - ZONE CHARGE
  - ZD - ZONE DISCHARGE
  - ZE - ZONE EQUALIZER
  - ZF - ZONE FILL
  - ZG - ZONE GROUND
  - ZH - ZONE HEATER
  - ZI - ZONE INLET
  - ZJ - ZONE JUNCTION
  - ZK - ZONE KITCHEN
  - ZL - ZONE LINE
  - ZM - ZONE METER
  - ZN - ZONE NIPPLE
  - ZO - ZONE OUTLET
  - ZP - ZONE PUMP
  - ZQ - ZONE QUALITY
  - ZR - ZONE REGISTER
  - ZS - ZONE SUPPLY
  - ZT - ZONE TREATMENT
  - ZV - ZONE VALVE
  - ZW - ZONE WASH
  - ZX - ZONE EXHAUST
  - ZY - ZONE YARD
  - ZZ - ZONE ZONE

**PIPELINE IDENTIFICATION**

- PIPELINE IDENTIFICATION**
- A-XXXX-YYYYZ-XXXXXX-YY
- XXXX - ISOLATION TYPE
  - YYYY - PIPE CLASS
  - ZZ - SERVICE NUMBER
  - XXXXXX - DIST NUMBER
  - YY - LINE SERVICE IDENTIFICATION
  - USE SEE IN NOTES

**EQUIPMENT IDENTIFICATION**

- EQUIPMENT IDENTIFICATION**
- PPPP-XXXX-YYZ
- PPPP - FOR MULTIPLE PIPES SHOWN
  - XXXX - SERVICE NUMBER
  - YYZ - FIRST PART OF SECTION NUMBER
  - ZZ - DIST NUMBER
  - YY - PROJECT NUMBER

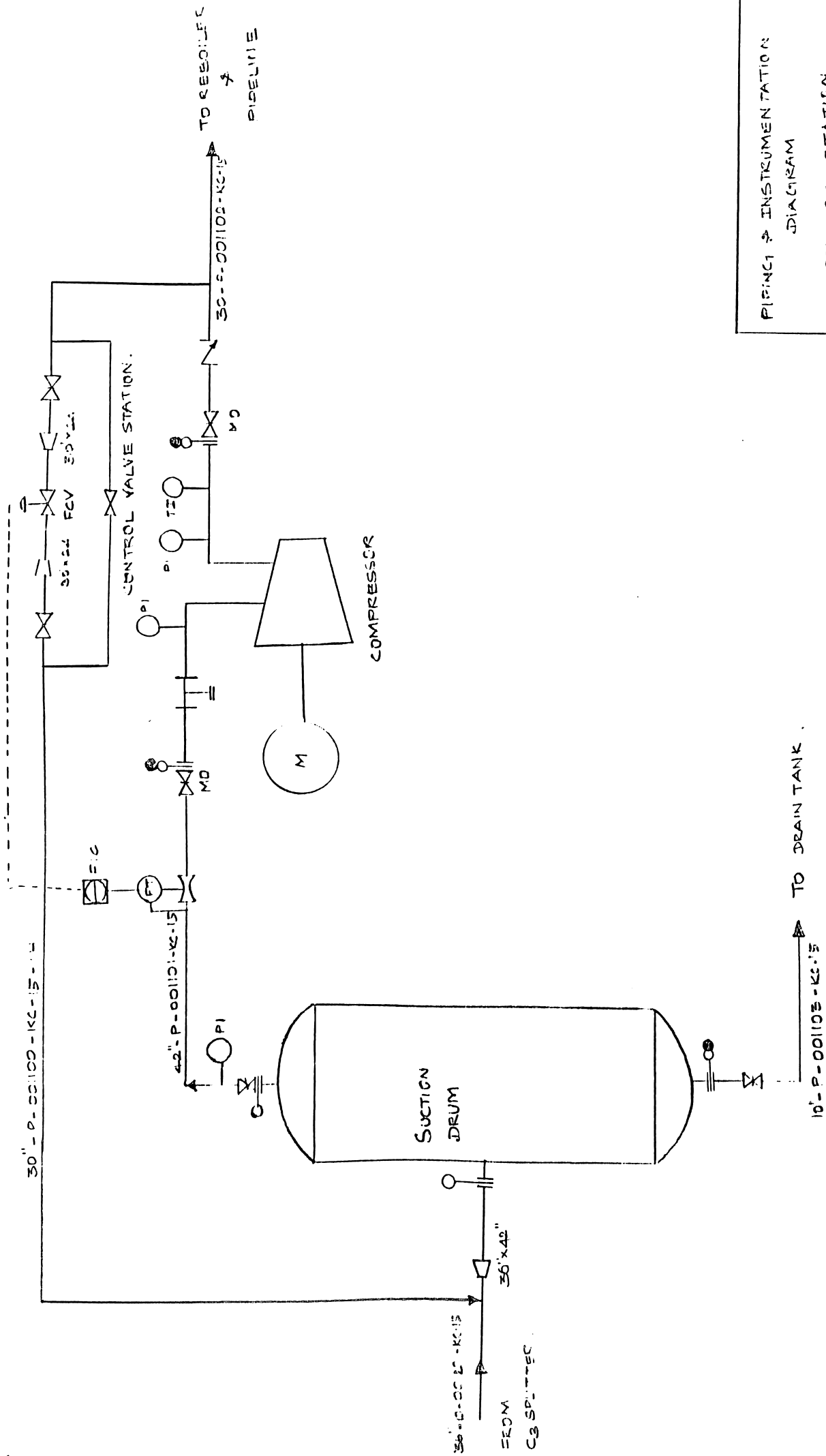
**INSULATION ABBREVIATIONS**

- INSULATION ABBREVIATIONS**
- IC - INSULATION
  - IB - INSULATION BANK
  - IC - INSULATION CHARGE
  - ID - INSULATION DISCHARGE
  - IE - INSULATION EQUALIZER
  - IF - INSULATION FILL
  - IG - INSULATION GROUND
  - IH - INSULATION HEATER
  - II - INSULATION INLET
  - IJ - INSULATION JUNCTION
  - IK - INSULATION KITCHEN
  - IL - INSULATION LINE
  - IM - INSULATION METER
  - IN - INSULATION NIPPLE
  - IO - INSULATION OUTLET
  - IP - INSULATION PUMP
  - IQ - INSULATION QUALITY
  - IR - INSULATION REGISTER
  - IS - INSULATION SUPPLY
  - IT - INSULATION TREATMENT
  - IV - INSULATION VALVE
  - IW - INSULATION WASH
  - IX - INSULATION EXHAUST
  - IY - INSULATION YARD
  - IZ - INSULATION ZONE

**MISCELLANEOUS ABBREVIATIONS**

- MISCELLANEOUS ABBREVIATIONS**
- AA - AIR
  - AB - AIRBORNE
  - AC - AIR CONDITIONING
  - AD - AIR DUCT
  - AE - AIR EXHAUST
  - AF - AIR FLOW
  - AG - AIR GATE
  - AH - AIR HEATER
  - AI - AIR INLET
  - AJ - AIR JUNCTION
  - AK - AIR KITCHEN
  - AL - AIR LINE
  - AM - AIR METER
  - AN - AIR NIPPLE
  - AO - AIR OUTLET
  - AP - AIR PUMP
  - AQ - AIR QUALITY
  - AR - AIR REGISTER
  - AS - AIR SUPPLY
  - AT - AIR TREATMENT
  - AV - AIR VALVE
  - AW - AIR WASH
  - AX - AIR EXHAUST
  - AY - AIR YARD
  - AZ - AIR ZONE
  - BA - BATTERY
  - BB - BATTERY BANK
  - BC - BATTERY CHARGE
  - BD - BATTERY DISCHARGE
  - BE - BATTERY EQUALIZER
  - BF - BATTERY FILL
  - BG - BATTERY GROUND
  - BH - BATTERY HEATER
  - BI - BATTERY INLET
  - BJ - BATTERY JUNCTION
  - BK - BATTERY KITCHEN
  - BL - BATTERY LINE
  - BM - BATTERY METER
  - BN - BATTERY NIPPLE
  - BO - BATTERY OUTLET
  - BP - BATTERY PUMP
  - BQ - BATTERY QUALITY
  - BR - BATTERY REGISTER
  - BS - BATTERY SUPPLY
  - BT - BATTERY TREATMENT
  - BV - BATTERY VALVE
  - BW - BATTERY WASH
  - BX - BATTERY EXHAUST
  - BY - BATTERY YARD
  - BZ - BATTERY ZONE
  - CA - CABLE
  - CB - CABLE BANK
  - CC - CABLE CHARGE
  - CD - CABLE DISCHARGE
  - CE - CABLE EQUALIZER
  - CF - CABLE FILL
  - CG - CABLE GROUND
  - CH - CABLE HEATER
  - CI - CABLE INLET
  - CJ - CABLE JUNCTION
  - CK - CABLE KITCHEN
  - CL - CABLE LINE
  - CM - CABLE METER
  - CN - CABLE NIPPLE
  - CO - CABLE OUTLET
  - CP - CABLE PUMP
  - CQ - CABLE QUALITY
  - CR - CABLE REGISTER
  - CS - CABLE SUPPLY
  - CT - CABLE TREATMENT
  - CV - CABLE VALVE
  - CW - CABLE WASH
  - CX - CABLE EXHAUST
  - CY - CABLE YARD
  - CZ - CABLE ZONE
  - DA - DAM
  - DB - DAM BANK
  - DC - DAM CHARGE
  - DD - DAM DISCHARGE
  - DE - DAM EQUALIZER
  - DF - DAM FILL
  - DG - DAM GROUND
  - DH - DAM HEATER
  - DI - DAM INLET
  - DJ - DAM JUNCTION
  - DK - DAM KITCHEN
  - DL - DAM LINE
  - DM - DAM METER
  - DN - DAM NIPPLE
  - DO - DAM OUTLET
  - DP - DAM PUMP
  - DQ - DAM QUALITY
  - DR - DAM REGISTER
  - DS - DAM SUPPLY
  - DT - DAM TREATMENT
  - DV - DAM VALVE
  - DW - DAM WASH
  - DX - DAM EXHAUST
  - DY - DAM YARD
  - DZ - DAM ZONE
  - EA - EARTH
  - EB - EARTH BANK
  - EC - EARTH CHARGE
  - ED - EARTH DISCHARGE
  - EE - EARTH EQUALIZER
  - EF - EARTH FILL
  - EG - EARTH GROUND
  - EH - EARTH HEATER
  - EI - EARTH INLET
  - EJ - EARTH JUNCTION
  - EK - EARTH KITCHEN
  - EL - EARTH LINE
  - EM - EARTH METER
  - EN - EARTH NIPPLE
  - EO - EARTH OUTLET
  - EP - EARTH PUMP
  - EQ - EARTH QUALITY
  - ER - EARTH REGISTER
  - ES - EARTH SUPPLY
  - ET - EARTH TREATMENT
  - EV - EARTH VALVE
  - EW - EARTH WASH
  - EX - EARTH EXHAUST
  - EY - EARTH YARD
  - EZ - EARTH ZONE
  - FA - FAN
  - FB - FAN BANK
  - FC - FAN CHARGE
  - FD - FAN DISCHARGE
  - FE - FAN EQUALIZER
  - FF - FAN FILL
  - FG - FAN GROUND
  - FH - FAN HEATER
  - FI - FAN INLET
  - FJ - FAN JUNCTION
  - FK - FAN KITCHEN
  - FL - FAN LINE
  - FM - FAN METER
  - FN - FAN NIPPLE
  - FO - FAN OUTLET
  - FP - FAN PUMP
  - FQ - FAN QUALITY
  - FR - FAN REGISTER
  - FS - FAN SUPPLY
  - FT - FAN TREATMENT
  - FV - FAN VALVE
  - FW - FAN WASH
  - FX - FAN EXHAUST
  - FY - FAN YARD
  - FZ - FAN ZONE
  - GA - GAS
  - GB - GAS BANK
  - GC - GAS CHARGE
  - GD - GAS DISCHARGE
  - GE - GAS EQUALIZER
  - GF - GAS FILL
  - GG - GAS GROUND
  - GH - GAS HEATER
  - GI - GAS INLET
  - GJ - GAS JUNCTION
  - GK - GAS KITCHEN
  - GL - GAS LINE
  - GM - GAS METER
  - GN - GAS NIPPLE
  - GO - GAS OUTLET
  - GP - GAS PUMP
  - GQ - GAS QUALITY
  - GR - GAS REGISTER
  - GS - GAS SUPPLY
  - GT - GAS TREATMENT
  - GV - GAS VALVE
  - GW - GAS WASH
  - GX - GAS EXHAUST
  - GY - GAS YARD
  - GZ - GAS ZONE
  - HA - HAZARDOUS
  - HB - HAZARDOUS BANK
  - HC - HAZARDOUS CHARGE
  - HD - HAZARDOUS DISCHARGE
  - HE - HAZARDOUS EQUALIZER
  - HF - HAZARDOUS FILL
  - HG - HAZARDOUS GROUND
  - HH - HAZARDOUS HEATER
  - HI - HAZARDOUS INLET
  - HJ - HAZARDOUS JUNCTION
  - HK - HAZARDOUS KITCHEN
  - HL - HAZARDOUS LINE
  - HM - HAZARDOUS METER
  - HN - HAZARDOUS NIPPLE
  - HO - HAZARDOUS OUTLET
  - HP - HAZARDOUS PUMP
  - HQ - HAZARDOUS QUALITY
  - HR - HAZARDOUS REGISTER
  - HS - HAZARDOUS SUPPLY
  - HT - HAZARDOUS TREATMENT
  - HV - HAZARDOUS VALVE
  - HW - HAZARDOUS WASH
  - HX - HAZARDOUS EXHAUST
  - HY - HAZARDOUS YARD
  - HZ - HAZARDOUS ZONE
  - IA - INSULATION
  - IB - INSULATION BANK
  - IC - INSULATION CHARGE
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  - IS - INSULATION SUPPLY
  - IT - INSULATION TREATMENT
  - IV - INSULATION VALVE
  - IW - INSULATION WASH
  - IX - INSULATION EXHAUST
  - IY - INSULATION YARD
  - IZ - INSULATION ZONE
  - JA - JUNCTION
  - JB - JUNCTION BANK
  - JC - JUNCTION CHARGE
  - JD - JUNCTION DISCHARGE
  - JE - JUNCTION EQUALIZER
  - JF - JUNCTION FILL
  - JG - JUNCTION GROUND
  - JH - JUNCTION HEATER
  - JI - JUNCTION INLET
  - IJ - JUNCTION JUNCTION
  - JK - JUNCTION KITCHEN
  - JL - JUNCTION LINE
  - JM - JUNCTION METER
  - JN - JUNCTION NIPPLE
  - JO - JUNCTION OUTLET
  - JP - JUNCTION PUMP
  - JQ - JUNCTION QUALITY
  - JR - JUNCTION REGISTER
  - JS - JUNCTION SUPPLY
  - JT - JUNCTION TREATMENT
  - JV - JUNCTION VALVE
  - JW - JUNCTION WASH
  - JX - JUNCTION EXHAUST
  - JY - JUNCTION YARD
  - JZ - JUNCTION ZONE
  - KA - KEYS
  - KB - KEYS BANK
  - KC - KEYS CHARGE
  - KD - KEYS DISCHARGE
  - KE - KEYS EQUALIZER
  - KF - KEYS FILL
  - KG - KEYS GROUND
  - KH - KEYS HEATER
  - KI - KEYS INLET
  - KJ - KEYS JUNCTION
  - KK - KEYS KITCHEN
  - KL - KEYS LINE
  - KM - KEYS METER
  - KN - KEYS NIPPLE
  - KO - KEYS OUTLET
  - KP - KEYS PUMP
  - KQ - KEYS QUALITY
  - KR - KEYS REGISTER
  - KS - KEYS SUPPLY
  - KT - KEYS TREATMENT
  - KV - KEYS VALVE
  - KW - KEYS WASH
  - KX - KEYS EXHAUST
  - KY - KEYS YARD
  - KZ - KEYS ZONE
  - LA - LAMP
  - LB - LAMP BANK
  - LC - LAMP CHARGE
  - LD - LAMP DISCHARGE
  - LE - LAMP EQUALIZER
  - LF - LAMP FILL
  - LG - LAMP GROUND
  - LH - LAMP HEATER
  - LI - LAMP INLET
  - LJ - LAMP JUNCTION
  - LK - LAMP KITCHEN
  - LL - LAMP LINE
  - LM - LAMP METER
  - LN - LAMP NIPPLE
  - LO - LAMP OUTLET
  - LP - LAMP PUMP
  - LQ - LAMP QUALITY
  - LR - LAMP REGISTER
  - LS - LAMP SUPPLY
  - LT - LAMP TREATMENT
  - LV - LAMP VALVE
  - LW - LAMP WASH
  - LX - LAMP EXHAUST
  - LY - L

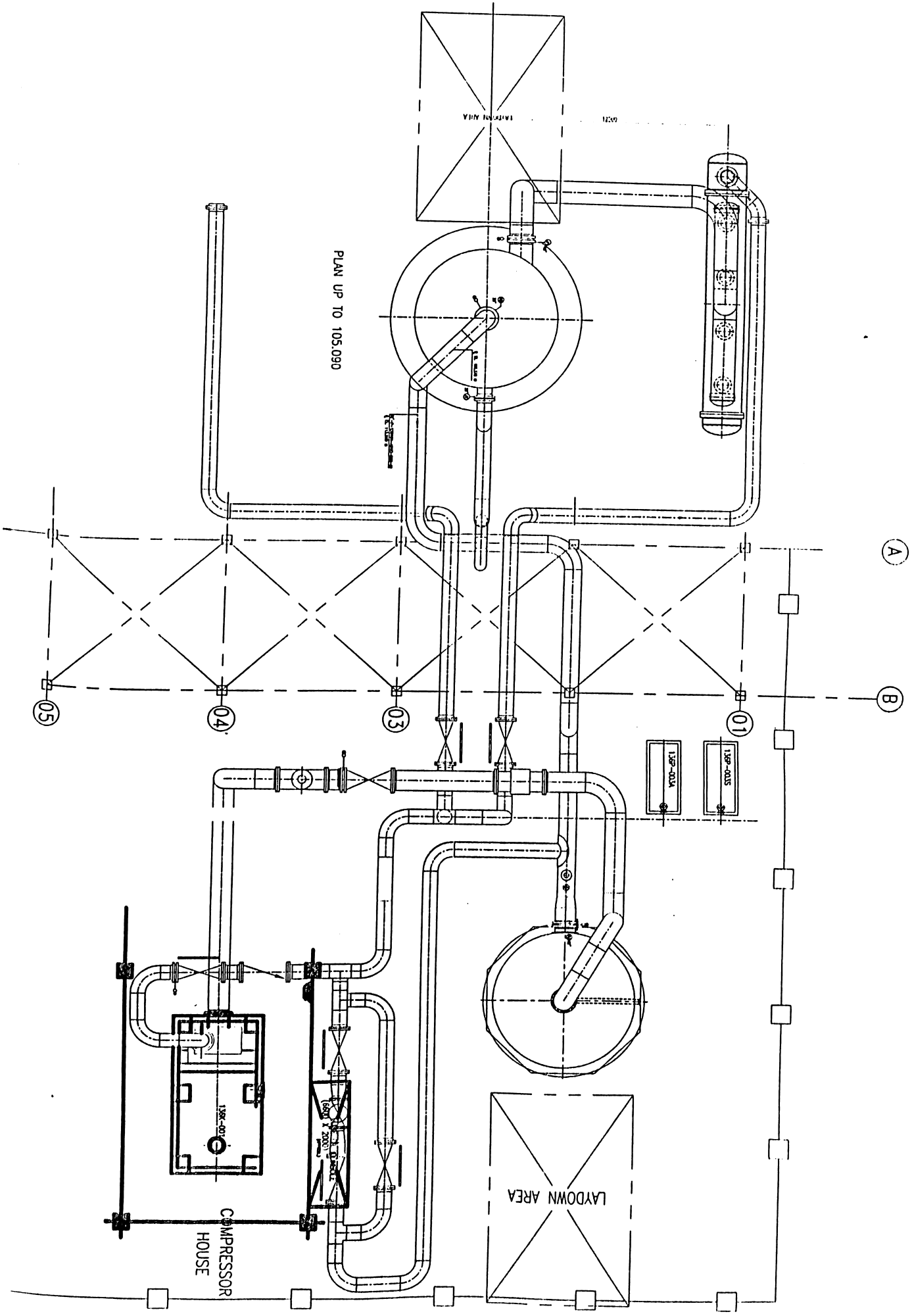
**4.11 PROCESS & INSTRUMENTATION DIAGRAM FOR COMPRESSOR  
STATION**



PIPING & INSTRUMENTATION  
 DIAGRAM  
 COMPRESSOR STATION



**4.12 PIPING ROUTING LAYOUT FOR COMPRESSOR STATION - OPTION - 1**



PLAN UP TO 105.090

LAYDOWN AREA

LAYDOWN AREA

COMPRESSOR HOUSE

15P-007

15P-003

15P-003A

15P-003B

A

B

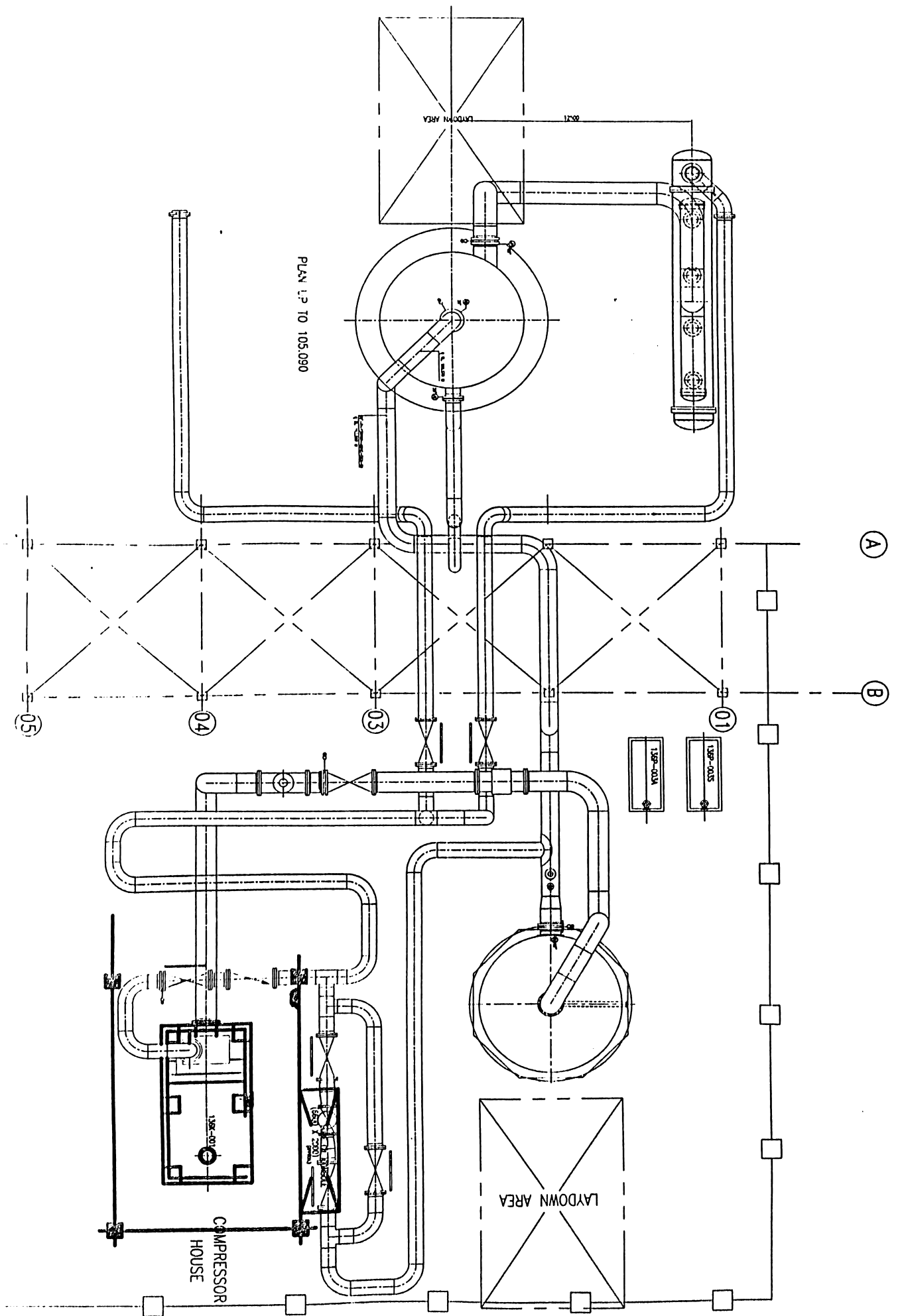
01

03

04

05

**4.12 PIPING ROUTING LAYOUT FOR COMPRESSOR STATION - OPTION - 2**



PLAN I.P. TO 105,090

LAYDOWN AREA

LAYDOWN AREA

COMPRESSOR HOUSE

138-004

138-003

138-011

138-001

A

B

01

03

04

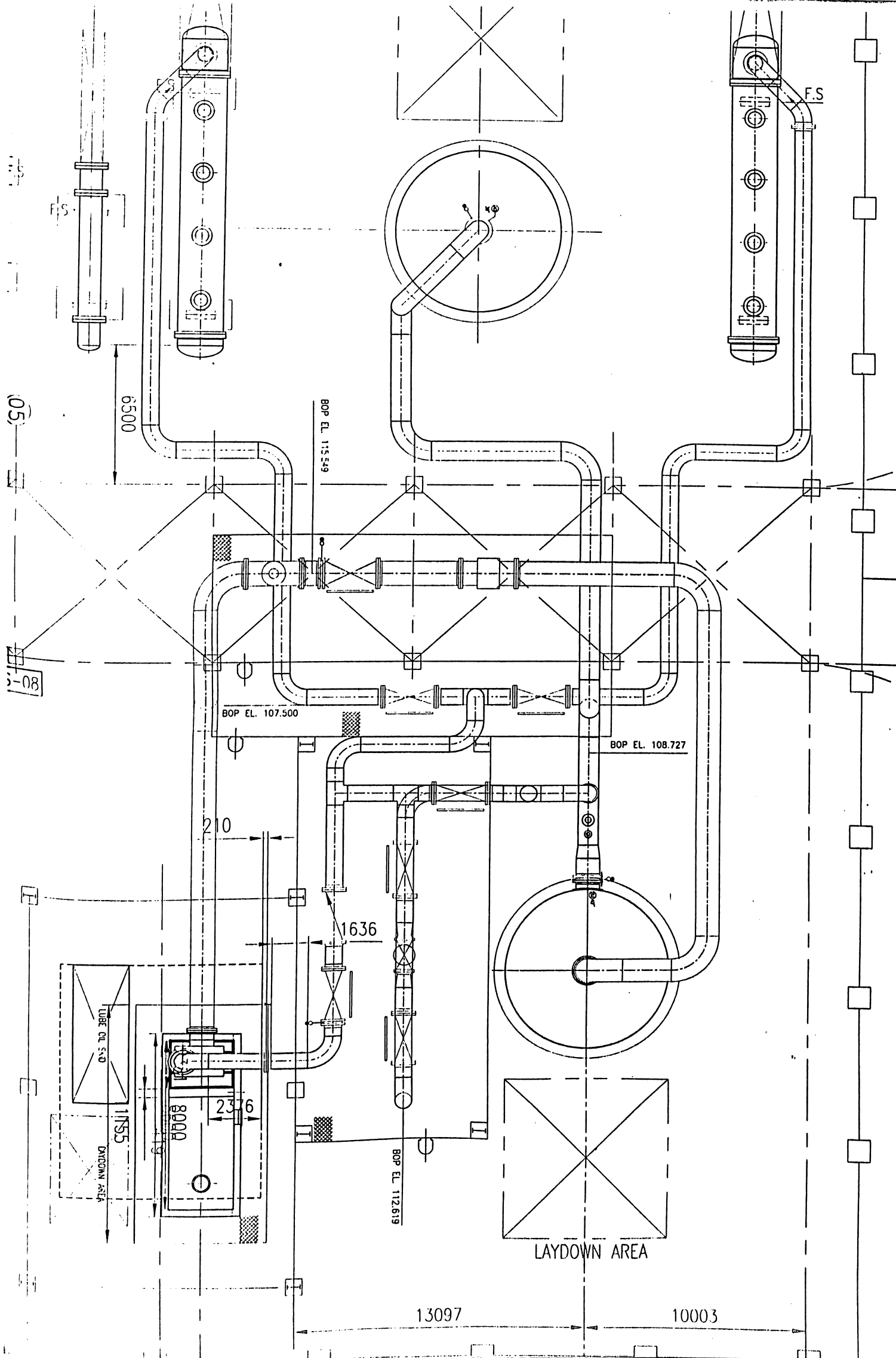
05

2521

**4.12 PIPING ROUTING LAYOUT FOR COMPRESSOR STATION - OPTION - 3**



**4.12 PIPING ROUTING LAYOUT FOR COMPRESSOR STATION - OPTION - 4  
APPROVED FOR MODELING**





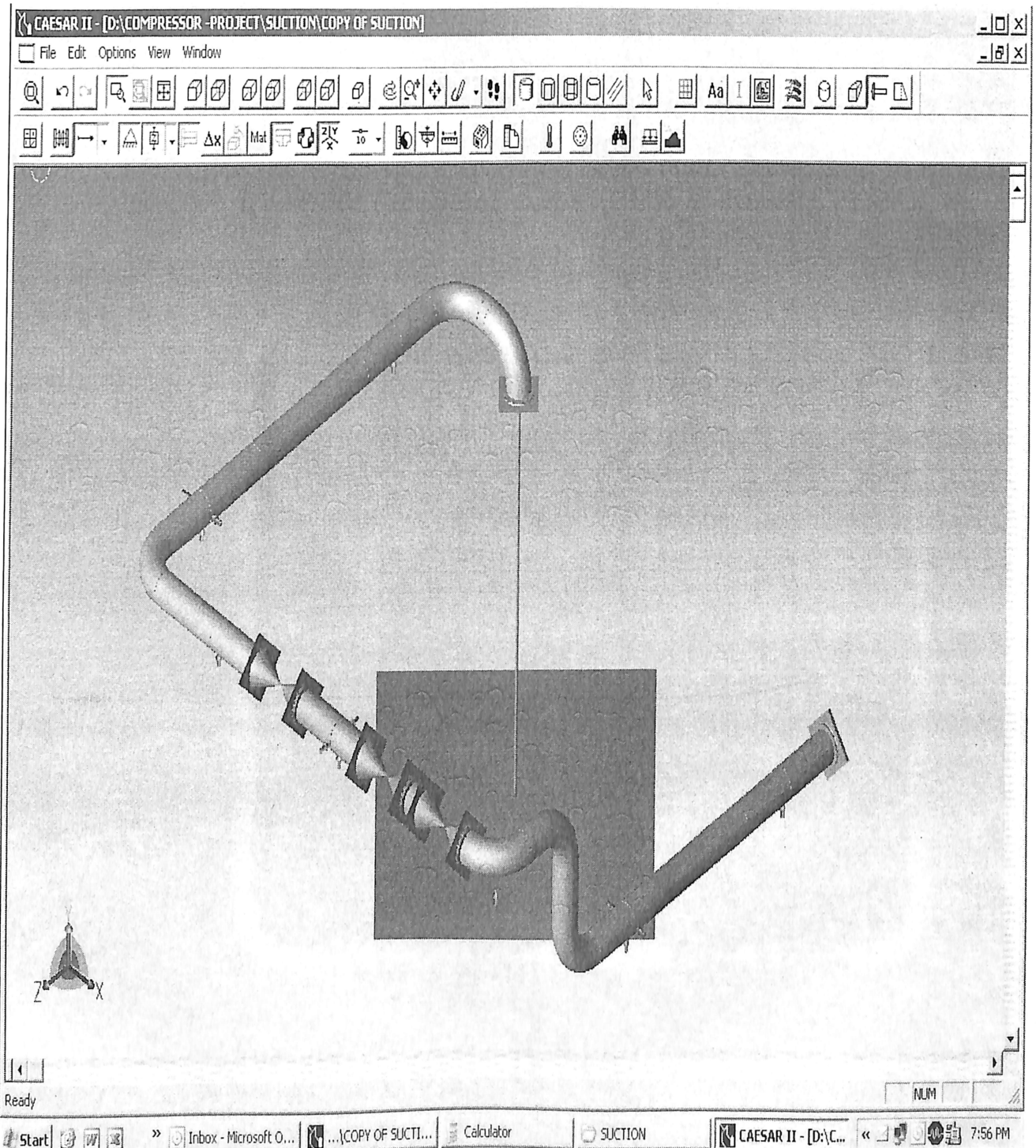
**4.13 ISOMETRIC DRAWING FOR COMPRESSOR SUCTION LINE**



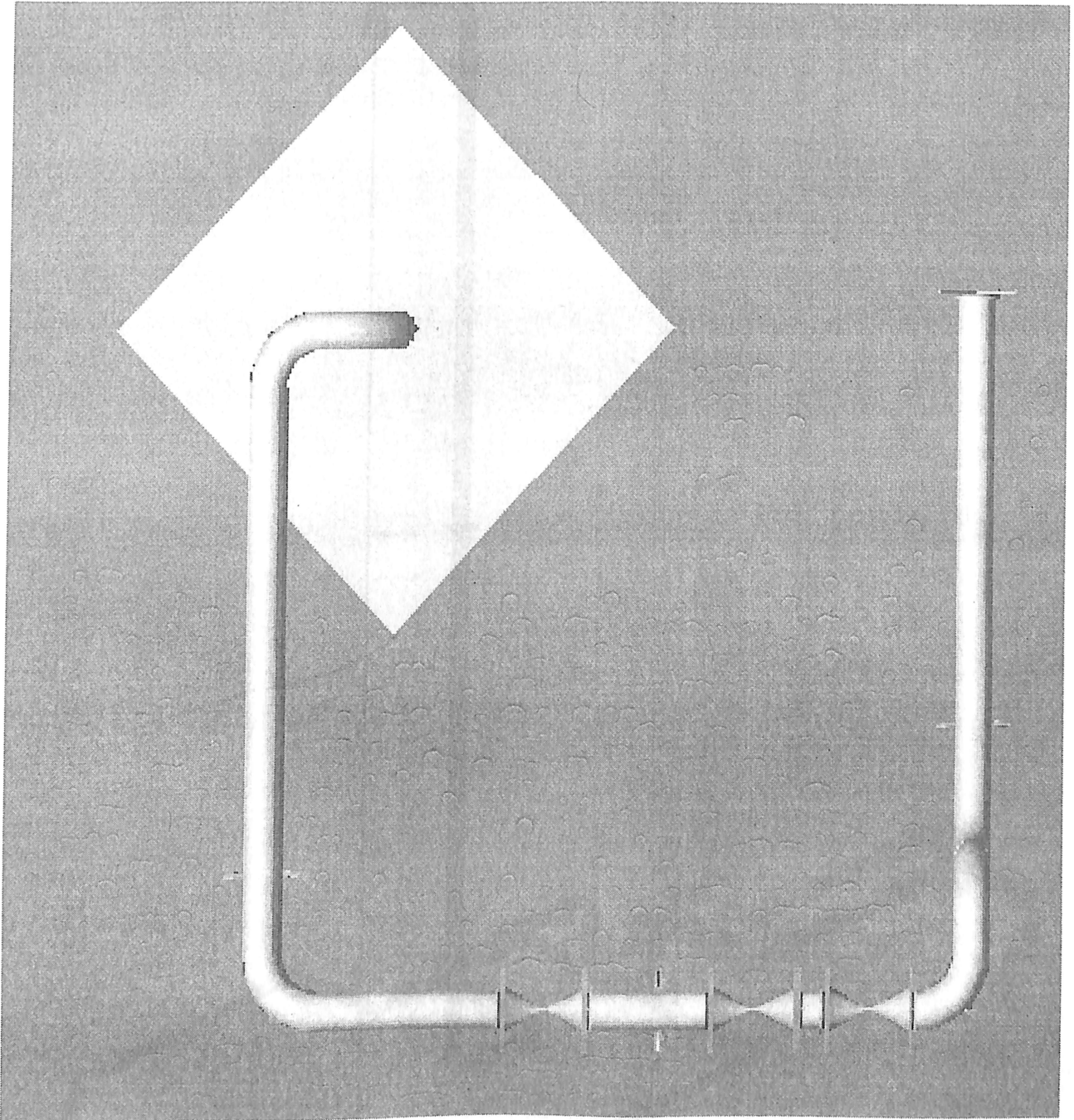
**4.13 ISOMETRIC DRAWING FOR COMPRESSOR DISCHARGE LINE**



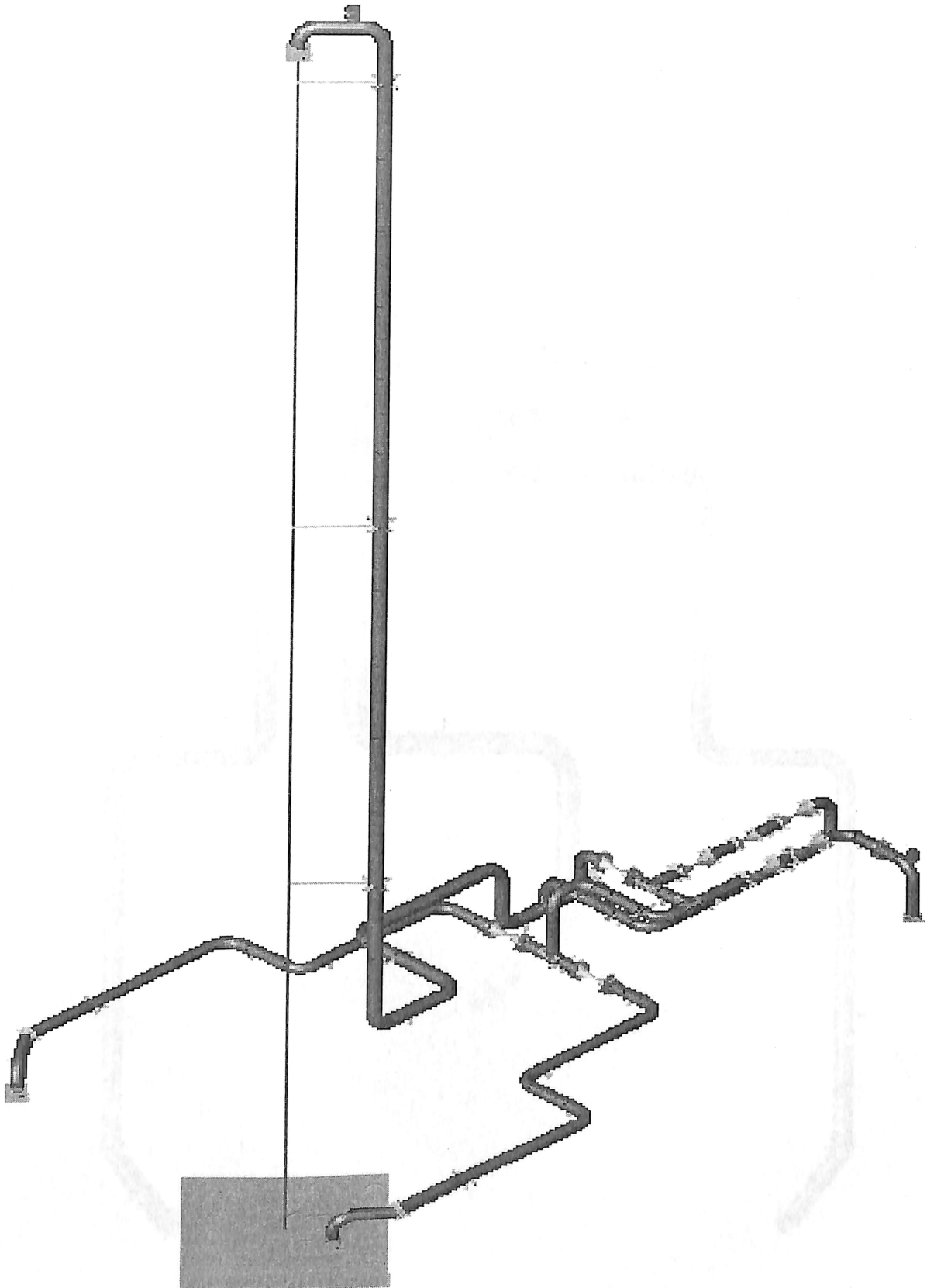
### 4.14 COMPRESSOR SUCTION LINE MODELING DIAGRAM IN CAESAR II ISOMETRIC VIEW



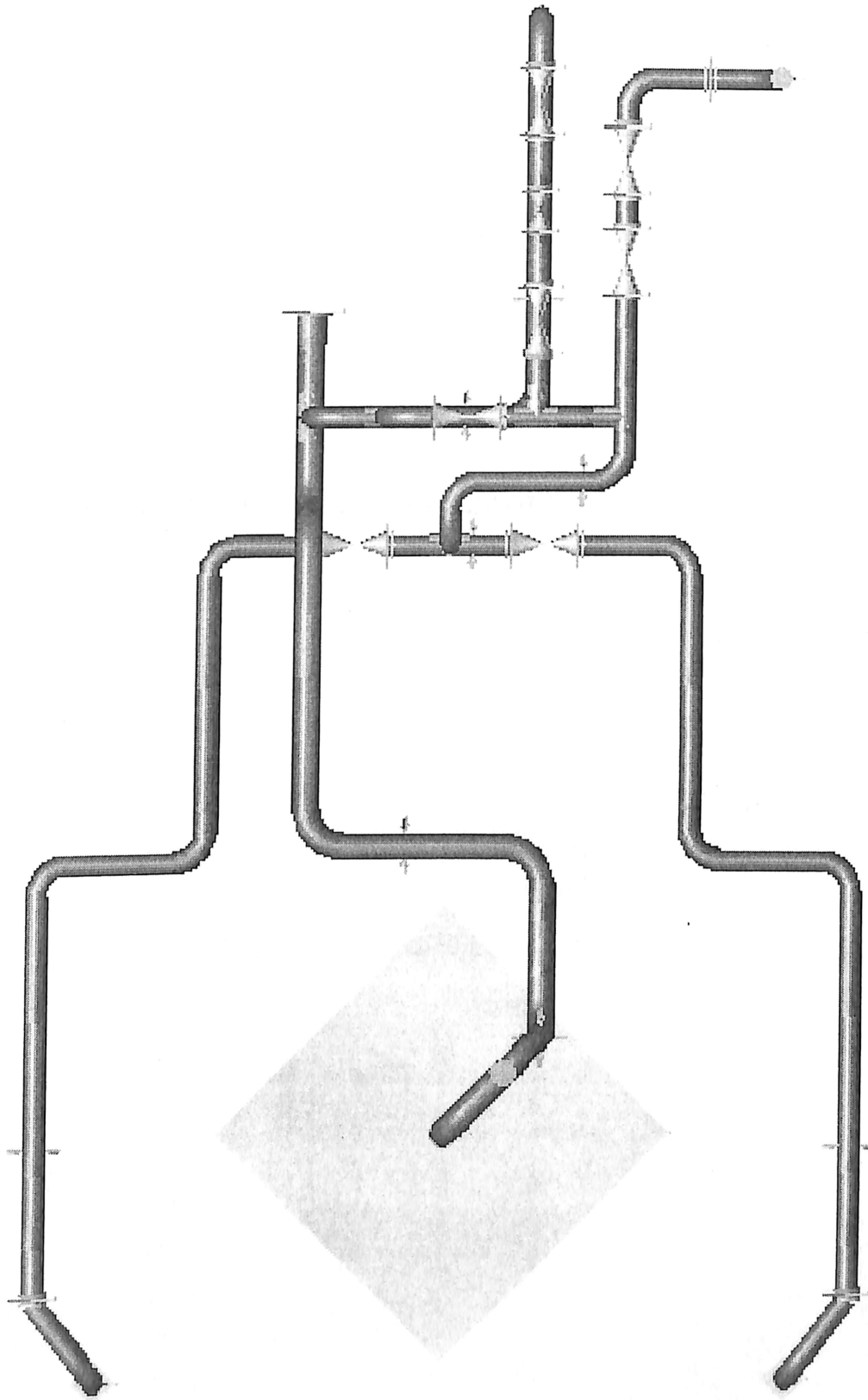
4.14 COMPRESSOR SUCTION LINE MODELING DIAGRAM IN CAESAR II  
TOP VIEW



4.15 COMPRESSOR DISCHARGE LINE MODELING DIAGRAM IN CAESAR II  
ISOMETRIC VIEW



4.15 COMPRESSOR DISCHARGE LINE MODELING DIAGRAM IN CAESAR II  
TOP VIEW





**4.16 STRESS ANALYSIS REPORT - CAESAR II**

# Design of Propylene Gas Pipeline System

---

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

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DISPLACEMENT REPORT, Nodal Movements (CASE 2)OPE) W+D1+T1+P1)	7
DISPLACEMENT REPORT, Nodal Movements (CASE 4)(SUS) W+P1)	8
RESTRAINT-DISPLACEMENT REPORT-RESTRAINT SUMMARY)	9
STRESS SUMMARY (CODE RESULT)	11

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

## INPUT LISTING

### PIPE DATA

From 10 To 20 DY= 171.000 mm.

#### PIPE

Dia= 1,066.800 mm. Wall= 12.700 mm. Insul= 50.000 mm. Cor= 1.5000 mm.

#### GENERAL

T1= 27 C T2= 120 C P1=1200.0000 KPa PHyd=1800.0000 KPa

Mat= (106)A106 B E= 203,395,424 KPa  $\nu$  = .292 Density= .0078 kg./cu.cm.

Insul= .0001 kg./cu.cm. Fluid= .0009996 kg./cu.cm.

RIGID Weight= 3,207.01 N.

#### RESTRAINTS

Node 10 ANC Cnode 1000

#### UNIFORM LOAD

GX1= .26 g's GY1= .00 g's GZ1= .00 g's GX2= .00 g's GY2= .17 g's

GZ2= .00 g's GX3= .00 g's GY3= .00 g's GZ3= .26 g's

#### WIND

Wind Shape= .650

#### ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa

Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa

Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

From 20 To 30 DY= 1,603.000 mm.

BEND at "TO" end

Radius= 1,600.200 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 29

From 30 To 35 DX= -2,000.000 mm.

From 35 To 40 DX= -1,815.000 mm.

BEND at "TO" end

Radius= 1,600.200 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 39

Angle/Node @2= .00 38

From 40 To 45 DZ= 3,600.000 mm.

#### RESTRAINTS

Node 45 +Y Mu = .30

From 45 To 60 DZ= 2,000.000 mm.

From 60 To 80 DZ= 6,000.000 mm.

From 80 To 85 DZ= 3,000.000 mm.

#### RESTRAINTS

Node 85 +Y Mu = .30

Node 85 X

From 85 To 100 DZ= 3,775.000 mm.

BEND at "TO" end

Radius= 1,600.200 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 49

Angle/Node @2= .00 48

## Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

-----  
From 100 To 110 DX= 4,812.000 mm.

RESTRAINTS

Node 110 +Y Mu = .30

-----  
From 110 To 120 DX= 2,188.000 mm.

-----  
From 120 To 130 DX= 171.000 mm.

RIGID Weight= 3,933.10 N.

RESTRAINTS

Node 130 ANC Cnode 131

-----  
From 131 To 140 DX= 2,500.000 mm.

RIGID Weight=60,000.00 N.

RESTRAINTS

Node 140 ANC Cnode 141

-----  
From 141 To 150 DX= 171.000 mm.

RIGID Weight= 3,207.01 N.

-----  
From 150 To 155 DX= 1,970.000 mm.

RESTRAINTS

Node 155 +Y Mu = .30

Node 155 Z

-----  
From 155 To 160 DX= 1,410.000 mm.

-----  
From 160 To 170 DX= 171.000 mm.

RIGID Weight= 3,207.01 N.

RESTRAINTS

Node 170 ANC Cnode 171

-----  
From 171 To 180 DX= 2,500.000 mm.

RIGID Weight=60,000.00 N.

RESTRAINTS

Node 180 ANC Cnode 181

-----  
From 181 To 190 DX= 100.000 mm.

RIGID Weight= 5,000.00 N.

RESTRAINTS

Node 190 ANC Cnode 191

-----  
From 191 To 200 DX= 171.000 mm.

RIGID Weight= 3,207.01 N.

-----  
From 200 To 210 DX= 500.000 mm.

-----  
From 210 To 220 DX= 171.000 mm.

RIGID Weight= 3,207.01 N.

RESTRAINTS

Node 220 ANC Cnode 221

-----  
From 221 To 230 DX= 2,500.000 mm.

RIGID Weight=60,000.00 N.

RESTRAINTS

Node 230 ANC Cnode 231

-----  
From 231 To 240 DX= 171.000 mm.

RIGID Weight= 3,207.01 N.

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line  
From 240 To 250 DX= 1,600.000 mm.

BEND at "TO" end

Radius= 1,600.200 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 189

RESTRAINTS

Node 250 +Y Mu = .30

-----  
From 250 To 260 DZ= -4,100.000 mm.

BEND at "TO" end

Radius= 1,600.200 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 199

Angle/Node @2= .00 198

-----  
From 260 To 270 DY= -5,482.000 mm.

BEND at "TO" end

Radius= 1,600.200 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 209

Angle/Node @2= .00 208

-----  
From 270 To 273 DZ= -3,597.000 mm.

RESTRAINTS

Node 273 +Y Mu = .30

Node 273 X

-----  
From 273 To 276 DZ= -6,567.000 mm.

-----  
From 276 To 278 DZ= -2,500.000 mm.

RESTRAINTS

Node 278 +Y Mu = .30

-----  
From 278 To 280 DZ= -2,500.000 mm.

-----  
From 280 To 290 DZ= -171.000 mm.

RIGID Weight= 3,207.01 N.

RESTRAINTS

Node 290 ANC Cnode 300

DISPLACEMENTS

Node 300 DX1= .000 mm. DY1= .000 mm. DZ1= 1.000 mm. RX1= .000

RY1= .000 RZ1= .000 DX2= .000 mm. DY2= .000 mm. DZ2= 2.000 mm.

RX2= .000 RY2= .000 RZ2= .000

-----  
From 1000 To 1010 DY= -1,850.000 mm.

-----  
PIPE DATA

Dia= 7,496.000 mm. Wall= 48.000 mm. Insul= .000 mm. Cor= 3.0000 mm.

GENERAL

T1= 27 C T2= 120 C P1=1200.0000 KPa PHyd=1800.0000 KPa

Mat= (106)A106 B E= 203,395,424 KPa v = .292 Density= .0078 kg./cu.cm.

Insul= .0001 kg./cu.cm. Fluid= .0009996 kg./cu.cm.

-----  
ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa

Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa

Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 1010 To 1020 DY= -4,500.000 mm.

-----  
From 1020 To 1030 DY= -1,850.000 mm.

-----  
From 1030 To 1040 DY= -5,650.000 mm.

RESTRAINTS

Node 1040 ANC

# Design of Propylene Gas Pipeline System

---

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

---

## CEASER II LOAD CASE REPORT

CASE 1 (HYD) WW+HP  
HYDRO TEST CASE

CASE 2 (OPE) W+D1+T1+P1  
OPERATING CASE CONDITION 1

CASE 3 (OPE) W+D2+T2+P1  
OPERATING CASE CONDITION 2

CASE 4 (SUS) W+P1  
SUSTAINED CASE CONDITION 1

CASE 5 (OPE) W+D1+T1+P1+U1

CASE 6 (OPE) W+D1+T1+P1-U1

CASE 7 (OPE) W+D1+T1+P1+U2

CASE 8 (OPE) W+D1+T1+P1-U2

CASE 9 (OPE) W+D1+T1+P1+U3

CASE 10 (OPE) W+D1+T1+P1-U3

CASE 11 (OPE) W+D1+T1+P1+WIN1

CASE 12 (OPE) W+D1+T1+P1-WIN1

CASE 13 (OPE) W+D1+T1+P1+WIN2

CASE 14 (OPE) W+D1+T1+P1-WIN2

CASE 15 (EXP) L15=L2-L4

CASE 16 (EXP) L16=L3-L4

CASE 17 (OCC) L17=L5-L2

CASE 18 (OCC) L18=L6-L2

CASE 19 (OCC) L19=L7-L2

CASE 20 (OCC) L20=L8-L2

CASE 21 (OCC) L21=L9-L2

CASE 22 (OCC) L22=L10-L2

CASE 23 (OCC) L23=L11-L2

CASE 24 (OCC) L24=L12-L2

CASE 25 (OCC) L25=L13-L2

CASE 26 (OCC) L26=L14-L2

CASE 27 (OCC) L27=L4+L17

## Design of Propylene Gas Pipeline System

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CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

CASE 28 (OCC) L28=L4+L18

CASE 29 (OCC) L29=L4+L19

CASE 30 (OCC) L30=L4+L20

CASE 31 (OCC) L31=L4+L21

CASE 32 (OCC) L32=L4+L22

CASE 33 (OCC) L33=L4+L23

CASE 34 (OCC) L34=L4+L24

CASE 35 (OCC) L35=L4+L25

CASE 36 (OCC) L36=L4+L26

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

DISPLACEMENT REPORT, Nodal Movements  
CASE 2 (OPE) W+D1+T1+P1

NODE	-----Translations (mm.)-----			-----Rotations (deg.)-----		
	DX	DY	DZ	RX	RY	RZ
10	0.002	0.911	-0.002	0.0000	0.0000	0.0000
20	0.002	0.923	-0.002	0.0000	0.0000	0.0000
29	-0.203	0.957	-0.188	-0.0137	-0.0070	0.0172
30	-0.509	0.543	-0.549	-0.0165	-0.0137	0.0259
35	-0.555	0.360	-0.649	-0.0164	-0.0137	0.0259
38	-0.579	0.262	-0.702	-0.0163	-0.0137	0.0258
39	-0.747	-0.065	-0.803	-0.0163	0.0009	0.0222
40	-0.621	-0.028	-0.622	-0.0019	0.0136	0.0259
45	-0.136	0.000	-0.395	0.0038	0.0125	0.0260
48	-0.736	-0.152	1.056	0.0064	-0.0198	0.0270
49	-1.037	-0.484	1.311	0.0398	-0.0090	0.0166
60	0.250	-0.294	-0.176	0.0079	0.0092	0.0262
80	0.531	-0.414	0.481	-0.0071	-0.0054	0.0266
85	0.000	0.000	0.810	-0.0018	-0.0155	0.0269
100	-0.920	-0.594	1.296	0.0464	0.0128	0.0110
110	-0.561	0.000	0.567	0.0532	0.0101	0.0058
120	-0.321	0.053	0.281	0.0578	0.0048	0.0008
130	-0.309	0.055	0.266	0.0578	0.0047	0.0008
131	-0.309	0.055	0.266	0.0578	0.0047	0.0008
140	-0.135	0.091	0.069	0.0582	0.0043	0.0006
141	-0.135	0.091	0.069	0.0582	0.0043	0.0006
150	-0.123	0.094	0.056	0.0583	0.0042	0.0006
155	0.093	0.000	0.000	0.0624	-0.0011	-0.0141
160	0.250	-0.605	0.080	0.0654	-0.0045	-0.0239
170	0.262	-0.678	0.093	0.0654	-0.0045	-0.0239
171	0.262	-0.678	0.093	0.0654	-0.0045	-0.0239
180	0.437	-1.724	0.296	0.0658	-0.0047	-0.0232
181	0.437	-1.724	0.296	0.0658	-0.0047	-0.0232
189	0.722	-1.785	0.388	0.0861	0.0225	0.0447
190	0.444	-1.764	0.305	0.0658	-0.0047	-0.0232
191	0.444	-1.764	0.305	0.0658	-0.0047	-0.0232
198	-0.265	0.483	-0.075	0.0304	0.0282	0.0309
199	-0.481	0.435	-0.126	-0.0232	0.0215	0.0299
200	0.455	-1.834	0.319	0.0658	-0.0047	-0.0231
208	0.403	-0.225	2.222	-0.0409	0.0213	0.0140
209	0.407	-0.497	2.658	-0.0055	0.0208	0.0072
210	0.511	-2.024	0.364	0.0669	-0.0049	-0.0189
220	0.523	-2.080	0.379	0.0669	-0.0049	-0.0188
221	0.523	-2.080	0.379	0.0669	-0.0049	-0.0188
230	0.698	-2.862	0.595	0.0673	-0.0048	-0.0173
231	0.698	-2.862	0.595	0.0673	-0.0048	-0.0173
240	0.710	-2.913	0.609	0.0673	-0.0048	-0.0172
250	0.184	0.000	0.028	0.0343	0.0288	0.0323
260	-0.191	0.037	0.532	-0.0422	0.0240	0.0161
270	0.182	-0.390	2.493	0.0112	0.0063	0.0103
273	0.000	0.000	2.266	0.0049	0.0039	0.0088
276	-0.084	-0.168	1.550	0.0022	-0.0010	0.0038
278	-0.030	0.000	1.278	0.0020	-0.0010	0.0019
280	0.000	0.000	1.012	0.0000	0.0000	0.0000
290	0.000	0.000	1.000	0.0000	0.0000	0.0000
300	0.000	0.000	1.000	0.0000	0.0000	0.0000
1000	0.002	0.911	-0.002	0.0000	0.0000	0.0000
1010	0.001	0.789	-0.001	0.0000	0.0000	0.0000
1020	0.001	0.493	-0.001	0.0000	0.0000	0.0000
1030	0.001	0.372	-0.001	0.0000	0.0000	0.0000
1040	0.000	0.000	0.000	0.0000	0.0000	0.0000



# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

DISPLACEMENT REPORT, Nodal Movements

CASE 4 (SUS) W+P1

NODE	-----Translations (mm.)-----			-----Rotations (deg.)-----		
	DX	DY	DZ	RX	RY	RZ
10	0.001	0.000	-0.001	0.0000	0.0000	0.0000
20	0.001	0.000	-0.001	0.0000	0.0000	0.0000
29	-0.126	-0.008	-0.148	-0.0115	-0.0047	0.0103
30	-0.276	-0.213	-0.400	-0.0140	-0.0082	0.0099
35	-0.296	-0.283	-0.459	-0.0141	-0.0081	0.0098
38	-0.306	-0.319	-0.490	-0.0142	-0.0081	0.0097
39	-0.389	-0.310	-0.563	-0.0160	-0.0005	0.0040
40	-0.343	-0.098	-0.489	-0.0038	0.0057	0.0074
45	-0.139	0.000	-0.391	0.0024	0.0052	0.0086
48	-0.232	-0.117	0.209	0.0052	-0.0062	0.0164
49	-0.313	-0.444	0.300	0.0327	-0.0021	0.0091
60	0.020	-0.265	-0.301	0.0075	0.0038	0.0098
80	0.162	-0.412	-0.032	-0.0067	-0.0015	0.0133
85	0.000	0.000	0.103	-0.0023	-0.0048	0.0151
100	-0.255	-0.562	0.288	0.0364	0.0043	0.0101
110	-0.099	0.000	0.057	0.0427	0.0027	0.0053
120	0.002	0.038	0.000	0.0470	0.0004	0.0007
130	0.003	0.040	-0.001	0.0471	0.0004	0.0007
131	0.003	0.040	-0.001	0.0471	0.0004	0.0007
140	0.013	0.073	-0.015	0.0474	0.0003	0.0006
141	0.013	0.073	-0.015	0.0474	0.0003	0.0006
150	0.014	0.075	-0.016	0.0474	0.0003	0.0006
155	0.106	0.000	0.000	0.0513	-0.0010	-0.0128
160	0.174	-0.559	0.036	0.0541	-0.0017	-0.0216
170	0.175	-0.624	0.041	0.0541	-0.0017	-0.0216
171	0.175	-0.624	0.041	0.0541	-0.0017	-0.0216
180	0.186	-1.566	0.114	0.0545	-0.0017	-0.0208
181	0.186	-1.566	0.114	0.0545	-0.0017	-0.0208
189	0.236	-1.509	0.134	0.0737	0.0083	0.0463
190	0.186	-1.602	0.117	0.0545	-0.0017	-0.0208
191	0.186	-1.602	0.117	0.0545	-0.0017	-0.0208
198	-0.156	0.209	-0.054	0.0137	0.0119	0.0308
199	-0.153	0.030	-0.001	-0.0182	0.0136	0.0266
200	0.187	-1.664	0.122	0.0545	-0.0017	-0.0207
208	0.430	-0.295	0.724	-0.0098	0.0167	0.0079
209	0.371	-0.345	0.746	0.0054	0.0166	0.0027
210	0.211	-1.832	0.138	0.0555	-0.0017	-0.0163
220	0.212	-1.881	0.143	0.0555	-0.0017	-0.0162
221	0.212	-1.881	0.143	0.0555	-0.0017	-0.0162
230	0.223	-2.548	0.215	0.0559	-0.0016	-0.0147
231	0.223	-2.548	0.215	0.0559	-0.0016	-0.0147
240	0.224	-2.591	0.220	0.0559	-0.0016	-0.0146
250	0.034	0.000	-0.009	0.0175	0.0120	0.0323
260	0.086	-0.178	0.301	-0.0113	0.0183	0.0098
270	0.162	-0.195	0.622	0.0060	0.0055	0.0053
273	0.000	0.000	0.523	0.0009	0.0034	0.0045
276	-0.063	-0.218	0.223	0.0034	-0.0009	0.0020
278	-0.017	0.000	0.109	0.0026	-0.0007	0.0010
280	0.000	0.000	0.001	0.0000	0.0000	0.0000
290	0.000	0.000	0.000	0.0000	0.0000	0.0000
300	0.000	0.000	0.000	0.0000	0.0000	0.0000
1000	0.001	0.000	-0.001	0.0000	0.0000	0.0000
1010	0.001	0.000	-0.001	0.0000	0.0000	0.0000
1020	0.000	0.000	0.000	0.0000	0.0000	0.0000
1030	0.000	0.000	0.000	0.0000	0.0000	0.0000
1040	0.000	0.000	0.000	0.0000	0.0000	0.0000

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints  
RESTRAINT SUMMARY

NODE	CASE	TYPE	---Forces(N. )---			---Moments(N.m.)----			--Displacements(mm.)--		
			FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
			Rigid ANC								
	1	HYD	1097.	-42434.	-10642.	-18652.	-17967.	5991.	0.0011	-0.0002	-0.0013
	2	OPE	16820.	-47736.	-14767.	-18594.	-24932.	9183.	0.0017	0.9107	-0.0017
	4	SUS	7637.	-41155.	-5988.	-14970.	-8343.	8623.	0.0007	-0.0002	-0.0007
MAX.	2		16820.	47736.	14767.	18652/1	24932.	9183.	0.002	0.911	0.002
			Rigid +Y								
	1	HYD	-9476.	-116512.	-33645	0.	0.	0.	-0.1654	0.0000	-0.5874
	2	OPE	-10722.	-109515.	-31056.	0.	0.	0.	-0.1362	0.0000	-0.3947
	4	SUS	-11876.	-117920.	-33323.	0.	0.	0.	-0.1395	0.0000	-0.3914
MAX.	1		11876/4	117920/4	33645/1	0./1	0./1	0./1	0.165/1	0.000/4	0.5874
			Rigid +Y Rigid X								
	1	HYD	-18522.	-108423.	31008.	0.	0.	0.	0.0000	0.0000	0.1771
	2	OPE	-36645.	-111574.	33472.	0.	0.	0.	0.0000	0.0000	0.8100
	4	SUS	-11903.	-108173.	18049.	0.	0.	0.	0.0000	0.0000	0.1031
MAX.			36645.	111574.	33472.	0./1	0./1	0./1	0.0000	0.0000	0.8100
			Rigid +Y								
	1	HYD	-25212.	-99393.	15920.	0.	0.	0.	-0.1683	0.0000	0.1063
	2	OPE	-20291.	-96207.	20526.	0.	0.	0.	-0.5609	0.0000	0.5674
	4	SUS	-17387.	-99994.	9915.	0.	0.	0.	-0.0993	0.0000	0.0566
MAX.			25212/1	99994/4	20526/2	0/1	0/1	0/1	0.561/2	0.00/4	0.57/2
			Rigid ANC								
	1	HYD	39746.	19045.	-2318.	-32433.	29141.	5213.	-0.0142	0.0444	0.0127
	2	OPE	50844.	17314.	1121.	-33865.	52062.	9190.	-0.3093	0.0549	0.2663
	4	SUS	28217.	19526.	-1701.	-31495.	19427.	3272.	0.0030	0.0397	-0.0008
MAX.			50844/2	19526/4	2318/1	33865/2	52062/2	9190/20	0.309/20	0.055/20	0.27/2
			Rigid ANC								
	1	HYD	39746.	-62580.	-2318.	-32433.	23346.	59632.	0.0015	0.0783	-0.017
	2	OPE	50844.	-64311.	1121.	-33865.	54865.	67936.	-0.1350	0.0914	0.069
	4	SUS	28217.	-62098.	-1701.	-31495.	15175.	56487.	0.0134	0.0730	-0.015
MAX.	2		50844	64311	2318/1	33865	54865	67936	0.135	0.091	0.069
			Rigid +Y Rigid Z								
	1	HYD	24577.	-228069.	1806.	0.	0.	0.	0.1403	0.	0.
	2	OPE	16233.	-231284.	11849.	0.	0.	0.	0.0927	0.	0.
	4	SUS	18489.	-227090.	1020.	0.	0.	0.	0.1056	0.	0.
MAX.			24577/1	231284/2	11849/2	0./1	0./1	0./1	0.140/1	0./2	0./2
			Rigid ANC								
	1	HYD	15170.	116397.	-4124.	-32433.	11864.	23338.	0.2441	-0.6384	0.059
	2	OPE	34610.	117881.	-10727.	-33865.	40306.	33000.	0.2618	-0.6778	0.093
	4	SUS	9728.	115900.	-2721.	-31495.	7232.	19947	0.1748	-0.6241	0.041
MAX.			34610.	117881.	10727.	33865.	40306.	33000.	0.2628	0.6778	0.093
			Rigid ANC								
	1	HYD	15170.	34772.	-4124.	-32433.	1554.	-165625.	0.2605	-1.6076	0.169
	2	OPE	34610.	36256.	-10727.	-33865.	13487.	-159672.	0.4365	-1.7235	0.296
	4	SUS	9728.	34275.	-2721.	-31495.	429.	-167774.	0.1858	-1.5659	0.114
MAX.	2		34610.	36256.	10727.	33865.	13487.	167774/4	0.437	1.724	0.296
			Rigid ANC								
	1	HYD	15170.	28907.	-4124.	-32433	1142.	-168809.	0.2612	-1.6452	0.173

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Suction Line

RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

RESTRAINT SUMMARY

NODE	CASE	TYPE	---Forces (N. )---			---Moments (N.m.)----			--Displacements (mm.)--		
			FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
	2	OPE	34610.	30391.	-10727.	-33865	12414.	-163005.	0.4435	-1.7642	0.305
	4	SUS	9728.	28410.	-2721.	-31495	157.	-170908.	0.1862	-1.6023	0.117
MAX.			34610	30391	10727	33865	12414	170908/4	0.444	1.7642	0.305
220			Rigid ANC								
	1	HYD	15170.	13659.	-4124.	-32433.	-2330.	-186730.	0.2998	-1.9334	0.212
	2	OPE	34610.	15143.	-10727.	-33865.	3382.	-182175.	0.5231	-2.0801	0.379
	4	SUS	9728.	13162.	-2721.	-31495.	-2134.	-188410.	0.2120	-1.8806	0.143
MAX.	2		34610.	15143.	10727.	33865.	3382.	188410/4	0.523	2.0801	0.379
230			Rigid ANC								
	1	HYD	15170.	-67965.	-4124.	-32433.	-12639.	-118847.	0.3162	-2.6311	0.321
	2	OPE	34610.	-66481.	-10727.	-33865.	-23437.	-118002.	0.6979	-2.8620	0.595
	4	SUS	9728.	-68462.	-2721.	-31495.	-8937.	-119284.	0.2229	-2.5480	0.215
MAX.	2		34610	68462	10727	33865.	23437	119284/4	0.698	2.862	0.595
250			Rigid +Y								
	1	HYD	11709.	-163622.	351.	0.	0.	0.	0.0669	0.0000	0.002
	2	OPE	32307.	-147704.	4823.	0.	0.	0.	0.1845	0.0000	0.028
	4	SUS	5942.	-168770.	-1587.	0.	0.	0.	0.0339	0.0000	-0.009
MAX.	2		32307	168770/4	4823	0./1	0./1	0./1	0.1845	0./4	0.028
273			Rigid +Y Rigid X								
	1	HYD	6911.	-117830.	35349.	0.	0.	0.	0.0000	0.0000	0.803
	2	OPE	5771.	-135735.	40720.	0.	0.	0.	0.0000	0.0000	2.266
	4	SUS	7165.	-111949.	33585.	0.	0.	0.	0.0000	0.0000	0.523
MAX.			7165/4	135735/2	40720/2	0./1	0./1	0./1	0.000/4	0.00/2	0.27/2
278			Rigid +Y								
	1	HYD	-2609.	-82360.	24570.	0.	0.	0.	-0.0179	0.0000	0.169
	2	OPE	-534.	-75337.	22595.	0.	0.	0.	-0.0302	0.0000	1.278
	4	SUS	-3036.	-84848.	19130.	0.	0.	0.	-0.0173	0.0000	0.109
MAX.			3036/4	84848/4	24570/1	0./1	0./1	0./1	0.030/2	0./4	1.28/2
290			Rigid ANC								
	1	HYD	-397.	1080.	-64169.	243.	-6906.	7635.	0.0000	0.0000	0.000
	2	OPE	-3076.	-2472.	-78133.	1746.	-12665.	12197.	0.0000	0.0000	1.000
	4	SUS	-344.	2339.	-53703.	-289.	-6669.	6298.	0.0000	0.0000	0.000
MAX.	2		3076.	2472	78133.	1746.	12665.	12197.	0.0000	0.0000	1.000
300			Displ. Reaction								
	1	HYD	-397.	1080.	-64169.	243.	-6906.	7635.	0.0000	0.0000	0.000
	2	OPE	-3076.	-2472.	-78133.	1746.	-12665.	12197.	0.0000	0.0000	1.000
	4	SUS	-344.	2339.	-53703.	-289.	-6669.	6298.	0.0000	0.0000	0.000
MAX.	2		3076.	2472.	78133.	1746.	12665.	12197.	0.0/1	0.0/1	1.0/2
1040			Rigid ANC								
	1	HYD	11097.	-42434.	-10642.	-166040.	-17967.	-147707.	0.	0.	0.
	2	OPE	16820.	-47736.	-14767.	-223119.	-24932.	-223775.	0.	0.	0.
	4	SUS	7637.	-41155.	-5988.	-97902.	-8343.	-97145.	0.	0.	0.
MAX.	2		16820.	47736.	14767.	223119.	24932.	223775.	0.	0.	0.

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

## STRESS SUMMARY

PIPING CODE: B31.3 -2002, April 30, 2002

### CASE 1 (HYD WW+HP)

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	36.7	@NODE	250	STRESS:	67228.4	ALLOWABLE:	183396.
BENDING STRESS:					30871.2	@NODE	250
TORSIONAL STRESS:					1480.6	@NODE	100
AXIAL STRESS:					36986.9	@NODE	199
HOOP STRESS:					73799.8	@NODE	29
3D MAX INTENSITY:					76729.1	@NODE	240

### CASE 4 (SUS) W+P1

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	45.7	@NODE	250	STRESS:	62962.3	ALLOWABLE:	137892.
BENDING STRESS:					35357.4	@NODE	250
TORSIONAL STRESS:					1623.5	@NODE	100
AXIAL STRESS:					28432.3	@NODE	199
HOOP STRESS:					55949.9	@NODE	29
3D MAX INTENSITY:					63732.0	@NODE	250

### CASE 15 (EXP) L15=L2-L4

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	4.3	@NODE	199	STRESS:	8805.5	ALLOWABLE:	206838.
BENDING STRESS:					8795.2	@NODE	199
TORSIONAL STRESS:					757.3	@NODE	20
AXIAL STRESS:					591.7	@NODE	160
HOOP STRESS:					0.0	@NODE	20
3D MAX INTENSITY:					10577.4	@NODE	199

### CASE 16 (EXP) L16=L3-L4

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	37.0	@NODE	155	STRESS:	76462.8	ALLOWABLE:	206838.
BENDING STRESS:					76353.0	@NODE	155
TORSIONAL STRESS:					14648.4	@NODE	20
AXIAL STRESS:					4379.6	@NODE	199
HOOP STRESS:					0.0	@NODE	20
3D MAX INTENSITY:					88732.6	@NODE	155

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

## CASE 27 (OCC) L27=L4+L17

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	34.9	@NODE	250	STRESS:	63950.4	ALLOWABLE:	183396.
BENDING STRESS:	36288.4	@NODE	250				
TORSIONAL STRESS:	1643.2	@NODE	100				
AXIAL STRESS:	29153.6	@NODE	155				
HOOP STRESS:	55949.9	@NODE	29				
3D MAX INTENSITY:	67208.1	@NODE	85				

## CASE 28 (OCC) L28=L4+L18

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	37.0	@NODE	250	STRESS:	67846.3	ALLOWABLE:	183396.
BENDING STRESS:	40215.1	@NODE	250				
TORSIONAL STRESS:	1675.2	@NODE	100				
AXIAL STRESS:	28736.0	@NODE	155				
HOOP STRESS:	55949.9	@NODE	29				
3D MAX INTENSITY:	68633.2	@NODE	250				

## CASE 29 (OCC) L29=L4+L19

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	37.7	@NODE	250	STRESS:	69221.8	ALLOWABLE:	183396.
BENDING STRESS:	41593.0	@NODE	250				
TORSIONAL STRESS:	1914.0	@NODE	49				
AXIAL STRESS:	28607.6	@NODE	199				
HOOP STRESS:	55949.9	@NODE	29				
3D MAX INTENSITY:	70007.3	@NODE	250				

## CASE 30 (OCC) L30=L4+L20

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	37.8	@NODE	250	STRESS:	69285.1	ALLOWABLE:	183396.
BENDING STRESS:	41672.0	@NODE	250				
TORSIONAL STRESS:	1884.0	@NODE	100				
AXIAL STRESS:	28616.3	@NODE	199				
HOOP STRESS:	55949.9	@NODE	29				
3D MAX INTENSITY:	70073.7	@NODE	250				

# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

## CASE 31 (OCC) L31=L4+L21

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	35.7	@NODE	250	STRESS:	65436.6	ALLOWABLE:	183396.
BENDING STRESS:					37177.2	@NODE	250
TORSIONAL STRESS:					1665.0	@NODE	100
AXIAL STRESS:					28498.8	@NODE	260
HOOP STRESS:					55949.9	@NODE	29
3D MAX INTENSITY:					68299.6	@NODE	155

## CASE 32 (OCC) L32=L4+L22

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	38.1	@NODE	240	STRESS:	69868.1	ALLOWABLE:	183396.
BENDING STRESS:					42350.5	@NODE	240
TORSIONAL STRESS:					1919.6	@NODE	20
AXIAL STRESS:					28469.3	@NODE	199
HOOP STRESS:					55949.9	@NODE	29
3D MAX INTENSITY:					71498.3	@NODE	240

## CASE 33 (OCC) L33=L4+L23

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	34.8	@NODE	250	STRESS:	63807.8	ALLOWABLE:	183396.
BENDING STRESS:					36185.2	@NODE	250
TORSIONAL STRESS:					1646.8	@NODE	100
AXIAL STRESS:					28435.1	@NODE	199
HOOP STRESS:					55949.9	@NODE	29
3D MAX INTENSITY:					64581.7	@NODE	250

## CASE 34 (OCC) L34=L4+L24

\*\*\*\* CODE STRESS CHECK PASSED

PIPING CODE: B31.3 -2002, April 30, 2002

HIGHEST STRESSES: (KPa)

CODE STRESS %:	34.7	@NODE	250	STRESS:	63632.4	ALLOWABLE:	183396.
BENDING STRESS:					36026.0	@NODE	250
TORSIONAL STRESS:					1629.6	@NODE	100
AXIAL STRESS:					28432.7	@NODE	199
HOOP STRESS:					55949.9	@NODE	29
3D MAX INTENSITY:					64405.5	@NODE	250

## Design of Propylene Gas Pipeline System

---

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

### CASE 35 (OCC) L35=L4+L25

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:34.5 @NODE 250 STRESS:63266.6 ALLOWABLE: 183396.

BENDING STRESS: 35588.8 @NODE 250

TORSIONAL STRESS: 1641.9 @NODE 100

AXIAL STRESS: 28454.0 @NODE 199

HOOP STRESS: 55949.9 @NODE 29

3D MAX INTENSITY: 64036.6 @NODE 250

### CASE 36 (OCC) L36=L4+L26

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:34.4 @NODE 250 STRESS:63047.7 ALLOWABLE: 183396.

BENDING STRESS: 35395.4 @NODE 250

TORSIONAL STRESS: 1625.7 @NODE 100

AXIAL STRESS: 28458.1 @NODE 199

HOOP STRESS: 55949.9 @NODE 29

3D MAX INTENSITY: 63817.3 @NODE 250

# Design of Propylene Gas Pipeline System

---

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# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

## INPUT LISTING

### PIPE DATA

From 10 To 20 DY= 213.000 mm.

PIPE

Dia= 762.000 mm. Wall= 12.700 mm. Insul= 50.000 mm. Cor= 1.5000 mm.

GENERAL

T1= 55 C T2= 120 C P1=2000.0000 KPa PHyd=3000.0000 KPa

Mat= (106)A106 B E= 203,395,424 KPa v = .292 Density= .0078 kg./cu.cm.

Insul= .0001 kg./cu.cm. Fluid= .0004750 kg./cu.cm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 10 ANC Cnode 2000

DISPLACEMENTS

Node 2000 DX1= .000 mm. DY1= .000 mm. DZ1= .000 mm. RX1= .000

RY1= .000 RZ1= .000 DX2= 2.312 mm. DY2= 2.312 mm. DZ2= 2.312 mm.

RX2= .000 RY2= .000 RZ2= .000

UNIFORM LOAD

GX1= .26 g's GY1= .00 g's GZ1= .00 g's GX2= .00 g's GY2= .17 g's

GZ2= .00 g's GX3= .00 g's GY3= .00 g's GZ3= .26 g's

WIND

Wind Shape= .650

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa

Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa

Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

From 20 To 30 DY= 3,800.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 29

Angle/Node @2= .00 28

HANGERS

Hanger Node = 30 Hanger Table = 0.0 Available Space = .0000 mm.

Allowed Load Variation = 25.0000 Max Allowed Travel = 40.0000 mm.

No. Hangers = 0.0 Short Range Flag = -1 User Operating Load = .00 N.

Free Node = 10 Free Node = 0 Free Code = 0.0 Spring Rate = .00 N./mm.

Theoretical Cold Load = .00 N.

From 30 To 35 DX= -1,200.000 mm.

From 35 To 40 DX= -1,176.000 mm.

From 40 To 50 DX= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 50 ANC Cnode 51

From 51 To 60 DX= -213.000 mm.

RIGID Weight= 4,141.09 N.

From 60 To 65 DX= -1,636.000 mm.

RESTRAINTS

Node 65 +Y

From 65 To 70 DX= -1,143.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 69

From 70 To 80 DZ= 1,532.000 mm.

# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

-----  
From 80 To 90 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 90 ANC Cnode 91  
-----

From 91 To 100 DZ= 91.000 mm.

RIGID Weight= 7,600.00 N.

RESTRAINTS

Node 100 ANC Cnode 101  
-----

From 101 To 110 DZ= 2,400.000 mm.

RIGID Weight=50,982.98 N.

RESTRAINTS

Node 110 ANC Cnode 111  
-----

From 111 To 120 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

-----  
From 120 To 130 DZ= 818.000 mm.

-----  
From 130 To 140 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 140 ANC Cnode 141  
-----

From 141 To 150 DZ= 2,400.000 mm.

RIGID Weight=50,983.00 N.

RESTRAINTS

Node 150 ANC Cnode 151  
-----

From 151 To 160 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

-----  
From 160 To 165 DZ= 2,059.000 mm.

RESTRAINTS

Node 165 +Y Mu = .30  
-----

From 165 To 170 DZ= 2,110.000 mm.

SIF's & TEE's

Node 170 Welding Tee  
-----

From 170 To 180 DZ= 2,339.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 179

Angle/Node @2= .00 178  
-----

From 180 To 182 DX= -1,500.000 mm.

RESTRAINTS

Node 182 Z  
-----

From 182 To 185 DX= -2,286.000 mm.

-----  
From 185 To 187 DX= -1,300.000 mm.

-----  
From 187 To 190 DX= -1,192.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 189

Angle/Node @2= .00 188  
-----

From 190 To 195 DZ= 2,286.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 194

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-----  
From 195 To 198 DY= -1,969.000 mm.  
-----

From 198 To 200 DY= -2,491.000 mm.  
-----

From 200 To 210 DY= -559.000 mm.

SIF's & TEE's

Node 210 Welding Tee  
-----

From 210 To 215 DX= 800.000 mm.

RESTRAINTS

Node 215 +Y Mu = .30

Node 215 Z  
-----

From 215 To 220 DX= 1,259.000 mm.  
-----

From 220 To 230 DX= 213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 230 ANC Cnode 231  
-----

From 231 To 240 DX= 2,400.000 mm.

RIGID Weight=50,982.98 N.

RESTRAINTS

Node 240 ANC Cnode 241  
-----

From 241 To 250 DX= 213.000 mm.

RIGID Weight= 4,141.09 N.  
-----

From 250 To 255 DX= 1,100.000 mm.

RESTRAINTS

Node 255 +Y Mu = .30  
-----

From 255 To 260 DX= 2,765.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000  
-----

From 260 To 265 DZ= 9,000.000 mm.

RESTRAINTS

Node 265 +Y Mu = .30

Node 265 Z  
-----

From 265 To 270 DZ= 2,287.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 269

Angle/Node @2= .00 268  
-----

From 270 To 275 DX= 4,000.000 mm.

RESTRAINTS

Node 275 +Y Mu = .30  
-----

From 275 To 280 DX= 1,951.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 279

Angle/Node @2= .00 278  
-----

From 280 To 285 DZ= 10,200.000 mm.

RESTRAINTS

Node 285 +Y

Node 285 X  
-----

From 285 To 288 DZ= 2,000.000 mm.  
-----

## Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

From 288 To 290 DZ= 3,071.000 mm.

From 290 To 300 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 300 ANC Cnode 301

From 301 To 310 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

From 310 To 315 DX= -2,201.000 mm. DZ= 2,883.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 314

From 315 To 330 DY= -1,492.000 mm.

From 330 To 340 DY= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 340 ANC Cnode 341

From 210 To 720 DX= -2,059.000 mm.

From 720 To 730 DX= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 730 ANC Cnode 731

From 731 To 740 DX= -2,400.000 mm.

RIGID Weight=50,982.98 N.

RESTRAINTS

Node 740 ANC Cnode 741

From 741 To 750 DX= -213.000 mm.

RIGID Weight= 4,141.09 N.

From 750 To 755 DX= -1,100.000 mm.

RESTRAINTS

Node 755 +Y Mu = .30

From 755 To 760 DX= -2,765.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000

From 760 To 765 DZ= 9,000.000 mm.

RESTRAINTS

Node 765 +Y Mu = .30

Node 765 Z

From 765 To 770 DZ= 2,287.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 769

Angle/Node @2= .00 768

From 770 To 775 DX= -4,000.000 mm.

RESTRAINTS

Node 775 +Y Mu = .30

From 775 To 780 DX= -1,951.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 779

Angle/Node @2= .00 778

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From 780 To 785 DZ= 10,200.000 mm.

RESTRAINTS

Node 785 +Y

Node 785 X

-----  
From 785 To 788 DZ= 2,000.000 mm.

-----  
From 788 To 790 DZ= 3,071.000 mm.

-----  
From 790 To 800 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 800 ANC Cnode 801

-----  
From 801 To 810 DZ= 213.000 mm.

RIGID Weight= 4,141.09 N.

-----  
From 810 To 815 DX= 2,201.000 mm. DZ= 2,883.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00 814

-----  
From 815 To 830 DY= -1,492.000 mm.

-----  
From 830 To 840 DY= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 840 ANC Cnode 841

-----  
From 170 To 175 DX= -2,200.000 mm.

RESTRAINTS

Node 175 +Y Mu = .30

-----  
From 175 To 1000 DX= -982.000 mm.

SIF's & TEE's

Node 1000 Welding Tee

-----  
From 1000 To 1005 DZ= -1,200.000 mm.

-----  
From 1005 To 1010 DZ= -859.000 mm.

-----  
From 1010 To 1020 DZ= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 1020 ANC Cnode 1021

-----  
From 1021 To 1030 DZ= -2,400.000 mm.

RIGID Weight=50,982.98 N.

RESTRAINTS

Node 1030 ANC Cnode 1031

-----  
From 1031 To 1040 DZ= -213.000 mm.

RIGID Weight= 4,141.09 N.

-----  
From 1040 To 1045 DZ= -550.000 mm.

-----  
From 1045 To 1050 DZ= -450.000 mm.

-----  
From 1050 To 1060 DZ= -610.000 mm.

REDUCER

Diam2= 609.600 mm.

-----  
From 1060 To 1070 DZ= -171.450 mm.

PIPE

## Design of Propylene Gas Pipeline System

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Dia= 609.600 mm. Wall= 12.700 mm. Insul= 50.000 mm.

RIGID Weight= 2,428.61 N.

RESTRAINTS

Node 1070 ANC Cnode 1071

-----  
From 1071 To 1080 DZ= -1,500.000 mm.

RIGID Weight=31,345.06 N.

RESTRAINTS

Node 1080 ANC Cnode 1081

-----  
From 1081 To 1090 DZ= -171.450 mm.

RIGID Weight= 2,428.61 N.

-----  
From 1090 To 1100 DZ= -610.000 mm.

REDUCER

Diam2= 762.000 mm.

-----  
From 1100 To 1105 DZ= -550.000 mm.

PIPE

Dia= 762.000 mm. Wall= 12.700 mm. Insul= 50.000 mm.

RESTRAINTS

Node 1105 +Y Mu = .30

-----  
From 1105 To 1110 DZ= -450.000 mm.

-----  
From 1110 To 1120 DZ= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 1120 ANC Cnode 1121

-----  
From 1121 To 1130 DZ= -2,400.000 mm.

RIGID Weight=50,982.98 N.

RESTRAINTS

Node 1130 ANC Cnode 1131

-----  
From 1131 To 1140 DZ= -213.000 mm.

RIGID Weight= 4,141.09 N.

-----  
From 1140 To 1150 DZ= -1,643.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1149 Angle/Node @2= .00 1148

-----  
From 1150 To 1160 DY= -3,582.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1159 Angle/Node @2= .00 1158

-----  
From 1160 To 1165 DZ= 3,200.000 mm.

RESTRAINTS

Node 1165 +Y Mu = .30

-----  
From 1165 To 1167 DZ= 7,000.000 mm.

RESTRAINTS

Node 1167 X

-----  
From 1167 To 1170 DZ= 4,216.900 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1169 Angle/Node @2= .00 1168

-----  
From 1170 To 1175 DX= -2,600.000 mm.

RESTRAINTS

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Node 1175 +Y Mu = .30  
Node 1175 Z

-----  
From 1175 To 1180 DX= -2,928.000 mm.

SIF's & TEE's

Node 1180 Welding Tee

-----  
From 1180 To 1190 DX= -2,717.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1189 Angle/Node @2= .00 1188

-----  
From 1190 To 1200 DY= -2,234.000 mm.

PIPE

Dia= 762.000 mm. Wall= 12.700 mm. Insul= 50.000 mm.

SIF's & TEE's

Node 1200 Weldolet

-----  
From 1000 To 1006 DX= -500.000 mm.

-----  
From 1006 To 1300 DX= -559.000 mm.

-----  
From 1300 To 1310 DX= -213.000 mm.

RIGID Weight= 4,141.09 N.

RESTRAINTS

Node 1310 ANC Cnode 1311

-----  
From 1311 To 1320 DX= -2,400.000 mm.

RIGID Weight=50,982.98 N.

RESTRAINTS

Node 1320 ANC Cnode 1321

-----  
From 1321 To 1330 DX= -213.000 mm.

RIGID Weight= 4,141.09 N.

-----  
From 1330 To 1340 DX= -1,643.000 mm.

BEND at "TO" end

Radius= 1,143.000 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1339 Angle/Node @2= .00 1338

-----  
From 1340 To 1180 DY= -3,582.000 mm.

-----  
From 1200 To 1350 DZ= -1,596.000 mm.

PIPE

Dia= 914.400 mm. Wall= 12.700 mm. Insul= 50.000 mm.

GENERAL

T1= 27 C

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa

Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa

Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 1350 To 1400 DZ= -707.000 mm.

-----  
From 1400 To 1410 DZ= -610.000 mm.

REDUCER

Diam2= 1,066.800 mm. Wall2= 12.700 mm.

-----  
From 1410 To 1415 DZ= -700.000 mm.

PIPE

Dia= 1,066.800 mm. Wall= 12.700 mm. Insul= 50.000 mm.

-----  
From 1415 To 1420 DZ= -171.000 mm.

# Design of Propylene Gas Pipeline System

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PIPE

Dia= 1,066.800 mm. Wall= 12.700 mm. Insul= 50.000 mm.

RIGID Weight= 3,207.01 N.

RESTRAINTS

Node 1420 ANC

-----  
From 1200 To 1250 DZ= 1,596.000 mm.

PIPE

Dia= 914.400 mm. Wall= 12.700 mm. Insul= 50.000 mm.

RESTRAINTS

Node 1250 +Y Mu = .30

-----  
From 1250 To 1500 DZ= 1,964.000 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1499 Angle/Node @2= .00 1498

-----  
From 1500 To 1510 DY= 5,316.000 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1509 Angle/Node @2= .00 1508

-----  
From 1510 To 1515 DZ= 10,200.000 mm.

RESTRAINTS

Node 1515 +Y Mu = .30

-----  
From 1515 To 1520 DZ= 1,652.000 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1519 Angle/Node @2= .00 1518

-----  
From 1520 To 1525 DX= 3,600.000 mm.

RESTRAINTS

Node 1525 Z

-----  
From 1525 To 1530 DX= 5,012.000 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1529 Angle/Node @2= .00 1528

-----  
From 1530 To 1535 DZ= 4,072.000 mm.

RESTRAINTS

Node 1535 +Y Mu = .30

-----  
From 1535 To 1540 DZ= 2,797.000 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1539 Angle/Node @2= .00 1538

-----  
From 1540 To 1550 DY= 6,000.000 mm.

-----  
From 1550 To 1555 DY= 6,000.000 mm.

RESTRAINTS

Node 1555 X

Node 1555 Z

-----  
From 1555 To 1560 DY= 6,000.000 mm.

-----  
From 1560 To 1565 DY= 6,000.000 mm.

-----  
From 1565 To 1570 DY= 6,000.000 mm.

-----  
From 1570 To 1575 DY= 6,000.000 mm.



# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

-----  
From 1575 To 1700 DY= 5,000.000 mm.  
-----

From 1700 To 1710 DY= 6,000.000 mm.

RESTRAINTS

Node 1700 X

Node 1700 Z  
-----

From 1710 To 1715 DY= 6,000.000 mm.  
-----

From 1715 To 1720 DY= 6,000.000 mm.  
-----

From 1720 To 1725 DY= 6,000.000 mm.  
-----

From 1725 To 1730 DY= 6,000.000 mm.  
-----

From 1730 To 1740 DY= 6,000.000 mm.

RESTRAINTS

Node 1740 X

Node 1740 Z  
-----

From 1740 To 2500 DY= 4,432.000 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1549 Angle/Node @2= .00 1548  
-----

From 2500 To 2505 DX= -1,272.792 mm. DZ= 1,272.792 mm.

HANGERS

Hanger Node = 2505 Hanger Table = 0.0 Available Space = .0000 mm.

Allowed Load Variation = 25.0000 Max Allowed Travel = 40.0000 mm.

No. Hangers = 2 Short Range Flag = -1 User Operating Load = .00 N.

Free Node = 0 Free Node = 0 Free Code = 0.0 Spring Rate = .00 N./mm.

Theoretical Cold Load = .00 N.  
-----

From 2505 To 2510 DX= -2,192.031 mm. DZ= 2,192.031 mm.

BEND at "TO" end

Radius= 1,371.600 mm. (LONG) Bend Angle= 90.000 Angle/Node @1= 45.00

1559 Angle/Node @2= .00 1558  
-----

From 2510 To 2520 DY= -1,500.000 mm.  
-----

From 2520 To 2530 DY= -210.000 mm.

RIGID Weight= 2,317.41 N.

RESTRAINTS

Node 2530 ANC Cnode 3500  
-----

From 341 To 1590 DY= -213.000 mm.

PIPE

Dia= 762.000 mm. Wall= 12.700 mm. Insul= 50.000 mm.

RIGID Weight= 4,141.09 N.  
-----

From 1590 To 1600 DY= -257.000 mm.

RESTRAINTS

Node 1600 ANC Cnode 1610

DISPLACEMENTS

Node 1610 DX1= -1.500 mm. DY1= 2.000 mm. DZ1= .000 mm.

DX2= -1.734 mm. DY2= 2.312 mm. DZ2= .000 mm.  
-----

From 841 To 1650 DY= -213.000 mm.

RIGID Weight= 4,141.09 N.  
-----

From 1650 To 1660 DY= -257.000 mm.

RESTRAINTS

# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

Node 1660 ANC Cnode 1670

DISPLACEMENTS

Node 1670 DX1= -.150 mm. DY1= 2.000 mm. DZ1= .000 mm. RX1= .000  
RY1= .000 RZ1= .000 DX2= .173 mm. DY2= 2.312 mm. DZ2= .000 mm.  
RX2= .000 RY2= .000 RZ2= .000

-----  
From 3500 To 3510 DY= -210.000 mm.

PIPE

Dia= 914.000 mm. Wall= 12.700 mm. Insul= 50.000 mm.

RIGID Weight= 2,317.11 N.

-----  
From 3520 To 3530 DY= -315.000 mm.

RESTRAINTS

Node 3530 ANC Cnode 3540

-----  
From 3540 To 3550 DY= -2,197.000 mm.

PIPE

Dia= 7,500.000 mm. Wall= 45.000 mm. Insul= 50.000 mm. Cor= 3.0000 mm.

GENERAL

P1= .0000 KPa PHyd= .0000 KPa

RIGID Weight= .00 N.

-----  
From 3550 To 3800 DY= -30,127.998 mm.

RIGID Weight= .00 N.

-----  
From 3800 To 3810 DY= -5,872.000 mm.

RIGID Weight= .00 N.

-----  
From 3810 To 3900 DY= -14,128.000 mm.

RIGID Weight= .00 N.

-----  
From 3900 To 3950 DY= -14,872.000 mm.

RIGID Weight= .00 N.

-----  
From 3950 To 4500 DY= -17,178.000 mm.

RIGID Weight= .00 N.

-----  
From 4500 To 4510 DY= -1,875.000 mm.

GENERAL

T1= 39 C T2= 100 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 4510 To 5000 DY= -9,100.000 mm.

GENERAL

T1= 21 C T2= 21 C

RIGID Weight= .00 N.

RESTRAINTS

Node 5000 ANC

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 3550 To 3560 DX= 2,651.650 mm. DZ= -2,651.651 mm.

GENERAL

T1= 27 C T2= 120 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa

# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 3560 To 1740 DX= 813.173 mm. DZ= -813.173 mm.

GENERAL

T1= 21 C T2= 21 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 3810 To 3820 DX= 2,651.650 mm. DZ= -2,651.651 mm.

GENERAL

T1= 27 C T2= 120 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 3820 To 1700 DX= 813.173 mm. DZ= -813.173 mm.

GENERAL

T1= 21 C T2= 21 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 3950 To 3960 DX= 2,651.650 mm. DZ= -2,651.651 mm.

GENERAL

T1= 27 C T2= 120 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

-----  
From 3960 To 1555 DX= 813.173 mm. DZ= -813.173 mm.

GENERAL

T1= 21 C T2= 21 C

RIGID Weight= .00 N.

ALLOWABLE STRESSES

B31.3 (2002) Sc= 137,892 KPa Sh1= 137,892 KPa Sh2= 137,892 KPa  
Sh3= 137,892 KPa Sh4= 137,892 KPa Sh5= 137,892 KPa Sh6= 137,892 KPa  
Sh7= 137,892 KPa Sh8= 137,892 KPa Sh9= 137,892 KPa

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

## LOAD CASE REPORT

CASE 1 (HGR) W

WEIGHT FOR HANGER LOADS

CASE 2 (HGR) W+D1+T1+P1

OPERATING FOR HANGER TRAVEL

CASE 3 (HYD) WW+HP+H

HYDRO TEST CASE

CASE 4 (OPE) W+D1+T1+P1+H

OPERATING CASE CONDITION 1

CASE 5 (OPE) W+D2+T2+P1+H

OPERATING CASE CONDITION 2

CASE 6 (OPE) W+D1+T1+P1+H+U1

CASE 7 (OPE) W+D1+T1+P1+H-U1

CASE 8 (OPE) W+D1+T1+P1+H+U2

CASE 9 (OPE) W+D1+T1+P1+H-U2

CASE 10 (OPE) W+D1+T1+P1+H+U3

CASE 11 (OPE) W+D1+T1+P1+H-U3

CASE 12 (OPE) W+D1+T1+P1+H+WIN1

CASE 13 (OPE) W+D1+T1+P1+H-WIN1

CASE 14 (OPE) W+D1+T1+P1+H+WIN2

CASE 15 (OPE) W+D1+T1+P1+H-WIN2

CASE 16 (SUS) W+P1+H

SUSTAINED CASE CONDITION 1

CASE 17 (EXP) L17=L4-L16

EXPANSION CASE CONDITION 1

CASE 18 (EXP) L18=L5-L16

EXPANSION CASE CONDITION 2

CASE 19 (OCC) L19=L6-L4

CASE 20 (OCC) L20=L7-L4

CASE 21 (OCC) L21=L8-L4

CASE 22 (OCC) L22=L9-L4

CASE 23 (OCC) L23=L10-L4

CASE 24 (OCC) L24=L11-L4

CASE 25 (OCC) L25=L12-L4

CASE 26 (OCC) L26=L13-L4

CASE 27 (OCC) L27=L14-L4

CASE 28 (OCC) L28=L15-L4

CASE 29 (OCC) L29=L16+L19

CASE 30 (OCC) L30=L16+L20

CASE 31 (OCC) L31=L16+L21

CASE 32 (OCC) L32=L16+L22

CASE 33 (OCC) L33=L16+L23

## Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

CASE 34 (OCC) L34=L16+L24

CASE 35 (OCC) L35=L16+L25

CASE 36 (OCC) L36=L16+L26

CASE 37 (OCC) L37=L16+L27

CASE 38 (OCC) L38=L16+L28

# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 4 (OPE) W+D1+T1+P1+H

NODE	-----Translations (mm.)-----			-----Rotations (deg.)-----		
	DX	DY	DZ	RX	RY	RZ
10	0.000	0.000	0.000	0.0000	0.0000	0.0000
20	0.000	0.081	0.000	0.0000	-0.0001	0.0000
28	0.046	1.093	-0.054	0.0012	-0.0208	-0.0014
29	-0.060	1.409	-0.036	0.0171	-0.0254	0.0008
30	-0.395	1.419	-0.490	0.0149	-0.0551	0.0204
35	-0.417	1.399	-0.546	0.0153	-0.0553	0.0205
40	-0.863	0.945	-1.732	0.0229	-0.0585	0.0238
50	-0.944	0.857	-1.949	0.0230	-0.0586	0.0239
51	-0.944	0.857	-1.949	0.0230	-0.0586	0.0239
60	-1.025	0.768	-2.167	0.0230	-0.0586	0.0239
65	-1.645	0.000	-3.856	0.0336	-0.0576	0.0326
69	-2.172	-1.153	-4.349	0.0479	-0.0246	0.0729
70	-2.326	-2.088	-4.104	0.0075	0.0192	0.0580
80	-2.190	-2.153	-3.958	0.0041	0.0207	0.0555
90	-2.113	-2.169	-3.877	0.0039	0.0207	0.0554
91	-2.113	-2.169	-3.877	0.0039	0.0207	0.0554
100	-2.080	-2.176	-3.842	0.0038	0.0208	0.0554
101	-2.080	-2.176	-3.842	0.0038	0.0208	0.0554
110	-1.199	-2.282	-2.931	0.0007	0.0213	0.0544
111	-1.199	-2.282	-2.931	0.0007	0.0213	0.0544
120	-1.119	-2.284	-2.850	0.0004	0.0213	0.0543
130	-0.797	-2.146	-2.541	-0.0194	0.0236	0.0490
140	-0.710	-2.074	-2.460	-0.0197	0.0236	0.0489
141	-0.710	-2.074	-2.460	-0.0197	0.0236	0.0489
150	0.287	-1.172	-1.549	-0.0227	0.0239	0.0480
151	0.287	-1.172	-1.549	-0.0227	0.0239	0.0480
160	0.376	-1.086	-1.468	-0.0229	0.0240	0.0479
165	1.301	0.000	-0.691	-0.0234	0.0271	0.0346
170	2.289	0.530	0.101	-0.0111	0.0207	0.0210
175	1.463	0.000	0.749	-0.0138	0.0115	0.0073
178	2.669	0.719	0.548	-0.0096	0.0156	0.0232
179	2.430	0.755	0.751	-0.0174	-0.0302	0.0217
180	1.892	0.607	0.279	-0.0233	-0.0433	0.0150
182	1.756	0.511	0.000	-0.0245	-0.0426	0.0148
185	0.888	-0.018	-1.588	-0.0321	-0.0376	0.0111
187	0.395	-0.242	-2.414	-0.0365	-0.0356	0.0093
188	0.376	-0.250	-2.445	-0.0366	-0.0356	0.0092
189	-0.089	-0.054	-2.731	-0.0445	-0.0234	-0.0026
190	-0.480	0.707	-2.542	-0.0560	-0.0152	-0.0066
194	-0.669	1.376	-1.911	-0.0509	-0.0076	-0.0026
195	-0.682	1.329	-1.236	-0.0248	-0.0041	0.0051
198	-0.604	1.019	-0.894	-0.0224	-0.0037	0.0055
200	-0.346	0.086	-0.096	-0.0136	-0.0025	0.0061
210	-0.286	-0.123	0.027	-0.0113	-0.0022	0.0060
215	0.015	0.000	0.000	-0.0091	0.0072	0.0041
220	0.489	0.000	-0.332	-0.0056	0.0217	0.0000
230	0.570	0.000	-0.413	-0.0056	0.0218	0.0000
231	0.570	0.000	-0.413	-0.0056	0.0218	0.0000
240	1.480	0.004	-1.359	-0.0051	0.0232	0.0001
241	1.480	0.004	-1.359	-0.0051	0.0232	0.0001
250	1.561	0.005	-1.445	-0.0051	0.0233	0.0001
255	1.976	0.000	-1.968	-0.0021	0.0300	-0.0056
260	3.146	-1.007	-2.952	0.0068	-0.0204	-0.0267
265	-0.612	0.000	0.000	-0.0204	-0.0276	-0.0142
268	-1.150	0.408	0.433	-0.0203	-0.0250	-0.0124
269	-1.123	0.625	0.735	-0.0196	0.0153	-0.0109
270	-0.641	0.602	0.321	-0.0187	0.0582	-0.0101
275	0.440	0.000	-2.776	-0.0142	0.0640	-0.0191
278	0.746	-0.320	-3.693	-0.0130	0.0637	-0.0238

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 4 (OPE) W+D1+T1+P1+H

NODE	-----Translations (mm.)-----			-----Rotations (deg.)-----		
	DX	DY	DZ	RX	RY	RZ
279	1.322	-0.928	-4.303	0.0000	0.0337	-0.0609
280	1.613	-1.372	-4.114	0.0025	-0.0083	-0.0669
285	0.000	0.000	-0.704	-0.0062	0.0028	-0.0881
288	0.289	-0.008	0.049	0.0032	0.0118	-0.0928
290	1.079	-0.272	1.205	0.0044	0.0144	-0.1000
300	1.132	-0.288	1.286	0.0043	0.0144	-0.1000
301	1.132	-0.288	1.286	0.0043	0.0144	-0.1000
310	1.186	-0.304	1.366	0.0043	0.0144	-0.1001
314	0.440	2.596	2.548	0.0477	0.0037	-0.0771
315	-0.532	2.241	1.644	0.0899	0.0007	-0.0545
330	-0.859	2.110	1.088	0.0908	0.0007	-0.0540
340	-1.059	2.029	0.750	0.0908	0.0007	-0.0540
341	-1.059	2.029	0.750	0.0908	0.0007	-0.0540
720	-1.060	-0.252	-0.439	-0.0057	-0.0222	-0.0026
730	-1.141	-0.242	-0.522	-0.0057	-0.0223	-0.0027
731	-1.141	-0.242	-0.522	-0.0057	-0.0223	-0.0027
740	-2.052	-0.105	-1.483	-0.0052	-0.0234	-0.0036
741	-2.052	-0.105	-1.483	-0.0052	-0.0234	-0.0036
750	-2.133	-0.091	-1.570	-0.0052	-0.0235	-0.0036
755	-2.546	0.000	-2.085	-0.0022	-0.0292	0.0007
760	-3.637	-0.749	-2.955	0.0071	0.0241	0.0213
765	0.433	0.000	0.000	-0.0156	0.0275	0.0094
768	0.961	0.299	0.432	-0.0145	0.0238	0.0077
769	0.822	0.414	0.672	-0.0087	-0.0309	0.0078
770	0.222	0.366	-0.064	-0.0072	-0.0865	0.0061
775	-0.858	0.000	-4.610	-0.0017	-0.0927	0.0129
778	-1.163	-0.226	-5.930	-0.0001	-0.0917	0.0164
779	-1.851	-0.691	-6.848	0.0084	-0.0478	0.0396
780	-2.223	-1.076	-6.711	0.0067	0.0098	0.0412
785	0.000	0.000	-3.307	-0.0095	-0.0003	0.0428
788	-0.235	0.172	-2.555	-0.0041	-0.0106	0.0432
790	-0.958	0.494	-1.400	-0.0108	-0.0122	0.0438
800	-1.003	0.534	-1.320	-0.0108	-0.0122	0.0438
801	-1.003	0.534	-1.320	-0.0108	-0.0122	0.0438
810	-1.049	0.574	-1.239	-0.0108	-0.0121	0.0438
814	-0.408	2.500	0.003	0.0001	0.0027	0.0258
815	-0.147	2.241	0.034	0.0019	-0.0010	0.0008
830	-0.148	2.110	0.017	0.0012	-0.0004	0.0002
840	-0.148	2.029	0.012	0.0012	-0.0004	0.0001
841	-0.148	2.029	0.012	0.0012	-0.0004	0.0001
1000	1.098	-0.111	0.909	-0.0150	0.0051	-0.0026
1005	0.992	-0.497	0.460	-0.0150	0.0051	-0.0037
1006	0.912	-0.062	0.931	-0.0127	0.0014	-0.0098
1010	0.914	-0.719	0.138	-0.0090	0.0052	-0.0044
1020	0.895	-0.753	0.057	-0.0089	0.0052	-0.0044
1021	0.895	-0.753	0.057	-0.0089	0.0052	-0.0044
1030	0.679	-1.083	-0.853	-0.0066	0.0052	-0.0045
1031	0.679	-1.083	-0.853	-0.0066	0.0052	-0.0045
1040	0.660	-1.107	-0.934	-0.0064	0.0052	-0.0046
1045	0.610	-1.121	-1.140	0.0014	0.0052	-0.0050
1050	0.569	-1.079	-1.308	0.0072	0.0052	-0.0054
1060	0.514	-0.941	-1.536	0.0168	0.0052	-0.0062
1070	0.498	-0.891	-1.601	0.0170	0.0052	-0.0062
1071	0.498	-0.891	-1.601	0.0170	0.0052	-0.0062
1080	0.361	-0.425	-2.170	0.0179	0.0052	-0.0063
1081	0.361	-0.425	-2.170	0.0179	0.0052	-0.0063
1090	0.346	-0.370	-2.235	0.0179	0.0052	-0.0064
1100	0.290	-0.155	-2.463	0.0150	0.0052	-0.0071
1105	0.239	0.000	-2.669	0.0101	0.0053	-0.0076

## Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 4 (OPE) W+D1+T1+P1+H

-----Translations (mm.)-----

-----Rotations (deg.)-----

NODE	DX	DY	DZ	RX	RY	RZ
1110	0.198	0.039	-2.841	0.0058	0.0053	-0.0080
1120	0.178	0.059	-2.922	0.0058	0.0053	-0.0080
1121	0.178	0.059	-2.922	0.0058	0.0053	-0.0080
1130	-0.042	0.290	-3.834	0.0057	0.0053	-0.0081
1131	-0.042	0.290	-3.834	0.0057	0.0053	-0.0081
1140	-0.062	0.311	-3.915	0.0057	0.0053	-0.0081
1148	-0.108	0.369	-4.105	0.0068	0.0052	-0.0086
1149	-0.241	0.458	-4.517	0.0207	0.0066	-0.0103
1150	-0.471	0.278	-4.936	0.0172	0.0085	-0.0163
1158	-0.849	-0.211	-5.312	0.0153	0.0083	-0.0171
1159	-1.094	-0.506	-5.235	-0.0088	0.0060	-0.0233
1160	-1.175	-0.415	-4.847	-0.0140	0.0032	-0.0254
1165	-1.061	0.000	-4.068	-0.0025	0.0031	-0.0269
1167	0.000	-1.240	-1.439	0.0045	0.0206	-0.0322
1168	1.387	-1.190	-0.285	-0.0042	0.0263	-0.0345
1169	1.499	-0.876	0.091	-0.0067	0.0048	-0.0347
1170	1.184	-0.438	0.157	-0.0004	-0.0064	-0.0188
1175	0.634	0.000	0.000	0.0026	-0.0022	-0.0121
1180	-0.463	0.248	0.162	0.0087	0.0030	-0.0029
1188	-1.041	0.660	0.253	0.0055	0.0028	-0.0163
1189	-1.364	0.691	0.231	0.0045	-0.0015	0.0094
1190	-1.074	0.260	0.195	-0.0011	-0.0019	0.0332
1200	-0.421	-0.139	0.227	-0.0016	-0.0040	0.0254
1250	-0.442	0.000	0.323	0.0000	-0.0014	0.0227
1300	0.705	0.070	0.921	-0.0103	-0.0022	-0.0182
1310	0.624	0.139	0.912	-0.0102	-0.0022	-0.0184
1311	0.624	0.139	0.912	-0.0102	-0.0022	-0.0184
1320	-0.286	0.961	0.804	-0.0095	-0.0027	-0.0204
1321	-0.286	0.961	0.804	-0.0095	-0.0027	-0.0204
1330	-0.367	1.038	0.793	-0.0094	-0.0027	-0.0205
1338	-0.553	1.251	0.763	-0.0072	-0.0028	-0.0224
1339	-0.967	1.451	0.742	-0.0020	-0.0033	-0.0099
1340	-0.987	1.145	0.647	0.0109	-0.0046	0.0160
1350	-0.200	-0.099	0.132	0.0020	-0.0068	0.0129
1400	-0.102	-0.058	0.090	0.0021	-0.0052	0.0073
1410	-0.040	-0.026	0.053	0.0014	-0.0031	0.0035
1415	-0.001	0.000	0.011	0.0000	-0.0001	0.0001
1420	0.000	0.000	0.000	0.0000	0.0000	0.0000
1498	-0.459	-0.042	0.361	0.0025	-0.0018	0.0216
1499	-0.655	-0.244	0.521	0.0101	-0.0024	0.0186
1500	-0.858	-0.200	0.475	-0.0187	0.0017	0.0033
1508	-0.927	-0.046	-0.441	-0.0196	0.0001	-0.0003
1509	-0.754	0.054	-0.585	0.0014	0.0046	-0.0167
1510	-0.523	-0.075	-0.475	0.0108	0.0050	-0.0203
1515	-0.017	0.000	0.088	-0.0091	0.0019	-0.0371
1518	-0.009	0.037	0.106	-0.0088	0.0018	-0.0376
1519	0.034	-0.152	0.164	-0.0069	0.0011	-0.0390
1520	0.110	-0.688	0.152	-0.0130	0.0037	-0.0287
1525	0.255	-1.744	0.000	-0.0187	0.0042	-0.0238
1528	0.493	-2.894	-0.282	-0.0280	0.0040	-0.0136
1529	0.553	-2.694	-0.271	-0.0378	-0.0030	0.0065
1530	0.469	-1.901	-0.170	-0.0426	-0.0091	0.0094
1535	0.027	0.000	0.007	-0.0318	-0.0090	0.0076
1538	-0.189	0.636	0.100	-0.0240	-0.0085	0.0067
1539	-0.332	0.778	0.147	0.0019	-0.0038	0.0039
1540	-0.364	0.818	0.207	-0.0006	-0.0014	-0.0020
1548	0.049	5.978	-0.049	-0.0018	0.0000	-0.0018
1549	0.124	6.113	-0.124	-0.0071	0.0000	-0.0071
1550	-0.161	1.114	0.104	-0.0015	-0.0008	-0.0025



# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 4 (OPE) W+D1+T1+P1+H

NODE	-----Translations (mm.)-----			-----Rotations (deg.)-----		
	DX	DY	DZ	RX	RY	RZ
1555	0.000	1.523	0.000	0.0002	0.0000	0.0002
1558	0.011	5.435	-0.011	0.0157	0.0000	0.0157
1559	0.129	4.887	-0.129	0.0252	0.0000	0.0252
1560	-0.015	1.855	0.015	0.0001	0.0000	0.0001
1565	-0.018	2.216	0.018	0.0000	0.0000	0.0000
1570	-0.014	2.605	0.014	-0.0001	0.0000	-0.0001
1575	-0.006	3.023	0.006	-0.0001	0.0000	-0.0001
1590	-1.260	2.015	0.412	0.0908	0.0007	-0.0540
1600	-1.500	2.000	0.000	0.0909	0.0007	-0.0540
1610	-1.500	2.000	0.000	0.0909	0.0007	-0.0540
1650	-0.147	2.015	0.008	0.0011	-0.0004	0.0001
1660	-0.150	2.000	0.000	0.0000	0.0000	0.0000
1670	-0.150	2.000	0.000	0.0000	0.0000	0.0000
1700	0.000	3.394	0.000	-0.0001	0.0000	-0.0001
1710	0.004	3.718	-0.004	0.0000	0.0000	0.0000
1715	0.005	4.071	-0.005	0.0000	0.0000	0.0000
1720	0.004	4.452	-0.004	0.0000	0.0000	0.0000
1725	0.002	4.862	-0.002	0.0000	0.0000	0.0000
1730	0.001	5.300	-0.001	0.0000	0.0000	0.0000
1740	0.000	5.767	0.000	0.0000	0.0000	0.0000
2000	0.000	0.000	0.000	0.0000	0.0000	0.0000
2500	0.111	6.177	-0.111	0.0108	0.0000	0.0108
2505	0.091	6.070	-0.091	0.0120	0.0000	0.0120
2510	0.553	4.564	-0.553	0.0263	0.0000	0.0263
2520	0.612	4.555	-0.612	0.0263	0.0000	0.0263
2530	0.709	4.542	-0.709	0.0263	0.0000	0.0263
3500	0.709	4.542	-0.709	0.0263	0.0000	0.0263
3510	0.805	4.528	-0.805	0.0263	0.0000	0.0263
3520	-0.174	5.933	0.174	0.0000	0.0000	0.0000
3530	-0.174	5.912	0.174	0.0000	0.0000	0.0000
3540	-0.174	5.912	0.174	0.0000	0.0000	0.0000
3550	-0.174	5.768	0.174	0.0000	0.0000	0.0000
3560	0.000	5.767	0.000	0.0000	0.0000	0.0000
3800	-0.172	3.788	0.172	0.0000	0.0000	0.0000
3810	-0.175	3.402	0.175	0.0000	0.0000	0.0000
3820	0.000	3.396	0.000	-0.0001	0.0000	-0.0001
3900	-0.191	2.474	0.191	0.0000	0.0000	0.0000
3950	-0.173	1.498	0.173	0.0002	0.0000	0.0002
3960	0.000	1.517	0.000	0.0002	0.0000	0.0002
4500	-0.056	0.371	0.056	0.0003	0.0000	0.0003
4510	-0.044	-0.002	0.044	0.0003	0.0000	0.0003
5000	0.000	0.000	0.000	0.0001	0.0000	0.0001

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 16 (SUS) W+P1+H

-----Translations (mm.)-----      -----Rotations (deg.)-----

NODE	DX	DY	DZ	RX	RY	RZ
10	0.000	0.000	0.000	0.0000	0.0000	0.0000
20	0.000	0.000	0.000	0.0000	0.0000	0.0000
28	0.068	0.005	0.127	0.0062	-0.0062	-0.0029
29	0.186	0.067	0.374	0.0296	-0.0013	-0.0120
30	0.253	0.204	0.540	0.0344	-0.0051	-0.0009
35	0.253	0.205	0.535	0.0346	-0.0051	-0.0008
40	0.253	0.196	0.412	0.0396	-0.0064	0.0025
50	0.253	0.186	0.388	0.0397	-0.0064	0.0026
51	0.253	0.186	0.388	0.0397	-0.0064	0.0026
60	0.253	0.177	0.364	0.0397	-0.0064	0.0026
65	0.253	0.000	0.165	0.0467	-0.0070	0.0132
69	0.215	-1.057	0.069	0.0616	-0.0056	0.0647
70	0.165	-2.078	0.044	0.0101	-0.0014	0.0493
80	0.156	-2.158	0.043	0.0060	-0.0012	0.0477
90	0.152	-2.181	0.043	0.0058	-0.0012	0.0476
91	0.152	-2.181	0.043	0.0058	-0.0012	0.0476
100	0.150	-2.191	0.043	0.0057	-0.0012	0.0476
101	0.150	-2.191	0.043	0.0057	-0.0012	0.0476
110	0.100	-2.369	0.043	0.0023	-0.0012	0.0469
111	0.100	-2.369	0.043	0.0023	-0.0012	0.0469
120	0.095	-2.377	0.043	0.0019	-0.0012	0.0469
130	0.081	-2.251	0.043	-0.0194	-0.0009	0.0434
140	0.078	-2.178	0.043	-0.0198	-0.0009	0.0433
141	0.078	-2.178	0.043	-0.0198	-0.0009	0.0433
150	0.043	-1.267	0.043	-0.0231	-0.0008	0.0426
151	0.043	-1.267	0.043	-0.0231	-0.0008	0.0426
160	0.040	-1.180	0.043	-0.0233	-0.0008	0.0426
165	0.024	0.000	0.042	-0.0283	-0.0001	0.0338
170	0.025	0.767	0.043	-0.0159	-0.0007	0.0247
175	0.028	0.000	-0.005	-0.0157	-0.0020	0.0196
178	0.005	1.039	0.044	-0.0130	-0.0010	0.0277
179	-0.012	1.002	0.038	-0.0098	-0.0012	0.0306
180	-0.020	0.625	0.016	-0.0121	-0.0027	0.0295
182	-0.020	0.439	0.000	-0.0130	-0.0028	0.0293
185	-0.021	-0.671	-0.134	-0.0182	-0.0038	0.0253
187	-0.021	-1.211	-0.224	-0.0212	-0.0041	0.0227
188	-0.021	-1.230	-0.227	-0.0213	-0.0041	0.0226
189	-0.055	-1.267	-0.303	-0.0298	-0.0063	0.0052
190	-0.147	-0.772	-0.341	-0.0385	-0.0060	0.0005
194	-0.215	-0.258	-0.140	-0.0289	-0.0039	0.0010
195	-0.213	-0.130	0.092	-0.0033	-0.0028	0.0024
198	-0.179	-0.127	0.124	-0.0012	-0.0023	0.0026
200	-0.040	-0.114	0.048	0.0046	-0.0007	0.0043
210	0.004	-0.110	-0.003	0.0059	-0.0003	0.0050
215	0.004	0.000	0.000	0.0070	-0.0002	0.0035
220	0.004	-0.006	0.002	0.0089	0.0000	0.0000
230	0.004	-0.007	0.002	0.0089	0.0000	0.0000
231	0.004	-0.007	0.002	0.0089	0.0000	0.0000
240	0.004	0.000	0.002	0.0091	0.0000	0.0002
241	0.004	0.000	0.002	0.0091	0.0000	0.0002
250	0.004	0.001	0.002	0.0091	0.0000	0.0002
255	0.004	0.000	0.001	0.0108	0.0000	-0.0053
260	0.005	-1.090	0.000	0.0077	0.0001	-0.0227
265	-0.002	0.000	0.000	-0.0204	-0.0003	-0.0134
268	-0.008	0.401	0.000	-0.0200	-0.0003	-0.0120
269	-0.014	0.603	0.003	-0.0184	-0.0004	-0.0111
270	-0.016	0.568	0.005	-0.0178	0.0003	-0.0099
275	-0.016	0.000	-0.024	-0.0143	0.0010	-0.0171
278	-0.016	-0.284	-0.042	-0.0133	0.0011	-0.0209

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30, 2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 16 (SUS) W+P1+H

-----Translations (mm.)-----      -----Rotations (deg.)-----

NODE	DX	DY	DZ	RX	RY	RZ
279	-0.018	-0.781	-0.046	-0.0032	-0.0014	-0.0506
280	-0.064	-1.096	-0.031	-0.0019	-0.0044	-0.0551
285	0.000	0.000	-0.036	0.0075	0.0112	-0.0716
288	0.509	-0.609	-0.038	0.0224	0.0172	-0.0752
290	1.599	-1.979	-0.039	0.0240	0.0222	-0.0809
300	1.682	-2.069	-0.039	0.0240	0.0222	-0.0809
301	1.682	-2.069	-0.039	0.0240	0.0222	-0.0809
310	1.765	-2.158	-0.039	0.0240	0.0222	-0.0809
314	2.334	-0.194	0.661	0.0186	0.0251	-0.0822
315	1.346	-0.003	0.447	0.0246	0.0260	-0.0750
330	0.891	-0.001	0.296	0.0247	0.0260	-0.0748
340	0.613	-0.001	0.204	0.0247	0.0260	-0.0748
341	0.613	-0.001	0.204	0.0247	0.0260	-0.0748
720	0.004	-0.229	-0.007	0.0088	0.0001	-0.0023
730	0.004	-0.221	-0.007	0.0088	0.0001	-0.0024
731	0.004	-0.221	-0.007	0.0088	0.0001	-0.0024
740	0.004	-0.096	-0.004	0.0091	0.0001	-0.0032
741	0.004	-0.096	-0.004	0.0091	0.0001	-0.0032
750	0.004	-0.083	-0.004	0.0091	0.0001	-0.0033
755	0.004	0.000	-0.002	0.0107	0.0001	0.0010
760	0.004	-0.861	0.000	0.0080	-0.0001	0.0178
765	0.000	0.000	0.000	-0.0163	0.0000	0.0088
768	0.001	0.308	0.000	-0.0150	0.0001	0.0075
769	0.004	0.421	0.001	-0.0085	0.0002	0.0081
770	0.004	0.365	0.002	-0.0073	-0.0001	0.0065
775	0.004	0.000	-0.011	-0.0026	-0.0005	0.0119
778	0.004	-0.206	-0.020	-0.0013	-0.0006	0.0149
779	0.002	-0.594	-0.028	0.0053	-0.0002	0.0329
780	0.009	-0.879	-0.027	0.0028	0.0010	0.0335
785	0.000	0.000	-0.029	0.0018	-0.0026	0.0327
788	-0.119	-0.328	-0.030	0.0123	-0.0038	0.0326
790	-0.323	-0.999	-0.031	0.0084	-0.0031	0.0323
800	-0.334	-1.030	-0.031	0.0083	-0.0031	0.0323
801	-0.334	-1.030	-0.031	0.0083	-0.0031	0.0323
810	-0.346	-1.061	-0.031	0.0083	-0.0031	0.0323
814	-0.220	-0.074	0.009	-0.0007	0.0029	0.0253
815	-0.012	-0.003	0.003	0.0002	-0.0010	0.0016
830	-0.006	-0.002	0.001	0.0001	-0.0005	0.0007
840	-0.003	-0.001	0.001	0.0001	-0.0004	0.0006
841	-0.003	-0.001	0.001	0.0001	-0.0004	0.0006
1000	0.030	-0.380	-0.046	-0.0156	-0.0027	0.0157
1005	0.068	-0.737	-0.045	-0.0125	-0.0011	0.0146
1006	0.031	-0.508	-0.075	-0.0149	-0.0036	0.0111
1010	0.077	-0.903	-0.044	-0.0050	-0.0002	0.0139
1020	0.077	-0.922	-0.044	-0.0048	-0.0001	0.0139
1021	0.077	-0.922	-0.044	-0.0048	-0.0001	0.0139
1030	0.080	-1.079	-0.044	-0.0026	0.0000	0.0138
1031	0.080	-1.079	-0.044	-0.0026	0.0000	0.0138
1040	0.080	-1.088	-0.044	-0.0024	0.0000	0.0138
1045	0.078	-1.064	-0.044	0.0046	0.0004	0.0133
1050	0.074	-0.997	-0.044	0.0094	0.0006	0.0129
1060	0.065	-0.842	-0.043	0.0168	0.0010	0.0122
1070	0.062	-0.792	-0.043	0.0169	0.0010	0.0122
1071	0.062	-0.792	-0.043	0.0169	0.0010	0.0122
1080	0.034	-0.335	-0.043	0.0172	0.0011	0.0120
1081	0.034	-0.335	-0.043	0.0172	0.0011	0.0120
1090	0.031	-0.282	-0.043	0.0171	0.0011	0.0120
1100	0.018	-0.096	-0.043	0.0100	0.0012	0.0113
1105	0.005	0.000	-0.042	0.0022	0.0012	0.0108

## Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30, 2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 16 (SUS) W+Pl+H

-----Translations (mm.)----- Rotations (deg.)-----

NODE	DX	DY	DZ	RX	RY	RZ
1110	-0.004	-0.037	-0.043	-0.0046	0.0012	0.0104
1120	-0.009	-0.055	-0.043	-0.0047	0.0012	0.0104
1121	-0.009	-0.055	-0.043	-0.0047	0.0012	0.0104
1130	-0.060	-0.278	-0.043	-0.0053	0.0012	0.0103
1131	-0.060	-0.278	-0.043	-0.0053	0.0012	0.0103
1140	-0.065	-0.298	-0.043	-0.0053	0.0012	0.0102
1148	-0.075	-0.343	-0.043	-0.0050	0.0012	0.0098
1149	-0.047	-0.365	-0.042	0.0014	0.0029	0.0080
1150	0.003	-0.351	-0.075	0.0016	0.0048	0.0019
1158	0.037	-0.348	-0.108	0.0008	0.0047	0.0011
1159	0.028	-0.308	-0.046	-0.0095	0.0025	-0.0051
1160	0.004	-0.156	0.018	-0.0067	-0.0001	-0.0072
1165	-0.001	0.000	0.016	0.0029	-0.0001	-0.0088
1167	0.000	-1.113	0.016	-0.0014	0.0004	-0.0142
1168	0.031	-0.671	0.015	-0.0125	0.0006	-0.0166
1169	0.035	-0.307	0.016	-0.0192	0.0000	-0.0182
1170	0.034	-0.019	0.011	-0.0137	-0.0004	-0.0024
1175	0.034	0.000	0.000	-0.0112	-0.0003	0.0047
1180	0.037	-0.485	-0.026	-0.0064	-0.0015	0.0029
1188	0.042	-0.346	-0.067	-0.0052	-0.0014	-0.0075
1189	-0.051	-0.122	-0.052	-0.0044	-0.0008	-0.0141
1190	-0.127	-0.062	-0.019	-0.0010	-0.0014	0.0019
1200	-0.071	-0.054	-0.005	-0.0006	-0.0008	0.0015
1250	-0.073	0.000	-0.007	0.0032	-0.0006	0.0002
1300	0.032	-0.597	-0.117	-0.0140	-0.0046	0.0050
1310	0.032	-0.616	-0.134	-0.0140	-0.0046	0.0049
1311	0.032	-0.616	-0.134	-0.0140	-0.0046	0.0049
1320	0.032	-0.779	-0.329	-0.0137	-0.0047	0.0031
1321	0.032	-0.779	-0.329	-0.0137	-0.0047	0.0031
1330	0.032	-0.790	-0.347	-0.0137	-0.0047	0.0030
1338	0.033	-0.783	-0.389	-0.0129	-0.0046	0.0002
1339	-0.062	-0.582	-0.376	-0.0114	-0.0037	-0.0161
1340	-0.159	-0.509	-0.275	-0.0062	-0.0042	0.0035
1350	-0.033	-0.044	-0.002	0.0008	-0.0012	0.0008
1400	-0.016	-0.028	-0.002	0.0009	-0.0009	0.0004
1410	-0.006	-0.013	-0.001	0.0006	-0.0005	0.0002
1415	0.000	0.000	0.000	0.0000	0.0000	0.0000
1420	0.000	0.000	0.000	0.0000	0.0000	0.0000
1498	-0.082	-0.075	-0.008	0.0059	-0.0010	-0.0003
1499	-0.141	-0.409	0.141	0.0195	-0.0048	-0.0006
1500	-0.114	-0.507	0.274	-0.0046	-0.0036	-0.0076
1508	0.272	-0.522	-0.004	-0.0058	-0.0052	-0.0097
1509	0.505	-0.549	0.002	0.0074	-0.0026	-0.0201
1510	0.617	-0.723	0.070	0.0078	-0.0032	-0.0222
1515	0.007	0.000	0.056	-0.0129	-0.0037	-0.0339
1518	-0.011	0.056	0.056	-0.0124	-0.0036	-0.0343
1519	-0.042	-0.090	0.063	-0.0066	-0.0001	-0.0360
1520	-0.037	-0.562	0.048	-0.0125	0.0013	-0.0230
1525	-0.037	-1.381	0.000	-0.0167	0.0009	-0.0175
1528	-0.037	-2.106	-0.021	-0.0236	0.0001	-0.0068
1529	-0.038	-1.841	-0.019	-0.0312	0.0000	0.0108
1530	-0.032	-1.198	-0.021	-0.0285	0.0007	0.0111
1535	0.004	0.000	-0.020	-0.0159	0.0008	0.0091
1538	0.024	0.224	-0.021	-0.0076	0.0007	0.0080
1539	-0.015	0.084	0.061	0.0136	0.0014	0.0065
1540	-0.065	-0.002	0.210	0.0014	0.0029	0.0008
1548	0.110	0.001	-0.110	-0.0041	0.0000	-0.0041
1549	0.331	0.168	-0.331	-0.0198	0.0000	-0.0198
1550	-0.059	-0.015	0.160	-0.0018	0.0016	-0.0006

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

DISPLACEMENT REPORT, Nodal Movements

CASE 16 (SUS) W+Pi+H

NODE	-----Translations (mm.)-----			-----Rotations (deg.)-----		
	DX	DY	DZ	RX	RY	RZ
1555	0.000	-0.007	0.000	0.0000	0.0000	0.0000
1558	0.470	0.855	-0.470	-0.0029	0.0000	-0.0029
1559	0.503	0.781	-0.503	0.0065	0.0000	0.0065
1560	0.000	-0.063	0.000	0.0000	0.0000	0.0000
1565	0.000	-0.090	0.000	0.0000	0.0000	0.0000
1570	-0.001	-0.089	0.001	0.0000	0.0000	0.0000
1575	-0.001	-0.059	0.001	0.0000	0.0000	0.0000
1590	0.335	-0.001	0.112	0.0247	0.0260	-0.0748
1600	0.000	0.000	0.000	0.0248	0.0260	-0.0748
1610	0.000	0.000	0.000	0.0248	0.0260	-0.0748
1650	-0.001	-0.001	0.001	0.0001	-0.0004	0.0006
1660	0.000	0.000	0.000	0.0000	0.0000	0.0000
1670	0.000	0.000	0.000	0.0000	0.0000	0.0000
1700	0.000	-0.012	0.000	0.0000	0.0000	0.0000
1710	0.001	-0.083	-0.001	0.0000	0.0000	0.0000
1715	0.001	-0.126	-0.001	0.0000	0.0000	0.0000
1720	0.000	-0.140	0.000	0.0000	0.0000	0.0000
1725	0.000	-0.126	0.000	0.0000	0.0000	0.0000
1730	-0.001	-0.083	0.001	0.0000	0.0000	0.0000
1740	0.000	-0.012	0.000	0.0000	0.0000	0.0000
2000	0.000	0.000	0.000	0.0000	0.0000	0.0000
2500	0.470	0.601	-0.470	-0.0078	0.0000	-0.0078
2505	0.470	0.694	-0.470	-0.0066	0.0000	-0.0066
2510	0.630	0.706	-0.630	0.0076	0.0000	0.0076
2520	0.647	0.706	-0.647	0.0076	0.0000	0.0076
2530	0.675	0.706	-0.675	0.0076	0.0000	0.0076
3500	0.675	0.706	-0.675	0.0076	0.0000	0.0076
3510	0.703	0.706	-0.703	0.0076	0.0000	0.0076
3520	0.000	-0.010	0.000	0.0000	0.0000	0.0000
3530	0.000	-0.010	0.000	0.0000	0.0000	0.0000
3540	0.000	-0.010	0.000	0.0000	0.0000	0.0000
3550	0.000	-0.010	0.000	0.0000	0.0000	0.0000
3560	0.000	-0.011	0.000	0.0000	0.0000	0.0000
3800	0.000	-0.009	0.000	0.0000	0.0000	0.0000
3810	0.000	-0.008	0.000	0.0000	0.0000	0.0000
3820	0.000	-0.011	0.000	0.0000	0.0000	0.0000
3900	0.000	-0.007	0.000	0.0000	0.0000	0.0000
3950	0.000	-0.005	0.000	0.0000	0.0000	0.0000
3960	0.000	-0.006	0.000	0.0000	0.0000	0.0000
4500	0.000	-0.002	0.000	0.0000	0.0000	0.0000
4510	0.000	-0.002	0.000	0.0000	0.0000	0.0000
5000	0.000	0.000	0.000	0.0000	0.0000	0.0000

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50 APR 30, 2008 18:52:38  
 Job name: Compressor Station Piping Stress Analysis - Discharge Line

## RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

### RESTRAINT SUMMARY

NODE	CASE	TYPE	---Forces(N. )			-----Moments(N.m. )			-----Displacements(mm.)--		
			FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
10			Rigid ANC								
	3	HYD	460.	-32196.	-3436.	13586.	-14997.	-640.	0.0000	0.0000	0.0000
	4	OPE	2184	-4629.	-13631.	-17613.	-44928.	-7314.	0.0000	0.0000	0.0000
	16	SUS	59.	673.	-2945.	12770.	-13379.	-8197.	0.0000	0.0000	0.0000
MAX.	4		2184.	32196/3	13631	17613.	44928.	8197/160.000/160.000/3			0.0000
30			Prog Design VSH								
	3	HYD	0.	6233.	0.	0.	0.	0.	-0.0009	0.0000	0.5887
	4	OPE	0.	-20772.	0.	0.	0.	0.	-0.3950	1.4189-	0.4900
	16	SUS	0.	-21112.	0.	0.	0.	0.	0.2527	0.2043	0.5398
MAX.	3		0.	21112/160.	0.	0.	0.	0.	0.395/4	1.419/4	0.589
50			Rigid ANC								
	3	HYD	-460.	-21707.	3436.	-27375.	6101.	-18442.	-0.0008	0.0516	0.4174
	4	OPE	-2184.	-8872.	13631.	-37087.	9638.	-23873.	-0.9438	0.8567	-1.9494
	16	SUS	-59.	-13835.	2945.	-24587.	5756.	-27699.	0.2527	0.1864	0.3882
MAX.	4		2184.	21707.	13631.	37087.	9638.	27699/16	0.944	0.857	1.9494
65			Rigid +Y								
	3	HYD	0.	-132053.	0.	0.	0.	0.	-0.0007	0.0000	0.1678
	4	OPE	0.	-103545.	0.	0.	0.	0.	-1.6455	0.0000	-3.8564
	16	SUS	0.	-108924.	0.	0.	0.	0.	0.2527	0.0000	0.1652
MAX.	3		0.	132053.	0.	0.	0.	0.	1.645/40.0000		3.856/4
90			Rigid ANC								
	3	HYD	-460.	74982.	3436.	120143.	-3376.	26807.	-0.0704	-2.3458	0.0465
	4	OPE	-2184.	68618.	13631.	95784.	-27334.	37208.	-2.1128	-2.1690	-3.8767
	16	SUS	-59.	69034.	2945.	109011.	-2951.	24681.	0.1517	-2.1810	0.0434
MAX.	4		2184	74982/3	13631	120143/327334.	37208.	2.113	2.346/3		3.8767
100			Rigid ANC								
	3	HYD	-460.	66982.	3436.	126603.	-3334.	26807.	-0.0697	-2.3566	0.0465
	4	OPE	-2184.	60817.	13631.	101673.	-27135.	37208.	-2.0798	-2.1756	-3.8421
	16	SUS	-59.	61233.	2945.	114938.	-2946.	24681.	0.1497	-2.1906	0.0434
MAX.	4		2184.	66982/3	13631.	126603/327135	37208.	2.080	2.357/3		3.8421
110			Rigid ANC								
	3	HYD	-460.	5449.	3436.	213521.	-2229.	26807.	-0.0520	-2.5592	0.0464
	4	OPE	-2184.	4545.	13631.	180109.	-21893.	37208.	-1.1986	-2.2818	-2.9310
	16	SUS	-59.	4961.	2945.	194373.	-2803.	24681.	0.0996	-2.3693	0.0433
MAX.	4		2184.	5449/3	13631.	213521/3	21893	37208.	1.1986	2.559/3	2.9310
140			Rigid ANC								
	3	HYD	-460.	-10103.	3436.	210627.	-1656.	26807.	-0.0395	-2.3520	0.0459
	4	OPE	-2184.	-8280.	13631.	177785.	-19176.	37208.	-0.7095	-2.0736	-2.4604
	16	SUS	-59.	-7864.	2945.	192567.	-2730.	24681.	0.0778	-2.1780	0.0429
MAX.	4		2184.	10103/3	13631	210627/3	19176	37208	0.710	2.352/3	2.4604
150			Rigid ANC								
	3	HYD	-460.	-71636.	3436.	112540.	-551.	26807.	-0.0108	-1.3593	0.0458
	4	OPE	-2184.	-64552.	13631.	90386.	-13933.	37208.	0.2871	-1.1717	-1.5492
	16	SUS	-59.	-64136.	2945.	106166.	-2587.	24681.	0.0432	-1.2671	0.0428
MAX.	4		2184.	71636/3	13631.	112540/3	13933.	37208.	0.287	1.359/3	1.5492
165			Rigid +								
	3	HYD	3185.	-114465.	7809.	0.	0.	0.	0.0182	0.0000	0.0446
	4	OPE	29625	-111815.	-15734	0.	0.	0.	1.3008	0.0000	-0.6909
	16	SUS	4277.	-95172.	7318.	0.	0.	0.	0.0244	0.0000	0.0418

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30, 2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

RESTRAINT SUMMARY

			---Forces(N. )-----				---Moments(N.m. )-----			---Displacements(mm.)---		
NODE	CASE	TYPE	FX	FY	FZ	MX	MY	MZ	DX	DY	DZ	
MAX.	3		29625/4	114465	15734/4	0.	0.	0.	1.301/4	0.0000	0.691/4	
			Rigid +Y									
	3	HYD	6311.	-135652.	-1360.	0.	0.	0.	0.0360	0.0000	-0.0078	
	4	OPE	21390	-80095.	10946.	0.	0.	0.	1.4633	0.0000	0.7488	
	16	SUS	4868.	-104536.	-950.	0.	0.	0.	0.0278	0.0000	-0.0054	
MAX.	4		21390	135652/3	10946	0./3	0./3	0./3	1.4633	0.000/3	0.7488	
			Rigid Z									
	3	HYD	0.	0.	-4302.	0.	0.	0.	-0.0040	0.1556	0.0000	
	4	OPE	0.	0.	38854.	0.	0.	0.	1.7562	0.5113	0.0000	
	16	SUS	0.	0.	-4083.	0.	0.	0.	-0.0201	0.4386	0.0000	
MAX.	4		0./3	0./3	38854	0./3	0./3	0./3	1.7562	0.5113	0.0000	
			Rigid +Y			Rigid Z						
	3	HYD	641.	-124861.	649.	0.	0.	0.	0.0037	0.0000	0.0000	
	4	OPE	2567.	-102425.	-20623.	0.	0.	0.	0.0147	0.0000	0.0000	
	16	SUS	755.	-101328.	568.	0.	0.	0.	0.0043	0.0000	0.0000	
MAX.	4		2567.	124861/3	20623.	0./3	0./3	0./3	0.015	0.0000	0.0000	
			Rigid ANC									
	3	HYD	507.	21559.	169	-12201.	-596.	3672.	0.0036	0.0119	0.0014	
	4	OPE	20021	23822.	9964.	-15929.	-77187.	-306.	0.5696	-0.0004	-0.4130	
	16	SUS	640.	23267.	230.	-8410.	-842.	-3661.	0.0042	-0.0066	0.0019	
MAX.	4		20021.	23822.	9964.	15929.	77187.	3672./3	0.570	0.012/3	0.4130	
			Rigid ANC									
	3	HYD	507.	-39973.	169.	-12201.	-191.	25769.	0.0035	0.0243	0.0015	
	4	OPE	20021	-32450.	9964.	-15929.	-53275.	10047.	1.4805	0.0044	-1.3587	
	16	SUS	640.	-33004.	230.	-8410.	-290.	8023.	0.0042	-0.0001	0.0019	
MAX.	4		20021.	39973/3	9964.	15929.	53275.	25769/3	1.4805	0.024/3	1.3587	
			Rigid +Y									
	3	HYD	603.	-97413.	209.	0.	0.	0.	0.0034	0.0000	0.0012	
	4	OPE	15616.	-73483.	-15560.	0.	0.	0.	1.9755	0.0000	-1.9684	
	16	SUS	707.	-72722.	251.	0.	0.	0.	0.0040	0.0000	0.0014	
MAX.	3		15616/4	97413.	15560/40.	0.	0.	0.	1.976/4	0.0000	1.968/4	
			Rigid +Y			Rigid Z						
	3	HYD	-486.	-35629.	792.	0.	0.	0.	-0.0028	0.0000	0.0000	
	4	OPE	-5814.	-19380.	18247.	0.	0.	0.	-0.6122	0.0000	0.0000	
	16	SUS	-344.	-23481.	592.	0.	0.	0.	-0.0020	0.0000	0.0000	
MAX.	4		5814.	35629/3	18247.	0./3	0./3	0./3	0.6122	0.000/3	0.0000	
			Rigid +Y									
	3	HYD	-3798.	-64578.	-5775.	0.	0.	0.	-0.0217	0.0000	-0.0330	
	4	OPE	2283.	-48627.	-14408.	0.	0.	0.	0.4399	0.0000	-2.7760	
	16	SUS	-2787.	-42851.	-4236.	0.	0.	0.	-0.0159	0.0000	-0.0242	
MAX.	3		3798.	64578.	14408/40.	0.	0.	0.	0.440/4	0.0000	2.78/4	
			Rigid +Y			Rigid X						
	3	HYD	9843.	-88456.	0.	0.	0.	0.	0.0000	0.0000	-0.0494	
	4	OPE	18361.	-50050.	0.	0.	0.	0.	0.0000	0.0000	-0.7043	
	16	SUS	7201.	-60806.	0.	0.	0.	0.	0.0000	0.0000	-0.0364	
MAX.	4		18361.	88456/3	0./3	0./3	0./3	0./3	0.0000	0.000/3	0.7043	
			Rigid ANC									
	3	HYD	-5655.	5647.	4942.	21933.	-6629.	13157.	2.3003	-2.8036	-0.0535	

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

## RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

### RESTRAINT SUMMARY

		---Forces(N. )-----			-----Moments(N.m. )-----			-----Displacements(mm.)---		
NODE	CASE TYPE	FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
	4 OPE-10634.	-3926.		20464.	4793.	12117.	13496.	1.1324	-0.2878	1.2856
	16 SUS-4138.	3840.		3623.	17377.	-4836.	10532.	1.6821	-2.0685	-0.0394
MAX.	4	10634.	5647/3	20464.	21933/3	12117.	13496.	2.300/3	2.804/3	1.2856
340										
	3 HYD-5655.	-35049.		4942.	-2323.	0.	-2658.	0.8382	-0.0018	0.2785
	4 OPE-10634.	-33543.		20464.	-9618.	0.	-4998.	-1.0595	2.0292	0.7498
	16 SUS-4138.	-25776.		3623.	-1703.	0.	-1945.	0.6127	-0.0014	0.2038
MAX.	4	10634.	35049/3	20464.	9618.	0./ 3	4998.	1.0595	2.0292	0.7498
730										
	3 HYD 635.	7047.	-235.	-11955.	-798.	0.	52869.	0.0036	-0.2543	-0.0051
	4 OPE-23911.	10348.	7776.	-15653.	62810.	52413.	-1.1411	-0.2419	-0.5215	
	16 SUS 739.	11549.	-318.	-8247.	-1066.	49039.	0.0042	-0.2206	-0.0070	
MAX.	4	23911.	11549/167776.	15653.	62810.	52869/3	1.1411	0.254/3	0.5215	
740										
	3 HYD 635.	-54486.	-235.	-11955.	-234.	-4058.	0.0036	-0.0957	-0.0030	
	4 OPE-23911.	-45924.	7776.	-15653.	44148.	9721.	-2.0518	-0.1045	-1.4829	
	16 SUS 739.	-44722.	-318.	-8247.	-303.	9231.	0.0042	-0.0963	-0.0041	
MAX.	4	23911.	54486/3	15653.	44148.	9721.	2.0518	0.1045	1.4829	
755										
	3 HYD 605.	-110895.	-248.	0.	0.	0.	0.0035	0.0000	-0.0014	
	4 OPE-19975.	-86062.	-16358.	0.	0.	0.	-2.5462	0.0000	-2.0852	
	16 SUS 715.	-83689.	-347.	0.	0.	0.	0.0041	0.0000	-0.0020	
MAX.	4	19975.	110895/316358.	0./ 3	0./ 3	0./ 3	2.5462	0.000/3	2.0852	
765										
	3 HYD 79.	-39189.	551.	0.	0.	0.	0.0005	0.0000	0.0000	
	4 OPE 6830.	-22766.	11973.	0.	0.	0.	0.4329	0.0000	0.0000	
	16 SUS 65.	-26095.	432.	0.	0.	0.	0.0004	0.0000	0.0000	
MAX.	4	6830.	39189/3	11973.	0./ 3	0./ 3	0.4329	0.000/3	0.0000	
775										
	3 HYD 1024.	-64702.	-2609.	0.	0.	0.	0.0058	0.0000	-0.0149	
	4 OPE-2612.	-47607.	-14041.	0.	0.	0.	-0.8576	0.0000	-4.6097	
	16 SUS 747.	-42923.	-1945.	0.	0.	0.	0.0043	0.0000	-0.0111	
MAX.	4	2612.	64702/3	14041.	0./ 3	0./ 3	0.8576	0.000/3	4.6097	
785										
	3 HYD-4232.	-84238.	0.	0.	0.	0.	0.0000	0.0000	-0.0391	
	4 OPE-23280.	-50300.	0.	0.	0.	0.	0.0000	0.0000	-3.3065	
	16 SUS-3105.	-57726.	0.	0.	0.	0.	0.0000	0.0000	-0.0294	
MAX.	4	23280.	84238/3	0./ 3	0./ 3	0./ 3	0.0000	0.000/3	3.3065	
800										
	3 HYD 3159.	4082.	2071.	37479.	-7745.	1940.	-0.4564	-1.3838	-0.0409	
	4 OPE 13622.	-2205.	24101.	26795.	-19970.	-1068.	-1.0035	0.5336	-1.3196	
	16 SUS 2317.	2695.	1542.	28737.	-5685.	490.	-0.3342	-1.0301	-0.0307	
MAX.	4	13622.	4082/3	24101.	37479/3	19970.	1.0035	1.384/3	1.3196	
840										
	3 HYD 3159.	-36614.	2071.	3483.	-12968.	25454.	-0.0044	-0.0019	0.0014	
	4 OPE 13622.	-31821.	24101.	23914.	-9098.	8543.	-0.1476	2.0292	0.0124	
	16 SUS 2317.	-26921.	1542.	2565.	-9465.	18591.	-0.0032	-0.0014	0.0010	
MAX.	4	13622.	36614/3	24101.	23914.	12968/3	25454/3	0.1476	2.0292	0.0124



# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50 APR 30,2008 18:52:38  
 Job name: Compressor Station Piping Stress Analysis - Discharge Line

## RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

### RESTRAINT SUMMARY

		---Forces(N. )-----			-----Moments(N.m. )-----			-----Displacements(mm.)--		
NODE	CASE TYPE	FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
1020										
			Rigid ANC							
	3	HYD 1693.	38806.	-4195.	-98426.	-9581.	5047.	0.0919	-1.0013	-0.0557
	4	OPE 22.	41975.	-32258.	-81962.	-308.	4994.	0.8953	-0.7532	0.0575
	16	SUS 1070.	34971.	-3766.	-90296.	-7793.	4906.	0.0773	-0.9217	-0.0444
MAX.	4	1693/3	41975.	32258.	98426/39581/3	5047/3		0.8953	1.001/3	0.0557
1030										
			Rigid ANC							
	3	HYD 1693.	-22727.	-4195.	-117721.	-5519.	5047.	0.0893	-1.1782	-0.0555
	4	OPE 22.	-14296.	-32258.	-115177.	-254.	4994.	0.6790	-1.0833	-0.8530
	16	SUS 1070.	-21301.	-3766.	-106701.	-5226.	4906.	0.0801	-1.0792	-0.0442
MAX.	3	1693.	22727.	32258/4	117721 5519.	5047.		0.679/4	1.1782	0.853/4
1070										
			Rigid ANC							
	3	HYD 1693.	-40699.	-4195.	-52418.	-2143.	5047.	0.0661	-0.8621	-0.0544
	4	OPE 22.	-28293.	-32258.	-70942.	-210.	4994.	0.4982	-0.8906	-1.6015
	16	SUS 1070.	-35297.	-3766.	-48497.	-3092.	4906.	0.0615	-0.7915	-0.0432
MAX.	4	1693/3	40699/3	32258	70942.	3092/165	5047/3	0.4982	0.8921/3	1.6015
1080										
			Rigid ANC							
	3	HYD 1693.	-76252.	-4195.	35295.	397.	5047.	0.0378	-0.3606	-0.0542
	4	OPE 22.	-61777.	-32258.	-3390.	-177.	4994.	0.3614	-0.4247	-2.1704
	16	SUS 1070.	-68781.	-3766.	29563.	-1487.	4906.	0.0338	-0.3346	-0.0431
MAX.	4	1693/3	76252/3	32258.	35295/31487/165	5047/3		0.3614	0.4247	2.1704
1105										
			Rigid +Y							
	3	HYD 2404.	-165403.	-9349.	0.	0.	0.	0.0137	0.0000	-0.0534
	4	OPE 3497.	-130467.	-38983.	0.	0.	0.	0.2395	0.0000	-2.6695
	16	SUS 957.	-146315.	-7408.	0.	0.	0.	0.0055	0.0000	-0.0423
MAX.	4	3497.	165403/3	38983.	0./ 3	0./ 3	0./ 3	0.2395	0.0000	2.6695
1120										
			Rigid ANC							
	3	HYD-711.	71179.	5153.	93584.	2179.	5047.	0.0061	-0.0720	-0.0538
	4	OPE 189.	54693.	6619.	45516.	-22.	4994.	0.1785	0.0593	-2.9218
	16	SUS 113.	63537.	3643.	81931.	12.	4906.	-0.0088	-0.0554	-0.0426
MAX.	3	711.	71179.	6619/4	93584.	2179	5047.	0.1785/4	0.07202.	9218/4
1130										
			Rigid ANC							
	3	HYD-711.	9647.	5153.	-3408.	473.	5047.	-0.0193	-0.3595	-0.0540
	4	OPE 189.	-1579.	6619.	-18221.	430.	4994.	-0.0421	0.2900	-3.8337
	16	SUS 113.	7265.	3643.	-3032.	283.	4906.	-0.0602	-0.2779	-0.0427
MAX.	3	711.	9647.	6619/4	18221/4473.	5047.		0.060/16	0.3595	3.8337
1165										
			Rigid +Y							
	3	HYD-1215.	-88563.	4118.	0.	0.	0.	-0.0069	0.0000	0.0235
	4	OPE-5281.	-69720.	-20238.	0.	0.	0.	-1.0615	0.0000	-4.0677
	16	SUS-88.	-59618.	2874.	0.	0.	0.	-0.0005	0.0000	0.0164
MAX.	4	5281.	88563/3	20238.	0./ 3	0./ 3	0./ 3	1.0615	0.0000/3	4.0677
1167										
			Rigid X							
	3	HYD 1299.	0.	0.	0.	0.	0.	0.0000	-1.7898	0.0223
	4	OPE 20863.	0.	0.	0.	0.	0.	0.0000	-1.2395	-1.4394
	16	SUS 707.	0.	0.	0.	0.	0.	0.0000	-1.1126	0.0155
MAX.	4	20863.	0./ 3	0./ 3	0./ 3	0./ 3	0./ 3	0.0000	1.790/3	1.4394
1175										
			Rigid Z Rigid +Y							
	3	HYD 8714.	-106169.	4274.	0.	0.	0.	0.0498	0.0000	0.0000
	4	OPE 15782.	-52605.	45536.	0.	0.	0.	0.6343	0.0000	0.0000
	16	SUS 5949.	-75163.	3531.	0.	0.	0.	0.0340	0.0000	0.0000

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50 APR 30, 2008 18:52:38  
 Job name: Compressor Station Piping Stress Analysis - Discharge Line

## RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

### RESTRAINT SUMMARY

			---Forces(N. )-----			-----Moments(N.m. )-----			-----Displacements(mm.)--		
NODE	CASE	TYPE	FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
MAX.	4		15782.	106169/345536.	0./ 3	0./ 3	0./ 3	0.6343	0.0000	0.0000	
			Rigid +Y								
1250	3	HYD-16645.	-187028.	-1898.	0.	0.	0.		-0.0950	0.0000	-0.0108
	4	OPE-35312.	-145834.	25830.	0.	0.	0.		-0.4420	0.0000	0.3233
	16	SUS-12793.	-126193.	-1208.	0.	0.	0.		-0.0731	0.0000	-0.0069
MAX.	4		35312.	187028/325830.	0./ 3	0./ 3	0./ 3	0.4420	0.000/3	0.3233	
			Rigid ANC								
1310	3	HYD-13432.	18943.	4901.	-9173.	13505.	95456.		0.0403	-0.6711	-0.1671
	4	OPE-49691.	2633.	13779.	-25688.	40591.	115451.		0.6239	0.1385	0.9124
	16	SUS-12408.	16108.	3945.	-8931.	10271.	90412.		0.0318	-0.6162	-0.1340
MAX.	4		49691.	18943/3	13779.	25688.	40591.	115451.	0.6239	0.671/3	0.9124
			Rigid ANC								
1320	3	HYD-13432.	-42590.	4901.	-9173.	1741.	67079.		0.0408	-0.8674	-0.4125
	4	OPE-49691.	-53639.	13779.	-25688.	7521.	54244.		-0.2860	0.9609	0.8036
	16	SUS-12408.	-40164.	3945.	-8931.	803.	61545.		0.0323	-0.7790	-0.3292
MAX.	4		49691.	53639.	13779.	25688.	7521.	67079/3	0.2860	0.9601	0.8036
			Rigid ANC								
1420	3	HYD-7760.	-33466.	-15101.	33467.	-21178.	3864.		0.0000	0.0000	0.0000
	4	OPE-45203.	-43422.	-45728.	61700.	-111985.	79031.		0.0000	0.0000	0.0000
	16	SUS-7000.	-26835.	-9575.	30128.	-18207.	4751.		0.0000	0.0000	0.0000
MAX.	4		45203.	43422.	45728.	61700.	111985.	79031.	0.0000	0.0000	0.0000
			Rigid +Y								
1515	3	HYD 1870.	-95204.	15144.	0.	0.	0.		0.0107	0.0000	0.0865
	4	OPE-3060.	-60739.	15415.	0.	0.	0.		-0.0175	0.0000	0.0880
	16	SUS 1172.	-61426.	9768.	0.	0.	0.		0.0067	0.0000	0.0558
MAX.	4		3060.	95204/3	15415.	0./ 3	0./ 3	0./ 3	0.0175	0.000/3	0.0880
			Rigid Z								
1525	3	HYD 0.	0.	5377.	0.	0.	0.		-0.0629	-2.1422	0.0000
	4	OPE 0.	0.	-2843.	0.	0.	0.		0.2553	-1.7435	0.0000
	16	SUS 0.	0.	3362.	0.	0.	0.		-0.0372	-1.3805	0.0000
MAX.	3		0.	5377.	0.	0.	0.		0.255/4	2.1422	0.0000
			Rigid +Y								
1535	3	HYD 1105.	-154744.	-5539.	0.	0.	0.		0.0063	0.0000	-0.0316
	4	OPE 4775.	-91826.	1206.	0.	0.	0.		0.0273	0.0000	0.0069
	16	SUS 737.	-99769.	-3535.	0.	0.	0.		0.0042	0.0000	-0.0202
MAX.	3		4775/4	154744.	5539.	0.	0.	0.	0.0273	0.0000	0.0316
			Rigid Z Rigid X								
1555	3	HYD-20684.	0.	22568.	0.	0.	0.		0.0000	-0.0109	0.0000
	4	OPE 802370.	0.	-802464.	0.	0.	0.		0.0000	1.5225	0.0000
	16	SUS-13567.	0.	14777.	0.	0.	0.		0.0000	-0.0069	0.0000
MAX.	4		802370.0./ 3	802464.0./ 3	0./ 3	0./ 3	0./ 3		0.0000	1.5225	0.0000
			Rigid ANC								
1600	3	HYD-5655.	-41823.	4942.	0.	0.	0.		0.0000	0.0000	0.0000
	4	OPE-10634.	-39286.	20464.	0.	0.	0.		-1.5000	2.0000	0.0000
	16	SUS-4138.	-31519.	3623.	0.	0.	0.		0.0000	0.0000	0.0000
MAX.	4		10634.41823/3	20464.	0.	0./16	0./ 3		1.5000	2.0000	0.0000
			Displ. Reaction								
1610	3	HYD-5655.	-41823.	4942.	0.	0.	0.		0.0000	0.0000	0.0000
	4	OPE-10634.	-39286.	20464.	0.	0.	0.		-1.5000	2.0000	0.0000

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50 APR 30,2008 18:52:38  
 Job name: Compressor Station Piping Stress Analysis - Discharge Line

## RESTRAINT-DISPLACEMENT REPORT, Loads on Restraints

### RESTRAINT SUMMARY

		---Forces(N. )			-----Moments(N.m. )			-----Displacements(mm.)--			
NODE	CASE	TYPE	FX	FY	FZ	MX	MY	MZ	DX	DY	DZ
	16	SUS	-4138.	-31519.	3623.	0.	0.	0.	0.0000	0.0000	0.0000
MAX.	4		10634.	41823/3	20464	0./ 3	0./ 3	0./ 3	1.5000	2.0000	0.0000
	1660										
	3	HYD	3159.	-43387.	2071.	4457.	-12968.	23969.	0.0000	0.0000	0.0000
	4	OPE	13622.	-37564.	24101.	35242.	-9098.	2140.	-0.1500	2.0000	0.0000
	16	SUS	2317.	-32664.	1542.	3289.	-9465.	17502.	0.0000	0.0000	0.0000
MAX.	4		13622.	43387/3	24101.	35242.	12968/3	23969/3	0.1500	2.0000	0.0000
	1670										
	3	HYD	3159.	-43387.	2071.	4457.	-12968.	23969.	0.0000	0.0000	0.0000
	4	OPE	13622.	-37564.	24101.	35242.	-9098.	2140.	-0.1500	2.0000	0.0000
	16	SUS	2317.	-32664.	1542.	3289.	-9465.	17502.	0.0000	0.0000	0.0000
MAX.	4		13622.	43387/3	24101.	35242.	12968/3	23969/3	0.1500	2.0000	0.0000
	1700										
	3	HYD	1381.	0.	-1501.	0.	0.	0.	0.0000	-0.0188	0.0000
	4	OPE	-271540	0.	271568.	0.	0.	0.	0.0000	3.3937	0.0000
	16	SUS	1905.	0.	-1982.	0.	0.	0.	0.0000	-0.0119	0.0000
MAX.	4		271540.	0./ 3	271568.	0./ 3	0./ 3	0./ 3	0.0000	3.3937	0.0000
	1740										
	3	HYD	28464.	0.	-28459.	0.	0.	0.	0.0000	-0.0193	0.0000
	4	OPE	41182.	0.	-41184.	0.	0.	0.	0.0000	5.7671	0.0000
	16	SUS	17539.	0.	-17536.	0.	0.	0.	0.0000	-0.0118	0.0000
MAX.	4		41182.	0./ 3	41184.	0./ 3	0./ 3	0./ 3	0.0000	5.7671	0.0000
	2000										
	3	HYD	460.	-32196.	-3436.	13586.	-14997.	-640.	0.0000	0.0000	0.0000
	4	OPE	2184.	-4629.	-13631.	-17613.	-44928.	-7314.	0.0000	0.0000	0.0000
	16	SUS	59.	673.	-2945.	12770.	-13379.	-8197.	0.0000	0.0000	0.0000
MAX.	4		2184.	32196/3	13631.	17613.	44928.	8197/16	0.0/16	0.00/3	0.0000
	2505										
	3	HYD	0.	-110973.	0.	0.	0.	0.	0.2543	0.0000	-0.2543
	4	OPE	0.	-75407.	0.	0.	0.	0.	0.0910	6.0704	-0.0910
	16	SUS	0.	-82939.	0.	0.	0.	0.	0.4703	0.6942	-0.4703
MAX.	16		0./ 3	110973/30.	0./ 3	0./ 3	0./ 3	0./ 3	0.4703	6.07/4	0.4703
	2530										
	3	HYD	0.	3648.	0.	0.	0.	0.	1.3400	-2.0334	-1.3400
	4	OPE	0.	2978.	0.	0.	0.	0.	0.7086	4.5415	-0.7086
	16	SUS	0.	2978.	0.	0.	0.	0.	0.6750	0.7061	-0.6750
MAX.	16		0./ 3	3648./ 30.	0./ 3	0./ 3	0./ 3	0./ 3	1.34/3	4.542/4	1.34/3
	3530										
	3	HYD	0.	-2832.	0.	0.	0.	0.	0.0006	-0.0156	-0.0006
	4	OPE	0.	-1827.	0.	0.	0.	0.	-0.1745	5.9125	0.1744
	16	SUS	0.	-1827.	0.	0.	0.	0.	0.0004	-0.0097	-0.0003
MAX.	16		0./ 3	2832./3	0./3	0./3	0./4	0./3	0.174/4	5.912/4	0.174/4
	5000										
	3	HYD	-10672.	-612890.	11071.	63167.	2923.	59286.	0.0000	0.0000	0.0000
	4	OPE	-573423	-400018.	573312.	9547096	-915.	95481950.	0.0000	0.0000	0.0000
	16	SUS	-6857.	-385308.	7113.	40603.	1875.	38114.	0.0000	0.0000	0.0000
MAX.	4		573423.	612890/3	573312	9547096	2923/3	95481950.	0.00/3	0.0000	0.0000

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

## STRESS SUMMARY

PIPING CODE: B31.3 -2002, April 30, 2002

CASE 3 (HYD) WW+HP+H

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	51.5	@NODE	1180	STRESS:	94445.7	ALLOWABLE:	183396.
BENDING STRESS:				52450.7	@NODE	1180	
TORSIONAL STRESS:				2572.0	@NODE	29	
AXIAL STRESS:				60399.7	@NODE	1410	
HOOP STRESS:				122999.7	@NODE	1410	
3D MAX INTENSITY:				127518.2	@NODE	1410	

CASE 16 (SUS) W+P1+H

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	63.5	@NODE	1000	STRESS:	87599.8	ALLOWABLE:	137892.
BENDING STRESS:				55503.7	@NODE	1000	
TORSIONAL STRESS:				2604.3	@NODE	29	
AXIAL STRESS:				45872.4	@NODE	1410	
HOOP STRESS:				93249.9	@NODE	1410	
3D MAX INTENSITY:				96261.5	@NODE	1410	

CASE 17 (EXP) L17=L4-L16

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	21.6	@NODE	1200	STRESS:	65345.3	ALLOWABLE:	302402.
BENDING STRESS:				65297.0	@NODE	1200	
TORSIONAL STRESS:				4643.2	@NODE	1350	
AXIAL STRESS:				2261.3	@NODE	1189	
HOOP STRESS:				0.0	@NODE	20	
3D MAX INTENSITY:				75399.3	@NODE	1200	

CASE 18 (EXP) L18=L5-L16

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	68.8	@NODE	210	STRESS:	208866.7	ALLOWABLE:	303707.
BENDING STRESS:				208851.2	@NODE	210	
TORSIONAL STRESS:				10972.1	@NODE	28	
AXIAL STRESS:				3975.1	@NODE	1189	
HOOP STRESS:				0.0	@NODE	20	

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

3D MAX INTENSITY: 237219.0 @NODE 210

## CASE 29 (OCC) L29=L16+L19

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:87.8 @NODE 1180 STRESS:161111.3 ALLOWABLE: 183396.

BENDING STRESS: 130625.1 @NODE 1180

TORSIONAL STRESS: 6113.8 @NODE 1350

AXIAL STRESS: 46012.0 @NODE 1410

HOOP STRESS: 93249.9 @NODE 1410

3D MAX INTENSITY: 187930.4 @NODE 1180

## CASE 30 (OCC) L30=L16+L20

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:72.8 @NODE 1000 STRESS:133455.3 ALLOWABLE: 183396.

BENDING STRESS: 100703.8 @NODE 1000

TORSIONAL STRESS: 3172.6 @NODE 1250

AXIAL STRESS: 46320.5 @NODE 1410

HOOP STRESS: 93249.9 @NODE 1410

3D MAX INTENSITY: 134684.3 @NODE 1000

## CASE 31 (OCC) L31=L16+L21

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:54.5 @NODE 1000 STRESS:99984.6 ALLOWABLE: 183396.

BENDING STRESS: 67639.9 @NODE 1000

TORSIONAL STRESS: 2990.4 @NODE 29

AXIAL STRESS: 46091.7 @NODE 1410

HOOP STRESS: 93249.9 @NODE 1410

3D MAX INTENSITY: 101211.9 @NODE 1000

## CASE 32 (OCC) L32=L16+L22

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:53.3 @NODE 1000 STRESS:97781.4 ALLOWABLE: 183396.

BENDING STRESS: 65615.0 @NODE 1000

TORSIONAL STRESS: 3013.2 @NODE 29

AXIAL STRESS: 45908.8 @NODE 1410

HOOP STRESS: 93249.9 @NODE 1410

3D MAX INTENSITY: 99009.0 @NODE 1000

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

## CASE 33 (OCC) L33=L16+L23

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	70.8	@NODE	1000	STRESS:	129798.6	ALLOWABLE:	183396.
BENDING STRESS:	97396.1	@NODE	1000				
TORSIONAL STRESS:	4347.0	@NODE	1006				
AXIAL STRESS:	46396.1	@NODE	1415				
HOOP STRESS:	93249.9	@NODE	1410				
3D MAX INTENSITY:	131062.0	@NODE	1000				

## CASE 34 (OCC) L34=L16+L24

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	71.3	@NODE	1000	STRESS:	130851.8	ALLOWABLE:	183396.
BENDING STRESS:	98544.5	@NODE	1000				
TORSIONAL STRESS:	4178.1	@NODE	1006				
AXIAL STRESS:	46124.0	@NODE	1415				
HOOP STRESS:	93249.9	@NODE	1410				
3D MAX INTENSITY:	132111.7	@NODE	1000				

## CASE 35 (OCC) L35=L16+L25

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	47.8	@NODE	1000	STRESS:	87599.8	ALLOWABLE:	183396.
BENDING STRESS:	55503.7	@NODE	1000				
TORSIONAL STRESS:	2604.3	@NODE	29				
AXIAL STRESS:	45872.4	@NODE	1410				
HOOP STRESS:	93249.9	@NODE	1410				
3D MAX INTENSITY:	96261.5	@NODE	1410				

## CASE 36 (OCC) L36=L16+L26

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	47.8	@NODE	1000	STRESS:	87599.8	ALLOWABLE:	183396.
BENDING STRESS:	55503.7	@NODE	1000				
TORSIONAL STRESS:	2604.3	@NODE	29				
AXIAL STRESS:	45872.4	@NODE	1410				
HOOP STRESS:	93249.9	@NODE	1410				
3D MAX INTENSITY:	96261.5	@NODE	1410				

# Design of Propylene Gas Pipeline System

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Job name: Compressor Station Piping Stress Analysis - Discharge Line

## CASE 37 (OCC) L37=L16+L27

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	48.7	@NODE 1000	STRESS:89332.0	ALLOWABLE:	183396.
BENDING STRESS:		57204.1 @NODE 1000			
TORSIONAL STRESS:		2622.6 @NODE 29			
AXIAL STRESS:		45951.6 @NODE 1410			
HOOP STRESS:		93249.9 @NODE 1410			
3D MAX INTENSITY:		96697.6 @NODE 1415			

## CASE 38 (OCC) L38=L16+L28

\*\*\*\* CODE STRESS CHECK PASSED

HIGHEST STRESSES: (KPa)

CODE STRESS %:	49.9	@NODE 1000	STRESS:91545.2	ALLOWABLE:	183396.
BENDING STRESS:		59409.0 @NODE 1000			
TORSIONAL STRESS:		2627.1 @NODE 29			
AXIAL STRESS:		45938.7 @NODE 1410			
HOOP STRESS:		93249.9 @NODE 1410			
3D MAX INTENSITY:		96546.8 @NODE 1415			

# Design of Propylene Gas Pipeline System

CAESAR II VERS 4.50

APR 30,2008 18:52:38

Job name: Compressor Station Piping Stress Analysis - Discharge Line

HANGER REPORT

(TABLE DATA FROM DESIGN RUNS)

NODE	NO. REQD	FIG. NO.	VERTICAL SIZE	MOVEMENT (mm.)	HOT LOAD (N.)	THEORETICAL INSTALLED LOAD (N.)	ACTUAL INSTALLED LOAD (N.)	SPRING RATE (N./mm.)	HORIZONTAL MOVEMENT (mm.)
30	1	82	14	1.419	20772.	21170.	0.	280.	0.629
									LOAD VARIATION = 2%
2505	2	82	17	6.070	37703.	41956.	0.	700.	0.129
									LOAD VARIATION = 11%



## 5. RESULT

### PIPELINE DESIGN

Throughput	= 16.68 MSCMD
Length of pipeline	= 10 Km
Supply Pressure	= 171.3913 psia
Supply Temperature	= 27°C
Receiving Terminal Pressure	= 213.35 – 227.57 psia [Minimum Required]
Design Pressure	= 300 psia = MAOP
Fluid Name	= Propylene Gas
Molecular weight	= 42.10
Diameter	= 30 Inch
Thickness	= 0.511 Inch
Grade of Line Pipe	= XS
Hoop stress $S_h$	= 8806.26 psia
Longitudinal stress $S_a$	= 4403.13 psia
Erosional Velocity [ue]	= 99.667 ft/sec
Operating Velocity [u]	= 59.800 ft/sec
Operating Velocity [u]	= 59.9311 ft/sec – Calculated
Reynolds Number $Re$	= 26299987
Transmission factor $[1/f]^{0.5}$	= 20.74
Delivery Terminal Pressure	= 229.2361 psia – Calculated

### COMPRESSOR DETAILS

Compressor Type	= Centrifugal Compressor [Single Stage]
Make	= Hitachi
Maximum Working Pressure	= 334 psia
Maximum Design Inlet Flow	= 696000 m <sup>3</sup> /hr
Design Speed	= 4500 rpm
Compression Ratio	= 1.74
Adiabatic Efficiency $[\eta_a]$	= 0.7982
Overall efficiency $[\eta_o]$	= 0.7822
Power Required	= 15978.76 kW
Suction Pressure $P_1$	= 171.3913 psia
Suction Pressure $P_2$	= 298.2635 psia

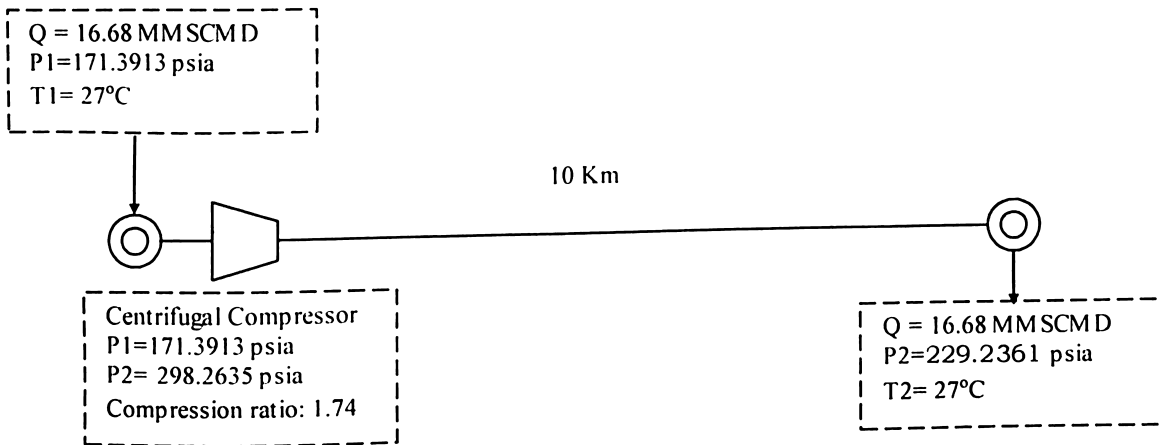


Figure 16 – Pipeline Design simulated Model

## STRESS ANALYSIS RESULT

### COMPRESSOR – SUCTION LINE

#### CASE 4 (SUS) W+P 1

\*\*\*\*CODE STRESS CHECK PASSED\*\*\*\*

Highest Stresses: (kpa)

Code Stress %:45.7 @Node 250 Stress: 62962.3 Allowable: 137892.

Bending Stress: 35357.4 @Node 250

Torsional Stress: 1623.5 @Node 100

Axial Stress: 28432.3 @Node 199

Hoop Stress: 55949.9 @Node 29

3d Max Intensity: 63732.0 @Node 250

### COMPRESSOR – DISCHARGE LINE

#### CASE 29 (OCC)

\*\*\*\*CODE STRESS CHECK PASSED\*\*\*\*

Highest Stresses: (kpa)

code Stress %:87.8 @node 1180

Stress: 161111.3 Allowable: 183396.

Bending Stress:130625.1 @Node 1180

Torsional Stress: 6113.8 @Node 1350

Axial Stress: 46012.0 @Node 1410

Hoop Stress: 93249.9 @Node 1410

3d Max Intensity: 187930.4 @Node 1180

## **6. CONCLUSION**

For the transportation of 16.68 MSCMD propylene gas from the refinery complex to the nearby petrochemical units has been transported through 10 km pipeline is designed to be of 30 inch with the wall thickness of 0.511 inch.

In this project the Process department and the Piping department activities has been carried and their results has been furnished for the effective, efficient and safer transportation of propylene gas to meet the customer demands at proper time to increase the productivity.

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