| Name: |
| :--- | :--- |
| Enrolment No: |


| Progr Cour Cours Nos. Instruc |  | $\begin{aligned} : & \text { III } \\ : & 3 \mathrm{hr} \\ \mathrm{~s} & : 100 \end{aligned}$ |  |
| :---: | :---: | :---: | :---: |
| $\begin{gathered} \text { SECTION A } \\ (\mathbf{5 X 4}=\mathbf{2 0} \text { marks) } \end{gathered}$ |  |  |  |
| S. No. |  | Marks | CO |
| 1 | A mixture of gases has the following composition by weight $\mathrm{N}_{2}=34 \mathrm{Cl}_{2}=22 \% \mathrm{Br}_{2}=$ $25 \%$ and $\mathrm{O}_{2}=19 \%$. Find (i) Composition of the gas mixture by volume \% (ii) Density of the gas mixture in $\mathrm{kg} / \mathrm{m} 3$ at $25^{\circ} \mathrm{C}$ \& 740 mm Hg . | 4 | CO1 |
| 2 | A mixture of acetone vapor and nitrogen gas at atmospheric pressure and 295 K contains acetone vapor to the extent that it exerts a partial pressure of 15 kPa . The vapor pressure of acetone at 295 K is 26.36 kPa . <br> Solve for <br> 1) Molal saturation <br> 2) Absolute saturation <br> 3) Relative saturation <br> \% relative saturation | 4 | CO 2 |
| 3 | 10 kg of $\mathrm{CH}_{4}$ is burnt with $10 \%$ excess air. What will be the volume of the air used for combustion if air is at $30^{\circ} \mathrm{C}$ and 1.3 atm pressure? | 4 | $\mathrm{CO3}$ |
| 4 | Aluminum reacts with chlorine gas to form aluminum chloride via the following reaction: $2 \mathrm{Al}+3 \mathrm{Cl}_{2}--->2 \mathrm{AlCl}_{3}$. If 34 g of aluminum and 39 g of chlorine gas are used. Find limiting reactant and calculate \%excess reactant. | 4 | CO4 |
| 5 | The heat capacity of silicon carbide is given by $C_{P}=37.221+1.22 \times 10^{-3} T-1.189 \times 10^{5} T^{-2}$ where Cp is in $\mathrm{KJ} / \mathrm{Kmol} \mathrm{K}$ and T is in K. Estimate the enthalpy change in silicon carbide in the range 0 to 1000 K . | 4 | CO5 |

## SECTION B

( $4 \times 10=40 \mathrm{marks}$ )

| $\mathbf{6}$ | A gas containing only $\mathrm{CH}_{4}$ and $\mathrm{N}_{2}$ is burned with air yielding a flue gas that has an <br> Orsat analysis of $\mathrm{CO}_{2}: 8.7 \%, \mathrm{CO}: 1.0 \%, \mathrm{O}_{2}: 3.8 \%$, and $\mathrm{N}_{2}: 86.5 \%$. Infer the percent <br> excess air used in combustion and the composition of the $\mathrm{CH}_{4}$ and $\mathrm{N}_{2}$ mixture. | $\mathbf{1 0}$ | $\mathbf{C O 3}$ |
| :---: | :--- | :---: | :---: |
| $\mathbf{7}$ | A 10.20 g sample of a gas has a volume of 5.25 L at $23^{\circ} \mathrm{C}$ and 751 mmHg . If 2.30 g <br> of the same gas is added to this constant 5.25 L volume and the temperature raised to <br> $67{ }^{\circ} \mathrm{C}$, what is the new gas pressure? | $\mathbf{1 0}$ | $\mathbf{C O 4}$ |
| $\mathbf{8}$ | A solution of sodium chloride is available at 343 K which is saturated. This solution <br> when cooled to 298 K, releases 100 g of crystals of NaCl . Estimate the weight of the <br> initial solution at $343 \mathrm{~K} . T h e ~ s o l u b i l i t y ~ o f ~$ <br> NaCl in water at 343 and 298 K are 6.39 and <br> $6.14 \mathrm{kmol} / 1000 \mathrm{~kg}$ water respectively. | $\mathbf{1 0}$ | $\mathbf{C O 5}$ |
| $\mathbf{9}$ | A liquid fermentation medium at $30^{\circ} \mathrm{C}$ is pumped at a rate of $2000 \mathrm{~kg} / \mathrm{h}$ through a <br> heater, where it is heated to $70^{\circ} \mathrm{C}$ under pressure. The waste heat water used to heat <br> this medium enters at $95^{\circ} \mathrm{C}$ and leaves at $85^{\circ} \mathrm{C}$. The average heat capacity of the <br> fermentation medium is $4.06 \mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{K}$, and that for water is $4.21 \mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{K}$. The | $\mathbf{1 0}$ | $\mathbf{C O 6}$ |


|  | fermentation stream and the wastewater stream are separated by a metal surface through which heat is transferred and the streams do not physically mix with each other as shown in figure below. <br> Calculate the water flow rate required and the amount of heat added to the fermentation medium assuming no heat losses. |  |  |
| :---: | :---: | :---: | :---: |
|  | SECTION C (2 $\mathbf{X} 20=40$ marks) |  |  |
| 10 | A simplified process for $\mathrm{SO}_{2}$ to $\mathrm{SO}_{3}$ is as shown in the figure below. <br> Sulfur is burned with $100 \%$ excess air in the burner though the conversion of $\mathrm{SO}_{2}$ is only $90 \%$. In the converter, the conversion from $\mathrm{SO}_{2}$ to $\mathrm{SO}_{3}$ is only $95 \%$. Calculate the lbs of air needed to burn 100 lbs of Sulfur and the composition of exiting stream from the converter. | 20 | CO4 |
| 11 | A natural gas stream has the following composition on mole basis: $\mathrm{CH}_{4}-84 \%, \mathrm{C}_{2} \mathrm{H}_{6}-13 \%$ and $\mathrm{N}_{2}-3 \%$. <br> Analyze the heat to be added to heat 10 kmol of natural gas from 298 K to 523 K using the heat capacity data given below.$C_{P}=a+b T+c T^{2}+d T^{-2}, \mathrm{~kJ} /(\mathrm{kmol}-\mathrm{K})$Gas a $\mathrm{b} \times 10^{3}$ $\mathrm{c} \times 10^{6}$ $\mathrm{~d} \times 10^{9}$ <br> $\mathrm{CH}_{4}$ 19.2494 52.1135 11.973 -11.3173 <br> $\mathrm{C}_{2} \mathrm{H}_{6}$ 5.4129 178.0872 -67.3749 8.7147 <br> $\mathrm{~N}_{2}$ 29.5909 -5.141 13.1829 -4.968 <br> OR <br> One kg of water is heated from 250 K to 400 K at one standard atmospheric pressure. Estimate, how much heat is required for this? <br> Data: The mean heat capacity of ice $\mathrm{Cp}=2.03 \mathrm{KJ} / \mathrm{kmol} \mathrm{K}$ (between 250 and 273 K ) The heat capacity of water between 273 K and 373 K is $1 \mathrm{btu} / \mathrm{lb}{ }^{\circ} \mathrm{F}$. <br> The heat capacity of water vapor from 373 to 400 K is $\mathrm{Cp}=30.475+9.652 \times 10^{-3} \mathrm{~T}+1.189 \times 10^{-6} \mathrm{~T}^{2}$. <br> The latent heat of fusion of water is $144 \mathrm{btu} / \mathrm{lb}$ and that of vaporization is 40608 $\mathrm{KJ} / \mathrm{Kmol}$. | 20 | CO6 |

