Name:

Enrolment No:



UNIVERSITY OF PETROLEUM AND ENERGY STUDIES

End Semester Examination, December 2023

Programme Name: B. Tech. in Chemical Engineering Semester : V
Course Name : Mass Transfer II Time : 3 hrs

Course Code : CHCE 3029 Max. Marks : 100

Nos. of page(s) : 2

Instructions : Attempt all questions. Assume any missing data with proper justification.

S. No.		Marks	CO
	Section A		
Q.1	Discuss the solid-liquid extraction equilibrium. What are the different contact strategies for solid liquid extraction?	10	CO1
Q.2	Define inference, recirculation, cooling range and approach in cooling tower equipment.	10	CO1
Q.3	The equilibrium distribution of A in a gas-liquid system is linear, $Y=\alpha X$; where α is a function of temperature $\ln\alpha=0.3512-\frac{26.462}{T(K)}$ The flow rate of the phases (solute-free basis) are: $G_s=38kmol/h$ and $L_s=49.5kmol/h$. The feed gas has 8% solute in it. Calculation the temperature when absorption factor becomes unity	10	CO2
Q.4	The saturation enthalpy versus temperature data is important to determine the height of the cooling tower. Estimate five data points for saturation enthalpy curve. The vapor pressure of water can be calculated by the following expression $\ln p_A^v \ (bar) = 11.96481 - \frac{3984.923}{T \ (K) - 39.724}$	10	CO2
Q.5	A solid having 20 % solute, 2 % water and the rest inert is to be leached with water at a rate of 2 ton/h. The overflow leaving the countercurrent leaching cascade has 15 % solute and no solid. The underflow carries 0.5 kg solution per kg inert independent of solution concentration. If 97 % of the solute is to be recovered, determine the number of ideal stages required for this solid-liquid extraction operation	10	CO3

Q.6	A 25 % solution of dioxane in water is to be continuously extracted at a rate of 1000 kg/h in a countercurrent extraction system with benzene to remove 95 % of dioxane. The benzene and water are substantially insoluble at this concentration range. Estimate the number of theoretical stages required if 900 kg of benzene is used per hour. The equilibrium distribution of dioxane between water and benzene is as follows:									10	CO3	
	Weight % dioxane in water			5.1		18.9		25.2				
	Weight % dioxane in benzene			5.2		22.5		32				
Q.7					S	ection E	3					
	The followinketone (MEHzeolite) is colored in the following section C/C_o in C/C_o in C/C_o in Data: bed he bed density: If the maxim $C/C_o = 0.03$	(x) from llected 9.5 0 56.2 0.768 sight 0.2 = 700 kg num per , determ	19 0.018 64.7 0.852 2 m, sup g/m ³ rmissible nine the	21 0.037 68.6 0.935 erficial	25.7 0.083 72.4 0.972 gas velo	34.3 0.287 77.1 0.963 ocity = 0	39 0.435 84.8 0.970	le of sil 42 0.491 97.1 0.981 $C_o = 0.$ e effluer	46.7 0.620 104.7 0.991 11 gmol	51.4 0.713 108.6 1	20	CO4
Q.8	In the laboratory drying test of a granular, hygroscopic wet solid, it took 8.5 hours to dry the solid from 28 % to 2 % moisture with a solid loading of 20 kg/m². The critical moisture content is 0.1 and equilibrium moisture content is 0.005. The falling rate of drying is linear in the moisture content. Calculate the time required for drying the material from 25 % to 1.5 % moisture under similar drying conditions. What are the highest and the lowest drying rates? All the moisture contents are on dry basis.									20	CO4	