| Name: <br> Enrolment No: |  |  |  |
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| SECTION A (20 M) |  |  |  |
| S. No. |  | Marks | CO |
| Q1 | Explain the concept of pump priming, NPSH and pump cavitation. | 4 | CO1 |
| Q2 | Explain the behaviour of non- Newtonian fluid, shear rate thinning and shear rate thicknening fluids with their examples. | 4 | CO1 |
| Q3 | What do you understand by major loss and minor loss. | 4 | CO1 |
| Q4 | Elaborate the advantages and limitations of venturi meter and orifice meter. | 4 | CO1 |
| Q5 | Discuss the static, dynamic, stagnation and piezometric pressure. | 4 | CO1 |
| SECTION B (40 M) |  |  |  |
| Q6 | Two coaxial glass tubes forming an annulus with a small gap are immerged in water. The inner and outer radii of the annulus are $\mathrm{r}_{2}$ and $\mathrm{r}_{1}$ respectively. What is the capillary rise of water in the annulus if the surface tension of water is $0.073 \mathrm{~N} / \mathrm{m}$ and contact angle is 30 degree. Derive the expression and solve the problem. | 10 | CO3 |
| Q7 | A nozzle is used to increase the velicity of fluid. A fluid whose density and velocity varies with the position in the pipeline. The velocity ( $u$ ) and density ( $\rho$ ) fields if the fluid through the nozzle is given by, $u=u_{0} e^{\left(-\frac{2 x}{L}\right)}$ and $\rho=\rho_{0} e^{\left(-\frac{x}{L}\right)}$. Show that the rate of change of density in Lagrangian frame of reference is $\frac{-0.05 u_{0} \rho_{0}}{L}$. | 10 | CO2 |
| Q8 | The velocity distribution for a fully developed laminar flow in a circular pipe of radius, R , is given by, $u=-\frac{R^{2}}{4 \mu} \frac{d P}{d x}\left[1-\left(\frac{r}{R}\right)^{2}\right]$. Determine the expressions for total discharge and pressure drop through the pipe of length $L$. The terms have their usual meanings. | 10 | CO 3 |


| Q9 | A metal plate $1.25 \mathrm{~m} \times 1.25 \mathrm{~m} \times 6 \mathrm{~mm}$ thick and weighing 90 N is placed midway in the 24 mm gap between the two vertical plane surfaces. The gap is filled with an oil of specific gravity 0.85 and dynamic viscosity $3.0 \mathrm{~N} . \mathrm{s} / \mathrm{m}^{2}$. Determine the force required to lift the plate with a constant velocity of $0.15 \mathrm{~m} / \mathrm{s}$. | 10 | CO 2 |
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|  | SECTION C (40 M) |  |  |
| Q10 | An hydrocarbon oil (mol. wt. $=220$; density $=1.8 \mathrm{gm} / \mathrm{cc}$. , and viscosity $=0.005 \mathrm{~Pa} . \mathrm{s}$ ) is beinh pumped from a storage tank at ground floor to the top of the distillation column of height 10 m at the rate of $2000 \mathrm{~kg} / \mathrm{min}$ through a 5 cm inner diameter smooth pipe. The pump efficiency is $60 \%$, calculate the pump power rwquirement. The losses of the pump can be taken as $1.5 \mathrm{kgf}-\mathrm{m} / \mathrm{kg}$. | 20 | $\mathrm{CO4}$ |
| Q11 | A necked-down or venturi section of a pipe flow develops a low pressure which can be used to aspirate liquid upward from a reservoir as shown in Figure below. Develop an expression for the exit velocity $V_{2}$ which is just sufficient to cause the reservoir liquid to rise in the tube up to section 1 . Consider the liquid originally flowing through the pipe and that to be pumped from the reservoir are same (neglect frictional losses). | 20 | $\mathrm{CO4}$ |

