| Name: <br> Enrolment No: |  |  |  |  |  |  |  |
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| Programme Name: B. Tech. APE (Gas) Semester $:$ IV <br> Course Name $:$ Natural Gas Engineering Time <br> Course Code $:$ CHCE 3001 $: 03 \mathrm{hrs}$ <br> Nos. of page(s) $:$ 4 Max. Marks <br> Instructions:    <br> $\quad \checkmark$ Draw diagrams wherever necessary   <br> $\checkmark$ Attempt questions in sequence   <br> $\checkmark$ Appendix with all the tables and graphs are attached at the end of the question paper   |  |  |  |  |  |  |  |
| SECTION A ( 5 X 4= 20 Marks) Answer all questions |  |  |  |  |  |  |  |
| S. No. |  |  |  |  |  | Marks | CO |
| 1. | Explain bio | and therm | mechanism |  |  | 4M | CO1 |
| 2. | The follow systems. T hydrocarbo | list of the positions ms. | ositional ressed in | of differe of mol\% | rocarbon <br> sify <br> System \#4 <br> 12.15 <br> 3.10 <br> 2.51 <br> 2.61 <br> 2.78 <br> 4.85 <br> 72.00 | 4M | CO 2 |
| 3. | Describe the working principle of an axial flow compressor. |  |  |  |  | 4M | CO3 |
| 4. | Compare orifice types including their effect on gas flow measurement. |  |  |  |  | 4M | CO 4 |
| 5. | Articulate the functions of a well-designed separator. |  |  |  |  | 4M | CO5 |
| SECTION B ( $4 \times 10=40$ Marks) <br> Answer all questions |  |  |  |  |  |  |  |
| 6. | a) Solve for compressibility for the given gas composition at 200 psia and $80^{\circ} \mathrm{F}$. $\mathrm{N}_{2}-1 \%, \mathrm{C}_{1}-89 \%, \mathrm{C}_{2}-5 \%$ and $\mathrm{C}_{3+}=5 \%$. Assume the C3+ fraction to be equivalent to $\mathrm{n}-$ $\mathrm{C}_{5}$. |  |  |  |  | $\begin{gathered} (5+5) \\ 10 \mathrm{M} \end{gathered}$ | $\begin{gathered} \mathrm{CO} 1 \\ \& \\ \mathrm{CO} 2 \end{gathered}$ |


|  | b)Illustrate the P-T diagram of ethane and heptane system |  |  |
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| 7. | A gas is being compressed from 150 psia and $200^{\circ} \mathrm{F}$ to 2000 psia. Determine its compression parameters at the suction end. The gas has the following composition expressed as mole fraction. $\mathrm{C}_{1}=0.9134, \mathrm{C}_{2}=0.0456, \mathrm{C}_{3}=0.0175$, $\mathrm{i}-\mathrm{C}_{4}=0.0043$, n $\mathrm{C}_{4}=0.0044, \mathrm{i}-\mathrm{C}_{5}=0.0148$. | 10M | CO3 |
| 8. | A 4-in diameter orifice meter is installed in a pipe with an inside diameter of 12.09 in . The differential pressure is measured at 30 in of water and the static pressure upstream is 600 psig . Gas gravity $=0.6$, gas flowing temperature $=70^{\circ} \mathrm{F}$. The base temperature and the base pressure are $60^{\circ} \mathrm{F}$ and 14.7 psia , respectively. Assuming flange taps, calculate the flow rate in standard $\mathrm{ft}^{3} / \mathrm{h}$. The barometric pressure is 14.5 psia . | 10M | CO 4 |
| 9. | Illustrate the working of a vertical separator with a neat diagram, its advantages and disadvantages. | 10M | CO5 |
|  | SECTION C ( $2 \times 20=40$ Marks) |  |  |
| 10. | Solve the adiabatic horsepower required to compress 1 MMcfd of a 0.6 grvaity natural gas from 100 psia and $80^{\circ} \mathrm{F}$ to 1600 psia . Intercoolers cool the gas to $80^{\circ} \mathrm{F}$. What is the heat load on the intercoolers and what is the final gas temperature. <br> Use: <br> a) The enthalpy -entropy diagram | 20M | CO3 |


|  | b) Analytical expressions. |  |  |
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| 11. | Meter equipped with flange taps, with static pressure from downstream tap: <br> D1 = line size=8.071 in. actual ID <br> D2=orifice size $=1$ in <br> Flowing temperature $=65^{\circ} \mathrm{F}$ <br> Ambient temperature $=70^{\circ} \mathrm{F}$ <br> Base pressure $=14.65 \mathrm{psia}$ <br> Base temperature $=50^{\circ} \mathrm{F}$ <br> Specific gravity $=0.570$ <br> Total heating value=999.1 Btu/cu ft <br> Mole fraction of nitrogen content $=0.011$ <br> Mole fraction of carbon dioxide content $=0$ <br> Average differential head=50 in water <br> Average downstream gauge pressure $=370$ psig <br> Solve for the orifice flow constant and the quantity rate of flow for 1 hour at base conditions | 20M | CO4 |
|  | (Or) |  |  |
|  | a)A metering system is required to measure approximately 8.5 MMSCFD of 0.62 gravity gas at a line pressure of 250 psig The meter run is to be made of 8 in pipe (7.981 in ID). Determine the size of the orifice plate to give a differential of about 50 inches. Flowing temperature averages about $80^{\circ} \mathrm{F}$. Use flange taps. <br> b)A 2 in [ 5.1 cm ] orifice plate is used in 3.438 in [ 8.7 cm ] ID pipeline. The differential pressure is 30 in of water. The static pressure upstream is 80 psia and the specific gravity is 0.65 . The flowing temperature of gas is $80^{\circ} \mathrm{F}$. Flange taps are used. Assume $F t b=F p b=1$. Calculate the gas flow rate through the pipe. | $\begin{gathered} (10+10) \\ 20 \mathrm{M} \end{gathered}$ | CO 4 |

