Name:

Enrolment No:



Semester: 6

UNIVERSITY OF PETROLEUM AND ENERGY STUDIES

End Semester Examination, May 2022

Course: Advanced Production Engineering

Program: M. Tech (PE)

Course Code: PEAU 7019

Time : 03 hrs.

Max. Marks: 100

Instructions: There is internal choice in Q9 & Q11

SECTION A (5Qx4M=20Marks)

S. No.		Marks	CO
Q 1	Define the following terms:		601
	a) cavitation b) liquid re-entrainment	4	CO1
Q 2	Classify the types of pumps used in oil and gas industry	4	CO2
Q 3	Classify the types of compressors used in oilfield	4	CO2
Q 4	State the retention time (in minutes or hours) of following pressure vessels used in surface production facility: a) FWKO b) Gunbarrel c) vertical heater treater d) electrostatic heater treater	4	CO3
Q 5	State the typical treating temperature (in °F) for loose, moderate, tight, very viscous emulsions operating inside a) Gunbarrel b) heater treater c) electrostatic heater treater	4	CO4
	SECTION B		•
	(4Qx10M= 40 Marks)		
Q 6	Name the equipment, draw any one schematic sketch and explain the process in brief, in which oil must be held at a temperature for a specific period of time to enable de-emulsifying the water in-oil emulsion.	10	CO3
Q 7	 a) Write four important objectives of stage separation in a surface production facility b) Estimate the free settling velocity (in ft/hr) of a 100 μm brine drop in oil. Following data is given: Specific Gravity of oil = 0.8, viscosity of oil = 10 cP, Specific Gravity of brine = 1.02 	10	CO4
Q 7 Q 8	surface production facility b) Estimate the free settling velocity (in ft/hr) of a 100 μm brine drop in oil. Following data is given: Specific Gravity of oil =	10	CO4

	considerations.		
	OR Discuss the potential operating problems during operation of a vertical separator		
	SECTION-C (2Qx20M=40 Marks)		
Q 10	a) Discuss in detail about vessel internal parts of a two-phase separatorb) Size a vertical 2 phase separator to determine diameter & seam		
0.11	to seam length of it. Following data is given: Gas flow rate = 10 mmscfd @ 0.6 specific gravity Oil flow rate = 2000 bopd @ 40 °API Operating Pressure of vessel = 1000 psia Operating Temperature of vessel = 60 °F diameter of droplet size to be removed = 140 µm Viscosity = 0.013 cP Gas compressibility factor = 0.84 Drag coefficient = 0.851	20	CO5
Q 11	 a) State the primary and secondary condition for hydrates formation b) State the function of baffles used in shell & tube heat exchanger c) Discuss about estimation of settling velocity of water with the law applicable d) Following data is given: 	20	CO6
	Gas flow rate = 25 mmscfd Oil flow rate = 3000 bopd Operating Pressure = 800 psig Operating Temperature = 80 F Flowing gas density = 3.4 lb/ft3 (for 20.3 Molecular Weight gas) Flowing oil density = 51.5 lb/ft3 (40 °API) Two phase separator is used. Calculate the diameter of vessel (in ft) and liquid capacity (in bbl/day). Assume 10 ft shell height of separator which is 30% liquid full. The value of constant, depending upon design and operating conditions, is 0.3		
	e) Define emulsion and emulsifying agents. State and explain the factors on which stability of emulsion depends upon.		
	OR		

- a) Discuss about the type of devices used for measurement of oil and gas flow rate.
- b) A liquid hydrocarbon (having density = 788.4 kg/m³ & viscosity = 5.857 * 10⁻⁷ kg/m–sec) flows through a pipe with inner diameter 4 cm and orifice meter installed to measure volumetric flow rate. Discharge coefficient is having the value of 0.61. The 2 pressure taps are connected to Hg U tube manometer (density of Hg = 13600 kg/m³) and column height difference is 11 cm. The ratio of orifice diameter to pipe diameter is 0.75. Calculate volumetric flowrate of hydrocarbon.
- c) Size a horizontal 3 phase separator. Following data is given:
 Oil flow rate= 5000 bpd @ 30 °API
 Water flow rate = 3000 bpd @ 1.07 specific gravity
 Gas flow rate = 5 mmscfd @ 0.6 specific gravity
 Operating pressure = 100 psia
 Operating temperature = 90 °F
 Retention time of oil = retention time of water = 10 min
 Viscosity of oil = 10 cP & Viscosity of water = 1 cP
 Gas density = 0.3 lb/ ft³ & Liquid density = 54.7 lb/ft³
 Drag coefficient = 2.01 & Gas compressibility factor = 0.99
 Droplet removal criterion is 100 microns liquids, 500 microns
 H₂O and 200 microns oil. Vessel is half full of liquid.