| Name: <br> Enrolment No: |  | Y@ |  |
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| Course <br> Program <br> Course <br> Instruc <br> $\checkmark$ Atte <br> Assume | UNIVERSITY OF PETROLEUM AND ENERGY STUDIES End Semester Examination, December 2022 | ks : 10 <br> marks). |  |
| SECTION-A |  |  |  |
| S. No. |  | Marks | CO |
| 1. | Make the following conversions: <br> (i) Pressure of 5 atm to cm Hg <br> (ii) $127 \mathrm{lb} / \mathrm{ft}^{3}$ to $\mathrm{gr} / \mathrm{cm}^{3}$ <br> (iii) 499 g of $\mathrm{CuSO}_{4} .5 \mathrm{H}_{2} \mathrm{O}$ into moles <br> (iv) $7.2 \mathrm{mg} / \mathrm{ml} \mathrm{CaCl}_{2}$ to normality | 12 M | CO1 |
| 2. | (a) Explain Limiting reactant, excess reactant, and percent excess reactant <br> (b) Ammonia reacts with sulfuric acid giving ammonium sulphate: $2 \mathrm{NH}_{3}+\mathrm{H}_{2} \mathrm{SO}_{4} \rightarrow\left(\mathrm{NH}_{4}\right)_{2} \mathrm{SO}_{4}$ <br> (i) $20 \mathrm{~m}^{3}$ of ammonia at 1.2 bar and 300 K reacts with 40 kg of sulphuric acid. Which one is the excess reactant and what is the percent excess? <br> (ii) How much ammonium sulphate is obtained | $4+8 \mathrm{M}$ | CO1 |
| 3. | It is desired to compress 10 lb of carbon dioxide to a volume of 20 cu ft . Calculate the pressure in pounds per square inch which is required at temperature of $30^{\circ} \mathrm{C}$ assuming the applicability of the ideal gas law. | 12 M | CO1 |
| 4. | $1000 \mathrm{~kg} / \mathrm{h}$ of a thermic fluid, to be used as a heat transfer medium, is being indirectly heated in a heater from 380 K to 550 K . Calculate the heat load on the heater in kW . The heat capacity equation for thermic fluid is $C_{P}=1.436+2.18 \times 10^{-3} T$ <br> Where $\mathrm{C}_{\mathrm{P}}$ is in $\mathrm{kJ} / \mathrm{kg} . \mathrm{K}$ and T is in K . | 12 M | CO2 |
| 5. | In a process for producing caustic $(\mathrm{NaOH}), 4000 \mathrm{~kg} / \mathrm{h}$ of a solution containing $10 \mathrm{wt} \%$ NaOH is evaporated in the first evaporator, giving a $20 \% \mathrm{NaOH}$ solution. This is then fed into a second evaporator, which gives a product of $50 \% \mathrm{NaOH}$. Calculate the following: <br> (a) The amount of water removed from each evaporator <br> (b) The capacity of triple effect evaporator | 12 M | CO 2 |

## SECTION-B

6. A wet solid containing $75 \%$ water is mixed with recycled dry solid to reduce the water content to $50 \%$ before being admitted into the granulator. The solid leaving the granulator is fed to a drier where it is brought into contact with dry air initially containing $0.20 \%$ water by weight. In the drier, the air picks up moisture and leaves with a moisture content of $5 \%$. The solids leaving the drier contain $25 \%$ water. A portion of solid is recycled. For $500 \mathrm{~kg} / \mathrm{h}$ of wet solid sent to the granulator as fresh feed, determine:
(a) The amount of solid recycled
(b) The circulation rate of air in the drier on a dry basis.
7. A solution of $10 \%$ (weight) acetone in water is subjected to fractional distillation at a rate of $1000 \mathrm{~kg} / \mathrm{h}$ to produce a distillate containing $90 \%$ acetone and a bottom product containing not more than $1 \%$ acetone. The feed enters at 340 K , distillate and residue leave the tower at 300 K and 370 K , respectively. A reflux ratio of 8 is employed. The rise in temperature of 30 K is permitted for the cooling water circulated in the condenser employed for condensing the vapors into the distillate product and the reflux. Saturated steam 276 kPa is available for supplying the heat of vaporization in the reboiler. Heat
$20 \mathrm{M} \quad \mathrm{CO} 4$

20 M
CO losses from the column may be neglected. The heat capacity of acetone is $2.2 \mathrm{~kJ} / \mathrm{kg} . \mathrm{K}$ and that of water is $4.2 \mathrm{~kJ} / \mathrm{kg} . \mathrm{K}$. The boiling point of $90 \%$ acetone-water solution is 332 K . The latent heat of vaporization of acetone at 332 K is $620 \mathrm{~kJ} / \mathrm{kg}$ and that of water is $2500 \mathrm{~kJ} / \mathrm{kg}$. $\lambda_{\text {steam }}$ at 276 kPa is $2730 \mathrm{~kJ} / \mathrm{kg}$. Calculate the cooling water circulation rate, and the rate of circulation of steam.

