| Name: <br> Enrolment No: |  | 1 UPES UNIVERSITY WITH A PURPOSE |  |
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| UNIVERSITY OF PETROLEUM AND ENERGY STUDIES  <br> End Semester Examination (Online Mode)  <br> Course: Chemical Reaction Engineering Semester: VIII <br> Program: B. Tech APE GAS Time $: \mathbf{0 3}$ hrs. <br> Course Code: CHEG 333 Max. Marks: $\mathbf{1 0 0}$ <br> Instructions:  |  |  |  |
| Each Question will carry 5 Marks $\quad$ SECTION A |  |  |  |
| S. No. |  | Marks | CO |
| Q 1 | A first order reaction is to be treated in a series of two mixed reactors. The total volume of the two reactors is <br> a) Minimum when the reactors are of different sizes <br> b) Maximum when the reactors are equal in size <br> c) Minimum when the reactors are equal in size | 5 | CO5 |
| Q2 | For identical feed compositions, flow rate and for elementary first order reactions, N equal size mixed reactors in series with a total volume V gives the same conversion as a single plug flow reactor of volume V for constant density systems. This is true for <br> a) $\mathrm{N}=1$ <br> b) $\mathrm{N}=\infty$ <br> c) $\mathrm{N}>1$ <br> d) $\mathrm{N}<1$ | 5 | CO5 |
| Q3 | For the irreversible unimolecular type reaction, A ---- products in a batch reactor, $80 \%$ reactant $\mathrm{A}\left(\mathrm{C}_{\mathrm{A} 0}=1 \mathrm{~mole} / \mathrm{lit}\right)$ is converted in a 480 second run and conversion is $90 \%$ after 18 min . The order of this reaction is <br> a) 1 <br> b) 2 <br> c) $1 / 2$ <br> d) $3 / 2$ | 5 | CO1 |
| Q4 | Suppose doubling the concentration of a reactant increased the rate of reaction by a factor of 4 , and tripling the concentration of the reactant increases the reaction rate by a factor of 9 . Then the rate of reaction is proportional to the concentration of the reactant raised to the <br> a) First power <br> b) Second power <br> c) Third power <br> d) Fourth power | 5 | CO2 |
| Q5 | For a steady state mixed reactor, the space time is equivalent to the holding time for <br> a) Constant fluid density systems <br> b) Variable fluid density systems <br> c) Non isothermal gas reactions <br> d) Gas reactions with changing number of moles. | 5 | CO 3 |


| Q6 | One liter per second of gaseous reactant A is introduced into a mixed reactor. The stoichiometry is A ----- 3 R , the conversion is $50 \%$ and under these conditions the leaving flow rate is 2 liters per second. The space time for this operation is <br> a) 1 sec <br> b) $1 / 2 \mathrm{sec}$ <br> c) 2 sec <br> d) $1 / 3 \mathrm{sec}$ | 5 | CO4 |
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|  | SECTION B |  |  |
| Each question will carry 10 marks |  |  |  |
| Q 7 | A 10-minute experimental run shows that $75 \%$ of liquid reactant is converted to product by a $1 / 2$ order rate. What would be the fraction converted in a half-hour run? | 10 | CO1 |
| Q8 | For irreversible first order series reaction A- $\qquad$ S, the value of rate constants $\mathrm{k}_{1}$ and $\mathrm{k}_{2}$ are $0.17(\mathrm{~min})^{-1}$ and $0.11(\mathrm{~min})^{-1}$ respectively. Calculate (i) the time at which the concentration of R is maximum and (ii) maximum concentration of R . Take $\mathrm{C}_{\mathrm{A} 0}=$ $1.25 \mathrm{~mol} / \mathrm{l}$. | 10 | CO2 |
| Q9 | Consider a feed with $\mathrm{C}_{\mathrm{A} 0}=100, \mathrm{C}_{\mathrm{B} 0}=200$ and $\mathrm{C}_{\mathrm{i} 0}=100$ enters a steady flow reactor in which isothermal gas phase reaction $A+3 B----6 R$ takes place. Determine $C_{B}$, $\mathrm{X}_{\mathrm{B}}, \mathrm{X}_{\mathrm{A}}$ at the exit of the reactor if $\mathrm{C}_{\mathrm{A}}$ at exit is 40 | 10 | $\mathrm{CO3}$ |
| Q10 | An aqueous feed of A and B ( $400 \mathrm{liter} / \mathrm{min}, 100 \mathrm{mmol} \mathrm{A} / \mathrm{liter}, 200 \mathrm{mmol} \mathrm{B} / \mathrm{liter}$ ) is to be converted to product in a plug flow reactor. The kinetics of the reaction is represented by mol A+B---- R, $-r_{A}=200 \mathrm{C}_{\mathrm{A}} \mathrm{C}_{\mathrm{B}} \mathrm{mol} /$ liter .min Find the volume of reactor needed for $99.9 \%$ conversion of A to product. | 10 | CO4 |
| Q11 | Liquid reactant A decomposes as per reaction scheme: <br> With rate equations: $\begin{aligned} & \mathrm{r}_{\mathrm{R}}=\mathrm{k}_{1} C_{A}^{2}, \quad \mathrm{~K}_{1}=0.4 \mathrm{~m}^{3} /(\mathrm{mol} . \mathrm{Min}) \\ & \mathrm{r}_{\mathrm{S}}=\mathrm{K}_{2} \mathrm{C}_{\mathrm{A}}, \quad \mathrm{~K}_{2}=2(\mathrm{~min})^{-1} \end{aligned}$ <br> An aqueous feed $\mathrm{A}(\mathrm{CA} 0=40 \mathrm{~mol} / \mathrm{m} 3)$ enters a reactor, decomposes, and a mixture of $A, R$, and $S$ leaves <br> Find $C_{R}$, and $C_{S}$ and $\tau$ for $X_{A}=0.9$ in a mixed flow reactor. <br> OR <br> Find $C_{R}$, and $C_{S}$ and $\tau$ for $X_{A}=0.9$ in a plug flow reactor. | 10 | CO5 |
| Each Question carries 20 Marks. |  |  |  |
| Q 12 | It is desired to produce $4000 \mathrm{kmol} /$ day of ethylene glycol. The reactor is operated isothermally. A $16.05 \mathrm{kmol} / \mathrm{m} 3$ solution of ethylene oxide in water is fed to the CSTR | 20 | CO5 |

together with an equal volumetric solution of water containing $90 \%$ by weight $\mathrm{H}_{2} \mathrm{SO}_{4}$. If $80 \%$ conversion is to be achieved, find the volume of reactor. How many CSTRs, each having volume 3 m 3 , would be required to if they are arranged in parallel? What is the corresponding conversion? How many CSTRs each having volume 3 m 3 would be required to if they are arranged in series? What is the corresponding conversion? The first order reaction rate constant is 0.311 (min)-1.

OR
The elementary irreversible aqueous-phase reaction $A+B----R+S$ is carried out isothermally as follows. Equal volumetric flow rates of two liquid streams are introduced into a 4-liter mixing tank. One stream contains $0.020 \mathrm{~mol} \mathrm{~A} / l i t e r$, the other $1.400 \mathrm{~mol} \mathrm{~B} /$ liter. The mixed stream is then passed through a 16 -liter plug flow reactor. We find that some R is formed in the mixing tank, its concentration being 0.002 $\mathrm{mol} / \mathrm{liter}$. Assuming that the mixing tank acts as a mixed flow reactor, find the concentration of R at the exit of the plug flow reactor as well as the fraction of initial A that has been converted in the system.

