| Name: <br> Enrolment No: |  |  |  |
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| UNIVERSITY OF PETROLEUM AND ENERGY STUDIES <br> End Semester Examination, December 2020   <br> Course: Engineering Thermodynamics   <br> Program: B. Tech. (APE-Gas)   <br> Course Code: MECH 2001   <br>    <br> Instructions: Assume any missing data. The notations used here have the usual meanings. Draw the diagrams,   <br> wherever necessary.   |  |  |  |
| SECTION - A (6 $\times 5$ = 30 marks) <br> (Answer all the questions) |  |  |  |
| S. <br> No. |  | Marks | CO |
| 1. | A Carnot engine operates between temperature levels of 600 K and 300 K . It derives a Carnot refrigerator, which provides cooling at 250 K and discards heat at 300 K . Determine the numerical value for the ratio of heat extracted by refrigerator to the heat delivered to the engine. <br> (a) 1 <br> (b) 1.5 <br> (c) 2 <br> (d) 2.5 | 5 | CO2 |
| 2. | $50 \mathrm{kmol} / \mathrm{h}$ of air is compressed from 1.2 bar to 6 bar in a steady flow compressor. Delivered mechanical power is 98.8 kW . Temperatures and velocities at the inlet point are 300 K and $10 \mathrm{~m} / \mathrm{s}$ \& exit point are \& 520 K and $3.5 \mathrm{~m} / \mathrm{s}$. Estimate the rate of heat transfer from the compressor. Assume for air that $\mathrm{C}_{\mathrm{p}}=3.5 \mathrm{R}$ and enthalpy is independent of pressure. <br> (a) -5.9 kW <br> (b) -10.5 kW <br> (c) -15.9 kW <br> (d) -18.9 kW | 5 | CO2 |
| 3. | At 286 K and 139.3 bar, the compressibility factor of methane is found to be 0.8 . At approximately what temperature and pressure, nitrogen will give the compressibility | 5 | $\mathrm{CO3}$ |


|  | factor of 0.8 . The critical temperature and pressure are 190.7 K and 45.8 bar for methane \& 126.2 K and 33.5 bar for nitrogen. <br> (a) 189 K and 101 bar <br> (b) 229 K and 111 bar <br> (c) 286 K and 33.5 bar <br> (d) 84 K and 11.2 bar |  |  |
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| 4. | Assuming that $\mathrm{CO}_{2}$ obeys the ideal gas law, calculate the density of $\mathrm{CO}_{2}$ in $\mathrm{kg} / \mathrm{m}^{3}$ at 540 K and 202 kPa <br> (a) 1 <br> (b) 2 <br> (c) 3 <br> (d) 4 | 5 | $\mathrm{CO3}$ |
| 5. | An ideal solution containing $40 \% \mathrm{~A}$ and $60 \% \mathrm{~B}$ is in equilibrium with its vapor. The vapor pressures of pure liquids at equilibrium temperature are 80 kPa for A and 40 kPa for B. The Vapor composition is <br> (a) $80 \% \mathrm{~A}$ <br> (b) $67 \% \mathrm{~A}$ <br> (c) $57 \% \mathrm{~A}$ <br> (d) $40 \% \mathrm{~A}$ | 5 | $\mathrm{CO4}$ |
| 6. | One ton of refrigeration is equal to <br> (a) $21 \mathrm{~kJ} / \mathrm{min}$ <br> (b) $210 \mathrm{~kJ} / \mathrm{min}$ <br> (c) $420 \mathrm{~kJ} / \mathrm{min}$ <br> (d) $620 \mathrm{~kJ} / \mathrm{min}$ | 5 | $\mathrm{CO5}$ |
|  | SECTION - B ( $\mathbf{5} \times \mathbf{1 0}=\mathbf{5 0}$ marks) <br> (Answer all the questions) |  |  |
| S. <br> No. |  | Marks | CO |
| 1. | A steel casting weighing 2 kg has an initial temperature of $500^{\circ} \mathrm{C}, 40 \mathrm{~kg}$ of water initially at $25^{\circ} \mathrm{C}$ is contained in a perfectly insulated steel tank weighing 5 kg . The casting is immersed in the water and the system is allowed to come to equilibrium. What is the | 10 | CO1 |


|  | final temperature? Ignore any effect of expansion or contraction, and assume constant specific heats of $4.18 \mathrm{~kJ} / \mathrm{kg}-\mathrm{K}$ for water and $0.50 \mathrm{~kJ} / \mathrm{kg}-\mathrm{K}$ for steel. |  |  |
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| 2. | For an ideal gas, prove that $\frac{\Delta S}{R}=\int_{T_{0}}^{T} \frac{C_{v}^{i g}}{R} \frac{d T}{T}+\ln \frac{V}{V_{0}}$ <br> where $\mathrm{T}_{0}$ and $\mathrm{V}_{0}$ are initial temperature and molar volume, respectively. | 10 | $\mathrm{CO2}$ |
| 3. | One cubic meter of an ideal gas at 600 K and 1000 kPa expands to five times its initial volume by a mechanically reversible, adiabatic process. Calculate the final temperature, pressure and work done by the gas for both cases. $\mathrm{C}_{\mathrm{p}}=21 \mathrm{~J} / \mathrm{mol}-\mathrm{K}$. | 10 | $\mathrm{CO3}$ |
| 4. | The excess Gibbs energy of a binary mixture at T and P is given by $\frac{G^{E}}{R T}=\left(-2.6 x_{1}-1.8 x_{2}\right) x_{1} x_{2}$ <br> Find expressions for $\ln \gamma_{1}$ and $\ln \gamma_{2}$. | 10 | $\mathrm{CO3}$ |
| 5. | A mixture of $25 \%$ n-pentane, $45 \%$ n-hexane and rest n -heptane is brought to a condition of $93{ }^{\circ} \mathrm{C}$ and 2 atm . All percentages are mole percentages. The $\mathrm{K}_{\mathrm{i}}$ values of n -pentane, n -hexane and n-heptane are $2.150,0.960$ and 0.430 , respectively. <br> (a) What molar fraction of the system is liquid? <br> (b) What are the phase composition of liquid and vapor? | 10 | $\mathrm{CO4}$ |
| SECTION - C ( $\mathbf{1} \times \mathbf{2 0}=\mathbf{2 0}$ marks $)$ <br> (Answer all the questions) |  |  |  |
| 1. | A refrigerator with tetrafluoroethane as refrigerant operates with an evaporation temperature of $-26^{\circ} \mathrm{C}$ and a condensation temperature of $27^{\circ} \mathrm{C}$. Saturated liquid refrigerant from the condenser flows through an expansion valve into the evaporator, from which it emerges as saturated vapor. <br> (a) For a cooling rate of 5.275 kW , what is the circulation rate of the refrigerant? <br> (b) By how much would the circulation rate be reduced if the throttle valve were replaced by a turbine in which the refrigerant expands isentropically? <br> (c) Determine the coefficient of performnce for isentropic compression of the vapor for part (a) and (b). | 20 | $\mathrm{CO5}$ |

Table: 1 Thermodynamic properties of Saturated Tetrafluoroethane

| Temperature <br> $\left({ }^{0} \mathrm{C}\right)$ | Saturation <br> pressure <br> MPa | Liquid <br> density <br> $\mathrm{kg} / \mathrm{m}^{3}$ | Specific <br> volume of <br> vapor $\mathrm{m}^{3} / \mathrm{kg}$ | Enthalpy <br> $(\mathrm{kJ} / \mathrm{kg})$ |  | Entropy <br> $(\mathrm{kJ} / \mathrm{kg}-\mathrm{K})$ |  |
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|  | P | $\rho^{1}$ | $\mathrm{~V}^{\mathrm{V}}$ | $\mathrm{H}^{\mathrm{l}}$ | $\mathrm{H}^{\mathrm{V}}$ | $\mathrm{S}^{1}$ | $\mathrm{~S}^{\mathrm{V}}$ |
|  | 0.10133 | 1374.3 | 0.19016 | 166.07 | 382.90 | 0.8701 | 1.7476 |
| 24 | 0.64566 | 1210.1 | 0.03189 | 233.05 | 411.93 | 1.1149 | 1.7169 |
| 28 | 0.72676 | 1194.9 | 0.02829 | 238.77 | 413.95 | 1.1338 | 1.7155 |



