| Name: <br> Enrolment No: |  |  |  |
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| UNIVERSITY OF PETROLEUM AND ENERGY STUDIES END Semester Examination, December 2019 |  |  |  |
| Programme Name: M.Tech-Energy System Semester :I  <br> Course Name $\quad:$ Thermodynamics and Heat Transfer Systems Time Max. Marks: $\mathbf{1 0 0}$ <br> Course Code $\quad:$ EPEC7028   <br> Nos. of page(s) $: \mathbf{3}$   <br> Instructions:   <br> i. There are three sections viz. Section A, Section B and Section C. Section A carries 20 marks, Section B carries 40   <br> $\quad$ marks and Section C carries 40 marks   <br> ii. $\quad$ Attempt all the questions in Section A, $B$ and any two in section $C$   <br> iii. $\quad$ Make appropriate assumptions wherever required   |  |  |  |
| SECTION A - 20 Marks |  |  |  |
| S. No. |  | Marks | CO |
| Q 1 | A closed thermodynamic system employs the cycle shown in the figure below: <br> If the system performs as a heat engine and the heat transfer to the low temperature heat reservoir is 50 MJ , determine the thermal efficiency of the cycle | 5 | $\mathrm{CO4}$ |
| Q 2 | It is impossible to construct a heat engine working on single reservoir. Interpret? | 5 | CO4 |
| Q 3 | An object is initially at a temperature above that of its surroundings. We have seen that many kinds of convective process will bring the object into equilibrium with its surroundings. Describe the characteristic of a process that will do so with the least net increase of the entropy of the universe. | 5 | $\mathrm{CO4}$ |
| Q. 4 | Is it possible to increase the heat transfer from a convectively cooled isothermal sphere by adding insulation? Explain fully. | 5 | CO1 |
| SECTION-B (40 Marks) |  |  |  |
| Q 6 | Humans are able to control their heat production rate and heat loss rate to maintain a nearly constant core temperature of $\mathrm{T}_{\mathrm{c}}=37^{\circ} \mathrm{C}$ under a wide range of environmental conditions. This process is called thermoregulation. From perspective of calculating heat transfer between a human body and its surroundings, we focus on a layer of skin | 10 | CO1 |


|  | and fat, with its outer surface exposed to the environment and its inner surface at a temperature slightly less than the core temperature, $\mathrm{T}_{\mathrm{i}}=35^{\circ} \mathrm{C}=308 \mathrm{~K}$. Consider a person with a skin/fat layer of thickness $L=3 \mathrm{~mm}$ and effective thermal conductivity $\mathrm{k}=0.3 \mathrm{~W} / \mathrm{mK}$. The person has a surface area $\mathrm{A}=1.8 \mathrm{~m}^{2}$ and is dressed in a bathing suit. The emissivity of skin is $\varepsilon=0.95$. <br> (a) When the person is in still air at $\mathrm{T}_{\infty}=297 \mathrm{~K}$, What is the skin surface temperature and rate of heat loss to the environment? Convective heat transfer to the air is characterized by a free convection coefficient of $h=2 \mathrm{~W} / \mathrm{m}^{2} \mathrm{~K}$. <br> (b) When the person is in water at $\mathrm{T}_{\infty}=297 \mathrm{~K}$, what is the skin surface temperature and heat loss rate? Heat transfer to the water is characterized by a convective coefficient of $h=200 \mathrm{~W} / \mathrm{m}^{2} \mathrm{k}$ |  |  |
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| Q 7 | Consider a concentric tube heat exchanger with hot and cold-water inlet temperature of $200^{\circ} \mathrm{C}$ and $35^{\circ} \mathrm{C}$ respectively. The flow rate of hot and cold fluids is 42 and $84 \mathrm{~kg} / \mathrm{h}$, respectively. Assume the overall heat transfer coefficient is $180 \mathrm{~W} / \mathrm{m}^{2} \mathrm{~K}$. What is the maximum heat transfer rate that could be achieved for the prescribed inlet conditions? If the exchanger is operated in counter flow with heat transfer area of $0.33 \mathrm{~m}^{2}$. Determine the outlet fluid temperature. | 10 | $\mathrm{CO3}$ |
| Q. 8 | Calculate the net radiant heat exchange per $\mathrm{m}^{2}$ area for two large parallel plates at temperatures of $427^{\circ} \mathrm{C}$ and $27^{\circ} \mathrm{C} . \varepsilon($ hot plate $)=0.9$ and $\varepsilon($ cold plate $)=0.6$. If a polished aluminum shield is placed between them, Compute the $\%$ reduction in the heat transfer $\varepsilon($ shield $)=0.4$ | 10 | $\mathrm{CO1}$ |
| Q. 9 | A heat engine receives heat from a source at 1500 K at a rate of $700 \mathrm{~kJ} / \mathrm{s}$, and it rejects the waste heat to a medium at 320 K . The measured power output of the heat engine is 320 kW , and the environment temperature is $25^{\circ} \mathrm{C}$. Determine (a) the reversible power, (b) the rate of irreversibility, and (c) the second-law efficiency of this heat engine. | 10 | $\mathrm{CO5}$ |
|  | SECTION C (40 Marks)- Attempt any two |  |  |
| Q 10 | At a particular instant of time, a square metal bar has an axial temperature distribution given by: $T(x)=50\left(1+8 x^{2}\right)$ where $x$ is the distance (in meters) measured from one end and T is the local temperature (in ${ }^{\circ} \mathrm{C}$ ). Due to its high thermal conductivity, the temperature in the bar may be assumed uniform at any cross-section. The cross-section of the bar has width $\mathrm{W}=2.5 \mathrm{~cm}$ and the length of the bar is $\mathrm{L}=0.3 \mathrm{~m}$. The density and specific heat of the metal are $\rho=2700 \mathrm{~kg} / \mathrm{m} 3$ and $\mathrm{c}=0.90 \mathrm{~J} / \mathrm{kg}-\mathrm{K}$, respectively. <br> a.) Is the average bar temperature rising or falling at this instant of time? (Assume that the bar can only transfer energy at its end points; i.e., the sides are insulated.) | 20 | $\mathrm{CO1}$ |


|  | b.) Calculate the change in internal energy if the bar is cooled to a uniform temperature of $\mathrm{T}_{\mathrm{f}}=20^{\circ} \mathrm{C}$. <br> c.) Calculate the change in entropy of the bar for the process in part (b). <br> d.) What is the change in exergy of the bar for the process in part (b) given a large heat sink at $20^{\circ} \mathrm{C}$ ? <br> e.) What is the maximum thermal efficiency at which work could be produced for the conditions in part (d)? |  |  |
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| Q. 11 | The sketch below shows an ideal experiment done in a perfectly insulated, rigid container with compartments separated by a frictionless piston. The two compartments contain different amounts of the same gas ( $\mathrm{m}_{\mathrm{A}}=1.2 \mathrm{~m}_{\mathrm{B}}$ ). The piston is nonadiabatic (heat can be transferred) and moves very slowly. Compartment A is initially at a higher temperature than compartment $\mathrm{B}\left(\mathrm{T}_{\mathrm{A}}>\mathrm{T}_{\mathrm{B}}\right)$ but the pressure in the two compartments is the same. Assume an ideal gas with constant $\mathrm{c}_{\mathrm{p}}$ and $\mathrm{c}_{\mathrm{v}}$. <br> a) Which way, if at all, does the piston move? Indicate by an arrow on the drawing and give an explanation (5 Marks). <br> b) Evaluate final temperatures and volumes in compartments A and B? Express your answer in terms of given properties ( 10 Marks). <br> c) Evaluate net work done in the experiment ( 5 Marks)? | 20 | CO4 |
| Q. 12 | The side of a building of height $\mathrm{H}=7 \mathrm{~m}$ and length $\mathrm{W}=30 \mathrm{~m}$ is made entirely of glass. Estimate the heat loss through this glass (Ignore the thermal resistance of the glass) when the temperature of the air inside the building is $20^{\circ} \mathrm{C}$, the outside air temperature is $-15^{\circ} \mathrm{C}$ and a wind of $15 \mathrm{~m} / \mathrm{s}$ blows parallel to the side of the building. Select the appropriate correlation from those listed below of local Nusselt number to estimate the average heat transfer coefficient. For air take: $\rho=1.2 \mathrm{~kg} / \mathrm{m}^{3}, \mu=1.8 \times 10^{-5}$ $\mathrm{kg} / \mathrm{m} \mathrm{s}, \mathrm{C}_{\mathrm{p}}=1 \mathrm{~kJ} / \mathrm{kg} \mathrm{K}$ and $\operatorname{Pr}=0.7$ <br> - Free convection in air, laminar $\left(\mathrm{Gr}_{\mathrm{x}}<10^{9}\right): \mathrm{Nu}=0.3 \mathrm{Gr}_{\mathrm{x}}{ }^{1 / 4}$ <br> - Free convection in air, turbulent $\left(\mathrm{Gr}_{\mathrm{x}}>10^{9}\right): \mathrm{Nu}=0.09 \mathrm{Gr}_{\mathrm{x}}{ }^{1 / 3}$ <br> - Forced convection, laminar $\left(\operatorname{Re}_{\mathrm{x}}<10^{5}\right): \mathrm{Nu}=0.33 \operatorname{Re}_{\mathrm{x}}{ }^{0.5} \operatorname{Pr}^{1 / 3}$ <br> - Forced convection, turbulent $\left(\operatorname{Re}_{\mathrm{x}}>10^{5}\right): \mathrm{Nu}=0.029 \operatorname{Re}_{\mathrm{x}}{ }^{0.8} \operatorname{Pr}^{1 / 3}$ | 20 | CO 2 |

