## UNIVERSITY OF PETROLEUM AND ENERGY STUDIES

## End Semester Examination, December 2017

Program Name: Int. B. Tech ET + LLB (IPR)
Course Name : Material and Energy Flow Computation
Semester - III

Course Code : CHEG 201
Max. Marks : 100
Duration : 3 Hrs
No. of page/s:

## Instructions:

Attempt all questions from Section-A (each carrying 10 marks); all Questions from Section-B (each carrying 12 marks) and any one Question from Section-C (carrying 20 marks).

## Section-A (Attempt All Questions)

| Section-A (Attempt All Questions) |  |  |  |
| :---: | :---: | :---: | :---: |
| 1. | An analysis of the vent gases from the chlorinator of a plant for making chlorinated rubber showed $70 \%$ by volume $\mathrm{HCl}, 20 \%$ by volume $C l_{2}$ and the rest is $C C l_{4}$. Determine: <br> (a) the $\%$ composition by weight <br> (b) the average molecular weight of the gas <br> (c) The density at standard conditions. | [10] | CO2 |
| 2. | The vapor pressure of diethyl ether at 273 K is 25 kPa and its latent heat of vaporization is $4.185 \times 10^{2} \mathrm{~kJ} / \mathrm{kg}$. Using the Classius-Clapeyron equation, estimate the vapor pressure at 293 K and 308 K . | [10] | CO 3 |
|  | SECTION B (Attempt All Questions) |  |  |
| 3. | Barium Chloride reacts with Sodium Sulphate to precipitate Barium Sulphate : $\mathrm{BaCl}_{2}+\mathrm{Na}_{2} \mathrm{SO}_{4} \rightarrow 2 \mathrm{NaCl}+\mathrm{BaSO}_{4}$ <br> (a) How many grams of Barium Chloride are needed to react with 100 g of sodium sulphate? <br> (b) For precipitating 50 g of Barium Sulphate, how many gram of the reactants are consumed? <br> (c) How many grams of Sodium Chloride would be obtained when 50 g of Barium Sulphate is precipitated? <br> Atomic weight of Barium $=137.32 \mathrm{~g} / \mathrm{mol}$ | [12] | $\mathrm{CO2}$ |
| 4. | A mixture of Benzene and air contains $15 \%$ Benzene by volume at 300 K and 101.3 kPa . The vapor pressure of Benzene at 300 K is 13.8 kPa . Calculate the following: <br> (a) The weight fraction of Benzene in the mixture <br> (b) The molal humidity <br> (c) The absolute humidity <br> (d) The percent saturation <br> (e) The percent relative saturation <br> (f) The mass of air in $100 \mathrm{~m}^{3}$ of the mixture | [12] | $\mathrm{CO4}$ |


| 5. | The flue gas from an industrial furnace has the following composition by volume: $\mathrm{CO}_{2}=11.73 \%, \mathrm{CO}=0.2 \%, \mathrm{~N}_{2}=0.09 \%, \mathrm{O}_{2}=6.81 \% \text { and } \mathrm{N}_{2}=81.17 \%$ <br> Calculate the percentage excess air employed in the combustion if the loss of carbon in clinker and ash is $1 \%$ of the fuel used and the fuel has the following composition by weight: $\mathrm{C}=74 \%, \mathrm{H}_{2}=5 \%, \mathrm{O}_{2}=5 \%, \mathrm{~N}_{2}=1 \%, \mathrm{~S}=1 \%, \mathrm{H}_{2} \mathrm{O}=9 \%$ and ash $=5 \%$. |  |  |  |  | [12] | CO5 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 6. | A solution of potassium dichromate in water contains $13 \% \mathrm{~K}_{2} \mathrm{Cr}_{2} \mathrm{O}_{7}$ by weight. 1000 kg of this solution is evaporated to remove some amount of water. The remaining solution is cooled to $20^{\circ} \mathrm{C}$. If the yield of $\mathrm{K}_{2} \mathrm{Cr}_{2} \mathrm{O}_{7}$ crystals is $80 \%$. Calculate the amount of water evaporated. Solubility of $\mathrm{K}_{2} \mathrm{Cr}_{2} \mathrm{O}_{7}$ is 0.390 kgmol per 1000 kg water $\left(20^{\circ} \mathrm{C}\right)$ atomic weight: $\mathrm{K}=39 \mathrm{~g} / \mathrm{mol}, \mathrm{Cr}=52 \mathrm{~g} / \mathrm{mol}$. |  |  |  |  | [12] | CO5 |
| 7. | Fresh juice contains $14 \%$ solids and $86 \%$ water by weight and is to be concentrated to contain $42 \%$ solids by weight. In a single evaporator system, it is found that the volatile constituents of juice escape with water leaving the concentrated juice $56 \%$, with a flat taste. To overcome this problem part of the fresh juice bypass the evaporator. Calculate: <br> (i) The fraction of juice that bypass the evaporator <br> (ii) The concentrated juice produced containing $42 \%$ solids by weight. |  |  |  |  | [12] | CO5 |
|  | SECTION C ( Attempt Any One) |  |  |  |  |  |  |
| 8. | A continuous fractionating column, operating at 1 atm., is to be used to separate $15000 \mathrm{~kg} / \mathrm{h}$ of a solution of Benzene and Toluene containing $50 \%$ (by weight) Benzene into an overhead product containing $96 \%$ (by weight) Benzene and $97 \%$ (by weight) Toluene in the bottom product. The feed will be at its boiling point and a reflux ratio of 2.5 kg of reflux per kg of distillate is to be used. Calculate the condenser and reboiler load. <br> Data: <br> Enthalpy of feed $=170.8 \mathrm{~kJ} / \mathrm{kg}$ <br> Enthalpy of reflux liquid $=67 \mathrm{~kJ} / \mathrm{kg}$ <br> Enthalpy of vapor leaving the column and entering the condenser $=540 \mathrm{~kJ} / \mathrm{kg}$ <br> Enthalpy of liquid leaving the reboiler $=201.8 \mathrm{~kJ} / \mathrm{kg}$ |  |  |  |  | [20 | CO6 |
| 9. | Obtain an empirical equation for calculating the heat of reaction at any temperature T (in $\mathrm{K})$ for the following reaction: $\mathrm{CO}(\mathrm{~g})+2 \mathrm{H}_{2}(\mathrm{~g}) \rightarrow \mathrm{CH}_{3} \mathrm{OH}(\mathrm{~g})$ <br> Data: $\Delta H_{R}^{o}$ at $298 K=-90.41 \mathrm{~kJ} / \mathrm{mol}$ $C_{p}^{o}=a+b T+c T^{2}+d T^{3}, \frac{\mathrm{~kJ}}{\mathrm{kmol} . \mathrm{K}}$ |  |  |  |  | [20] | $\mathrm{CO6}$ |



