| Name: <br> Enrolment No: |  |  |  |
| :---: | :---: | :---: | :---: |
| Course <br> Progra <br> Course <br> Instru | \left.UNIVERSITY OF PETROLEUM AND ENERGY STUDIES  <br> End Semester Examination, May 2019 $\right]$ Semester: 4 <br> ions: Please submit the APPENDIX- 1 along with the answer script. |  |  |
| SECTION A |  |  |  |
| S. No. |  | Marks | CO |
| Q 1 | What is flow separation? | 5 | CO1 |
| Q 2 | What is closed circuit crushing? | 5 | CO2 |
| Q 3 | (a) Define mesh and pitch of screens. <br> (b) What does TSS stands for, w.r.t. to particle characterization? | $\begin{aligned} & 4 \\ & 1 \end{aligned}$ | CO 3 |
| Q 4 | What is shear-mixing mechanism? | 5 | CO4 |
| Q 5 | Give two examples of fluid flow through beds of solids. | 5 | CO5 |
| SECTION B |  |  |  |
| Q 6 | Differentiate between free settling and hindered settling of particles in a fluid. | 8 | CO1 |
| Q 7 | Derive the critical rotation speed ( $N_{\mathrm{c}}$ ) for a ball mill and calculate the critical speed in revolution/minute, of a ball mill with an internal diameter of 1200 mm loaded with balls of 70 mm diameter. <br> OR <br> Describe the working of any (one) comminution equipment for crushing a feed of intermediate size materials, along with a proper-labelled diagram. | 8 <br> 8 | CO 2 |
| Q 8 | The screen analysis representing size distribution of particles is shown in Fig. 1. Using Gates-Gaudin-Schumann method, compute the particle size distribution of the particles (for three sizes) present in the pan. | 8 | CO3 |
| Q 9 | What is agglomeration? What are the different stages of agglomeration of particulate matter? <br> OR <br> Describe in brief the dense phase pneumatic conveying system with a proper-labelled diagram. | 8 <br> 8 | CO4 |
| Q 10 | What are nanoparticles? Give three applications of nanoparticle w.r.t. its properties. | 8 | CO5 |
| SECTION C |  |  |  |


| Q11 | (i) Derive the expression of terminal settling velocity $\left(V_{\mathrm{t}}\right)$ of a particle falling in a <br> fluid with very low Reynolds number. <br> (ii) How does the size of a container (or vessel) affect the terminal settling velocity <br> ( $V_{\mathrm{t}}$ ) of a particle? Give the expression for terminal settling velocity when the ratio of <br> the size of particle to that of the size of container is significant. <br> OR | $\mathbf{1 0}$ | $\mathbf{1 0}$ |
| :--- | :--- | :--- | :--- |
| A cyclone separator is used to remove sand grains from an airstream at $150^{\circ} \mathrm{C}$. If the <br> cyclone body is 0.6 m in diameter and the average tangential velocity is $16 \mathrm{~m} / \mathrm{s}$, what <br> is the radial near the walls for a particle of $20 \mu \mathrm{~m}$ in size? How much are these <br> values greater than the terminal velocity in gravity settling? Given data: You can <br> make use of Fig. $\mathbf{2}$ and $\mathbf{3}$. While, specific gravity of particles $=2.2$. | $\mathbf{2 0}$ | $\mathbf{C O 1}$ |  |
| Q 12 | Derive Ergun equation for flow of liquid through packed bed. Mention all the <br> assumptions wherever necessary. | $\mathbf{2 0}$ | $\mathbf{C O 5}$ |

## APPENDIX- 1

| This sheet (containing Fig. $1-3$ ) needs to be submitted along with the answer script. |  |
| :--- | :--- |
| Roll number: | SAP ID: |

Fig 1:
Particle
size
distributio
n results of
a screen analysis.


Fig 2: Plot
for drag coefficient vs
Reynolds number of single particle.



Fig. 3: Viscosity of gases.

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## UNIVERSITY OF PETROLEUM AND ENERGY STUDIES End Semester Examination, May 2019

Course: Particulate Technology
Program: B. Tech (Chemical Engineering)
Course Code: CHCE 2007

Semester: 4
Time 03 hrs.
Max. Marks: 100

Instructions: Please submit the APPENDIX-1 along with the answer script.

## SECTION A

| S. No. |  | Marks | CO |
| :--- | :--- | :---: | :---: |
| Q 1 | What is terminal settling velocity? Give its mathematical expression. | 5 | CO1 |
| Q 2 | State Bond's law for size reduction of particulate matter? Give its mathematical <br> expression. | 5 | CO2 |
| Q 3 | (a) Define aperture and pitch of a screen. <br> (b) What does BSS stands for, w.r.t. to particle characterization? | 4 | CO3 |
| Q 4 | Explain convective mixing of solids. | 5 | CO4 |
| Q 5 | Illustrate any two examples of fluid flow through beds of solids. | 5 | CO5 |

## SECTION B

| Q 6 | Differentiate between free settling and hindered settling. | 8 | CO1 |
| :---: | :---: | :---: | :---: |
| Q 7 | Describe in brief the working of a jaw crusher along with a proper-labelled diagram. <br> OR <br> Differentiate between a cone crusher and gyratory crusher. | 8 8 | CO 2 |
| Q 8 | The screen analysis of a sample of 100 g of crushed quartz is shown in Table 1. The density of the particles is $2,650 \mathrm{~kg} / \mathrm{m}^{3}$ and the shape factors are $\boldsymbol{a}=2$ and sphericity, $\phi_{s}=0.571$. For material between 5 -mesh and 10 -mesh in particle size, calculate the fraction of particles retained on $6 / 8$ mesh. | 8 | $\mathrm{CO3}$ |
| Q 9 | Explain the various stages of agglomeration of a particulate matter. <br> OR <br> Describe in brief the dilute phase pneumatic conveying system with a proper-labelled diagram. | 8 8 | CO4 |
| Q 10 | Describe any four applications of a nanoparticle (or nanomaterials) in various field of science and technology. | 8 | $\mathrm{CO5}$ |
| SECTION-C |  |  |  |
| Q 11 | (i) A particle of $50 \mu \mathrm{~m}$ in size is falling in a stationary fluid under the effect of gravity. Derive the expression of terminal settling velocity $\left(V_{t}\right)$ of the particle. Also, include all necessary assumptions wherever needed. | 10 | CO1 |


|  | (ii) Describe the influence of the size of container (or vessel) on the terminal settling <br> velocity $\left(V_{t}\right)$ of a particle. Also, mention the expression for terminal settling <br> velocity when the ratio of size of particle to that of container is significant. | $\mathbf{1 0}$ |  |
| :--- | :--- | :--- | :--- |
| Q12 | A partial oxidation is carried out by passing air with 1.2 mole percent of propane <br> through 40 mm tubes packed with 2 m of 3 mm by 3 mm cylindrical pellets. The air <br> enters at $350^{\circ} \mathrm{C}$ and 2.0 atm with a superficial velocity of $1 \mathrm{~m} / \mathrm{s}$. What is the pressure <br> drop through the packed tubes? Given data: Void fraction $=0.4$, and viscosity of air <br> at $350^{\circ} \mathrm{C}=3.5 \times 10^{-5} \mathrm{~kg} \mathrm{~m}^{-1} \mathrm{~s}^{-1}$. | $\mathbf{2 0}$ | $\mathbf{C O 5}$ |
| Derive the expression of pressure drop for flow of fluids through packed beds of <br> solids with the help of a proper-labelled diagram. Mention all the assumptions <br> wherever necessary. | OR |  |  |

## APPENDIX- 1

This page needs to be submitted along with the answer script.
Roll number: $\quad$ SAP ID:

Table 1: Results of screen analysis of a mixture of particles of various sizes.

| Mesh <br> No. | Mesh <br> opening, <br> mm | Mass <br> retained, <br> grams |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 4 | 4.75 | - |  |  |  |  |  |
| 5 | 3.35 | 15 |  |  |  |  |  |
| 6 | 2.80 | 45 |  |  |  |  |  |
| 8 | 2 | 20 |  |  |  |  |  |
| 10 | 1.80 | 10 |  |  |  |  |  |
| Pan | - | 10 |  |  |  |  |  |

