Roll No:

## 1 UPES

## UNIVERSITY OF PETROLEUM AND ENERGY STUDIES

## End Semester Examination, May 2018

Program: B. Tech (ET_IPR)
Subject (Course): Heat and Mass Transfer Process
Course Code : GNEG 353
Semester - IV
Max. Marks : 100

No. of page/s: 03

## Instructions:

Assume suitable data if missing with proper justification

|  | Section-A <br> Answer all the questions |  |  |
| :---: | :---: | :---: | :---: |
| Q. No | Question | Marks | CO |
| 1 | A 100 mm diameter pipe carrying a hot chemical at $250^{\circ} \mathrm{C}$ is covered with layers of insulation, each 50 mm thick. The length of the pipe is 5 m . The outer surface temperature of the composite is $35^{\circ} \mathrm{C}$. The rate of heat loss through the pipe is 270 W . If the thickness of the outer insulation is increased by $25 \%$, the heat loss is reduced to 260 W . Calculate the thermal conductivities of the two insulating materials. | 12 | CO1 |
| 2 | Discuss overall heat transfer coefficient (U) for a parallel flow heat exchanger. Also consider fouling factor | 12 | CO4 |
| 3 | A mixture of He and $\mathrm{N}_{2}$ gas is contained in a pipe at 298 K and 1 atm total pressure which is constant throughout. At one end of the pipe at point 1 the partial pressure pA 1 of He is 0.60 atm and at the other end $0.2 \mathrm{~m} \mathrm{pA} 2=0.20 \mathrm{~atm}$. Calculate the flux of He at steady state if DAB of the $\mathrm{He}-\mathrm{N}_{2}$ mixture is $0.687 \times 10^{-4} \mathrm{~m}^{2} / \mathrm{s}$ | 12 | CO5 |
| 4 | Consider the $5-\mathrm{m} \times 5-\mathrm{m} \times 5-\mathrm{m}$ cubical furnace, whose surfaces closely approximate black surfaces. The base, top, and side surfaces of the furnace are maintained at uniform temperatures of $800 \mathrm{~K}, 1500 \mathrm{~K}$, and 500 K , respectively. Determine (a) the net rate of radiation heat transfer between the base and the side surfaces, $(b)$ the net rate of radiation heat transfer between the base and the top surface, and $(c)$ the net radiation heat transfer from the base surface <br> Data: $F_{12}=0.2$ | 12 | CO3 |
| 5 | A 20 cm diameter pipe carrying steam is provided with 5 cm thick insulation whose thermal conductivity varies with temperature as $k(T)$ $=0.062\left(1+0.362 \times 10^{-2} \mathrm{~T}\right) \mathrm{W} / \mathrm{m}^{\circ} \mathrm{C}$ where T is in ${ }^{0} \mathrm{C}$. The temperatures at | 12 | CO1 |


|  | the pipe surface and at the outer surface of the insulation are $275^{\circ} \mathrm{C}$ and $65^{\circ} \mathrm{C}$ respectively. Calculate (a) the rate of heat transfer for the meter length of the pipe (b) the temperature at the mid-thickness of the insulation. |  |  |
| :---: | :---: | :---: | :---: |
|  | SECTION-B <br> Answer all the questions |  |  |
| 6 | (a) Discuss about dropwise condensation | 8 | CO 2 |
|  | (b) Saturated steam at atmospheric pressure condenses on a 2-m-high and $3-\mathrm{m}$ wide vertical plate that is maintained at $80^{\circ} \mathrm{C}$ by circulating cooling water through the other side. Determine (a) the rate of heat transfer by condensation to the plate and (b) the rate at which the condensate drips off the plate at the bottom. | 12 | CO 2 |
| Section-BAnswer all the questions |  |  |  |
| 7 | (a) Discuss boiling curve and boiling regims in pool boiling | 8 | CO 2 |
|  | (b) Water is to be boiled at atmospheric pressure in a mechanically polished stainless steel pan placed on top of a heating unit. The inner surface of the bottom of the pan is maintained at $108^{\circ} \mathrm{C}$. If the diameter of the bottom of the pan is 30 cm , determine <br> (a) the rate of heat transfer to the water and $(b)$ the rate of evaporation of water. The properties of water at the saturation temperature of $100^{\circ} \mathrm{C}$ are $=1.75 \begin{array}{ll} \begin{array}{l} \sigma=0.0589 \mathrm{~N} / \mathrm{m} \\ \rho_{\mathrm{l}}=957.9 \mathrm{~kg} / \mathrm{m}^{3} \end{array} & \mathrm{~h}_{\mathrm{fg}}=2257.0 \times 10^{3} \mathrm{~J} / \mathrm{kg} \end{array} \operatorname{Pr}_{1}$ | 12 | CO 2 |

