


Name:			
Enrolment No:			
<div>UPES</div> <div>End Semester Examination, May 2025</div> <div><div>Programme Name : B. Tech Chemical Engineering</div><div>Semester : IV</div><div>Course Name : Numerical Methods in ChE</div><div>Time : 03 hrs</div><div>Course Code : CHCE2019</div><div>Max. Marks: 100</div><div>Nos. of page(s) : 2</div><div>Instructions: (a) Attempt all questions.</div><div>(b) Assume the value of missing data, if any.</div></div>			
SECTION A (12×5 = 60 M)			
S. No.		Marks	CO
Q 1	<p>In the below system of linear equations assume any real value of a_{12}, a_{23}, a_{31} and b_2 so that the system has a unique solution and solve the equation by Gauss Gauss-Seidel method</p> $\begin{bmatrix} a_{12} & 2 & 1 \\ 1 & 3 & a_{23} \\ a_{31} & 2 & 6 \end{bmatrix} \begin{bmatrix} x_1 \\ x_2 \\ x_3 \end{bmatrix} = \begin{bmatrix} 2 \\ b_2 \\ 3 \end{bmatrix}$	12 M	CO1
Q 2	<p>The Ergun equation is used to describe the flow of fluid through a packed bed. ΔP is the pressure drop, ρ is the density of the fluid, G_o is the mass velocity, D_p is the diameter of the particles within the bed, μ is the fluid viscosity, L is the length of the bed and ε is the void fraction of the bed.</p> $\frac{\Delta P \rho D_p}{G_o^2 L} \frac{\varepsilon^3}{1-\varepsilon} - 150 \frac{1-\varepsilon}{(D_p G_o / \mu)} - 1.75 = 0$ <p>Experiments are carried out on a packed bed to estimate the void fraction of the bed, ε. The best fit values of the dimensionless parameters of the bed are reported as, $\frac{D_p G_o}{\mu} = 1000$ and $\frac{\Delta P \rho D_p}{G_o^2 L} = 10$.</p> <p>Use an open iterative scheme of your choice to estimate the value of ε using an initial guess of 0.25. Do <i>Three</i> iterations.</p>	12 M	CO2
Q 3	<p>Heat transfer in a straight fin of uniform cross section is given as,</p> $\frac{d^2 \theta}{dx^2} - m^2 \theta = 0$ $x=0, \quad \theta=1$	12 M	CO3

	$x=1, \quad \frac{d\theta}{dx} = -(Bi)\theta$ <p>Where θ is the dimensionless temperature at any position in the fin, x is the dimensionless location, Bi is the dimensionless Biot number, and m^2 is the product of Bi and a dimensionless group involving the fin dimensions. Obtain the algebraic equations to be solved using the finite difference technique with step size 0.25. [You don't need to solve the problem]</p>																						
Q 4	<p>Fit a second-order polynomial using the least square method to the following data</p> <table><tr><td>x</td><td>0</td><td>1</td><td>2</td><td>3</td><td>4</td><td>5</td></tr><tr><td>y</td><td>2.1</td><td>7.7</td><td>13.6</td><td>27.2</td><td>40.9</td><td>61.1</td></tr></table>	x	0	1	2	3	4	5	y	2.1	7.7	13.6	27.2	40.9	61.1	12 M	CO2						
x	0	1	2	3	4	5																	
y	2.1	7.7	13.6	27.2	40.9	61.1																	
Q5	<p>The river is 80 meters wide. The following table gives the depth D in meters at a distance x meters from one bank. Calculate the cross-section area of the river using (a) Simpson's 1/3 rule (b) Simpson's 3/8 rule.</p> <table><tr><td>x in meter</td><td>0</td><td>10</td><td>20</td><td>30</td><td>40</td><td>50</td><td>60</td><td>70</td><td>80</td></tr><tr><td>D in meter</td><td>0</td><td>4</td><td>7</td><td>9</td><td>12</td><td>15</td><td>14</td><td>8</td><td>3</td></tr></table>	x in meter	0	10	20	30	40	50	60	70	80	D in meter	0	4	7	9	12	15	14	8	3	12 M	CO3
x in meter	0	10	20	30	40	50	60	70	80														
D in meter	0	4	7	9	12	15	14	8	3														
<p style="text-align: center;">SECTION B (20×2 = 40 M)</p>																							
Q 6	<p>(a) Use the Newton-Raphson method, with 3 as starting point, to find a fraction that is within 10^{-4} of $\sqrt{10}$.</p> <p>(b) Discuss the conditions for the rate of convergence of the Newton-Raphson algorithm using the fixed-point iteration method.</p>	20 M	CO2																				
Q 7	<p>Consider a series reaction $A \xrightarrow{k_1} B \xrightarrow{k_2} C$ carried out in a batch reactor. The differential equation for component A is,</p> $\frac{dC_A}{dt} = -k_1 C_A$ <p>for component B is,</p>	20 M	CO4																				

$$\frac{dC_B}{dt} = k_1 C_A - k_2 C_B$$

and for component C ,

$$\frac{dC_c}{dt} = k_2 C_B$$

The initial condition is: at $t = 0$, $C_A = 1$, $C_B = 0$, and $C_c = 0.5$. The rate constants are $k_1 = k_2 = 1 \text{ sec}^{-1}$. Use the fourth-order Runge-Kutta method to determine the concentration of A, B and C up to 6 sec, using a step size of 2 sec.